History of 81-10:

81-10 mgs. in Yaly and mortfly technical reports

12-55 considering purchase of a mercury-still-to recover Hz by distillation 10-12,1961 8/10 six concs. stop

9/EX-24. equipment H20 Spill sin pgo 34,57,93 113 141 148,106

decenting description (Depier)

V Refo:

1. efficiency study 1959

2. Specifications instructions 1956, 1953

3. operating procedure (not dated)

4. log sheets (1957-1962) A-2, A-4, A-5

5. Y/EX-21/DEL REV (DO Not Use Y/EX-24 anymore - out dated)

Spills > 81-10 B-4 (1953)

Stroopa.xls

		TABLE	i 61-10 Mercu	iy Recuvery	Operations (3/57	~ <i></i>	
						Days in	Total lbs.
Month/Year	Condensed (lbs)	Cumulative	Decanted (lbs)	Cumulative	Comments	Operation	recovered
Apr-57	4,204	4,204	31,151	31,151		13	35,35
May-57	19,982	24,186				18	·
Jun-57	56,343	80,529		·		26	<u> </u>
Jul-57	60,452	140,981		ļ		29	
Aug-57	30,141	171,122	<u></u>		<u> </u>	30	4
Sep-57	48,527	219,649	<u> </u>	 	i	27	400,39
Oct-57	73,595	293,244		American and a second a second and a second	Larranter and the control of the con	30	488,94
Nov-57	65,483	358,727	52,494		no logsheet	29	606,92
Dec-57	36,008	394,735				21	659,19
Jan-58	54,801	449,536				26	718,76
Feb-58	45,523	495,059			<u> </u>	24	
Mar-58	59,717	554,776		L		31	839,85
Apr-58	58,770	613,546			<u> </u>	30	
May-58	52,747	666,293			<u> </u>	22	988,98
Jun-58	0_,,,,	666,293			L	0	990,030
Jul-58	65,959			338,664		21	1,070,910
Aug-58	71,727		<u> </u>			31	1,160,38
Sep-58	82,257			<u> </u>		28	1,280,63
Oct-58	67,396					29	
Nov-58	92,869	1,046,501				30	
Dec-58	48,583	1,095,084				30	
Jan-59	29,481	1,124,565			<u> </u>	16	
Feb-59	0	1,124,565				0	
Mar-59	24,912	1,149,477	ļ.,,	\$		13	·
Apr-59	30,391	1,179,868				30	2,178,06
May-59	20,327	1,200,195	***********************************			30	2,336,45
Jun-59	25,140	1,225,335	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,		2711-1111111111111111111111111111111111	30	2,396,94
Jul-59	23,384	1,248,719		<u> </u>		31	2,435,34
Aug-59	28,268	1,276,987				31	2,475,23
Sep-59	24,037	1,301,024		<u> </u>		30	L
Oct-59	8,166	1,309,190				20	
Nov-59	0,100	1,309,190		4		0	
Dec-59	5,901	1,315,091	42,941	1,304,616		4	
Jan-60	24,202	1,339,293		1,354,878		20	2,694,17
Feb-60	14,100	1,353,393				20	
Mar-60	20,594	1,373,987				27	2,789,03
Apr-60	19,873	1,373,860				30	
May-60	6,687	1,400,547				21	2,901,61
Jun-60	3,986	1,404,533	· · · · · · · · · · · · · · · · · · ·			22	2,920,02
Jul-60	7,359	1,411,892	11,796			20	2,939,18
Aug-60	2,515	1,414,407	15,751			23	2,957,44
Sep-60	4,130	1,418,537				19	2,981,82
Oct-60	6,403	1,410,557		1,584,972		18	
Nov-60	4,876	1,429,816				21	3,033,69
Dec-60	9,965	1,429,010				23	
Jan-61	11,378	The state of the s	ng nyana ngantinga ni ya masa katawa na wata saanaa maana iliaanse	him in the company of the company of the	20 720		Annual Control of the
Feb-61	7,358	1,451,159 1,458,517		1,639,674 1,661,051	28,729 28,735		· · · · · · · · · · · · · · · · · · ·

81100P2.XLS

Mar-61	21,912	1,480,429	32,493	1,693,544	54,405	31	3,173,973
Apr-61	33,089	1,513,518	33,930	1,727,474	67,019	30	3,240,992
May-61	0	1,513,518	0	1,727,474	0	. 0	3,240,992
Jun-61	0	1,513,518	0	1,727,474	0	0	3,240,992
Jul-61	0	1,513,518	0	1,727,474	0	0	3,240,992
Aug-61	15,467	1,528,985	0	1,727,474	no logsheet	?	3,256,459
Sep-61	15,468	1,544,453	0	1,727,474	no logsheet	?	3,271,927
Oct-61	15,467	1,559,920	0	1,727,474	no logsheet	?	3,287,394
Nov-61	15,468	1,575,388	0	1,727,474	no logsheet	?	3,302,862
Dec-61	15,467	1,590,855	0	1,727,474	no logsheet	?	3,318,329
Jan-62	22,744	1,613,599	6,314	1,733,788		20	3,347,387
Feb-62	32,619	1,646,218	43,312	1,777,100		28	3,423,318
Mar-62	39,505	1,685,723	43,003	1,820,103		30	3,505,826
Apr-62	12,762	1,698,485	24,977	1,845,080		30	3,543,565
May-62	7,615	1,706,100	8,580	1,853,660		12	3,559,760
Jun-62	0	1,706,100	0	1,853,660		0	3,559,760
Jul-62	0	1,706,100	0	1,853,660		0	3,559,760
Aug-62	0	1,706,100	29,453	1,883,113		?	3,589,213
Sep-62	0	1,706,100	5,039	1,888,152		?	3,594,252
Oct-62	.0	1,706,100	0	1,888,152		?	3,594,252
	Condensed %	47.47%	Decanted %	52.53%			
			1 5 1				
	= peak operations						
Source: Y/HG-0	005 and Y/HG-0023 logs	heets					
						21	720
				Calculations	Performed by	$> 1/\sqrt{\lambda}$	Coor
					Date	6-5	5-95
	.,						
				Calculations	Checked by		
					Date		



1135 Atlantic Avenue Alameda, CA 94501 415.521.5200 FAX 415.521.1547

Subject: A/R LOSSES FROM 8/-/0

By: TR 17 Date: 4/4/95 Sheet: 1053

AIR LOSSES FROM ROASTING AND DECAMPTING AT 21-10

S. FLACH 4/3/95

48-4790 OF Hy WAS CONDENSED FROM ROASTING

ASSUME 46.5%

RACOUBAY Actual Zi JOAR 1010 195 7 10300 719, 499 p.93 From Rons Take 394, 135 (actual 2) 3 3 4 567 700, 349 1,189,734 1958 1,189,134 553 226 220,007 ~ 770,734 1959 770,714 358 410 256,225/96/ -106,0663 /cm 124,690 ~ 442,397 1960 205715 109,699 69824 150,207 353,260/962 3,597,645 275,923 TOTAL 3,597,208/ 3,597,208/ 1100/672 102/ 1924506/

RECOVERY PROM 264,464 (setual 3 84 93Z 489,385 636 508 550,767 41Z 364 3175707 236 682 146,526 80 335 173 685

1,700,687 - ASSANING UNITS ARTE POUNDS, CHACK THIS!

NOT SPECIFIED ON Po 93 OF Y-EX/24

- 6 SIGNIFICANT DIQUE ACCURACY MAY DE SPURIOUS. CRECK PHIS

FROM J. REECE UNION CARBIDS NOCKEAR MOON OF 5/15/59 [Y/46-0499] PZ ROSULTS OF TEST RUL

MERCUAY RECOVERED 34/18 RECOVERY + Known LOSSES 371. / LB

FARNACE EXECUTIVEY = 341 = 919 = 12



1135 Atlantic Avenue Alameda, CA 94501 415.521.5200 FAX 415.521.1547 Subject: AIR LOSSES FROM 81-10

By: TRM Date: 4/4/95 Sheet: 2 0 = 3

', ROASTING FURNACE INPUT : RECOVERY

FROM PAGE Z, LOSS TO STACH GAS IS

18 18 = ,000485 OR ,0485 To or WALTS

RAMAINING LOSS IS TO ASH OR SCRUBBER WATER SCRUBBER WATER DISCHARGE SKOWS UP IN WATER DISCHARGE MEASUREMENT

, , ROASTING FURNACE LOSS IS

= .000485 (FURNACE RECOVERY) 8

= .0005278 FURNACE RECOVERY

SO AIR COSS FROM ROASTANG AT 8/-10 15

ESTIMATED AT: YEAR

AIR LOSS (LBS)

177 1957 4289 292 1958 3259 189 1959 1975 109 1960 1374 36,9 1961 1030 1962 74.7 1030 883 TOTAL

Y-AX/29 BSTIMATIE OR 8201-4+8201-5 AIR EXMAUST LOSSES



1135 Atlantic Avenue Alameda, CA 94501 415-521-5200 FAX 415-521.1547 Subject: Air Lossus Fran 8/-10

By: TRM Date: 4/4/95 Sheet: 30/3

DETERMINE DETAILS OF DECEMENTE PROCESS OUTDOORS?

INDOORS?
IN ENCLOSED VESSELS?
HOLDING TIME FOR
DRAINING PROCESS?

Hiel

INTER-COMPANY CORRESPONDENCE

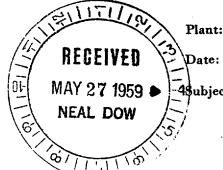
UNION CARBIDE NUCLEAR COMPANY

A Division of Union Carbide and Carbon Corporation

To:

J. S. Reece

Copies To: V. Defenderfer File



Plant: Y-12

May 15, 1959

M-80

-4\$ubject: 81-10 Operations on Solvent

Contaminated Dirt

Y/HG-0499

The following is a summary of the work done at 81-10 on the solvent recovery from dirt which was excavated from 9201-2 grounds:

- 1. 120 drums of solvent contaminated dirt was prepared for the furnace by pulverizing and screening out the rocks.
- 2. On May 4, 1959, this material was started as feed to the furnace. At this time the entire 81-10 system was void of solvent.
- 3. On May 5, 1959, we added 1141 pounds of solvent to the system from outside sources in order to arrive at daily production figures by reading the sight glass on the solvent receiver.
- 4. On May 6, 1959, we removed 827 pounds of solvent from the receiver due to not being able to get accurate daily production figures by this method.
- 5. It was decided that we withdraw each days production from the receiver and weight.
- 6. The results of the operations are as follows:

Date	Drum Fed	Lbs of Feed	Vol. Feed (Cr. Ft.)	Production (Lbs.)
5-4-59	6	2184	33	Not Determined Not Determined Not Determined 13 54 53
5-5-59	16	5824	88	
5-6-59	19	6916	104.5	
5-7-59	18	6552	99	
5-8-59	*17	6188	93.5	
5-9-59	8	2912	44	

* Started feeding uncontaminated carbon dust.
The operation was shut down from 11:30 A.M., 5-9-59 until 7:00 A.M. on 5-11-59 because of furnace ash removal problems.

APPROVED FOR PUBLIC RELEASE

Technical Information Office

Date

5-11-59 at 9:30 A.M. Total 84

30,576

462

130

(or 17.1 Cr Yds)

On 5-11-59 at 9:30 A.M., we started feeding 20 drums of solvent contaminated dirt which, according to visual determination, should have been richer than the above 84 drums.

5-11-59 and 5-12-59 results.

Total 20

7,280

110

100#

Grand Total

104

37,856

572

341

7. Following is a summary of the actual recovery plus the known losses in comparison with the expected production according to Laboratory Analysis:

Analysis on Feed Dirt 2.25% Hg
Analysis on Furnace Ash < .03% "
Analysis on Cyclone Ash < .06% "
Analysis on Scrubber Water .0025% Hg
Analysis on Stack Gases 14.11 gram/day

Expected production = $2.25\% \times 37,856\% = 851.71 \text{ lbs Hg.}$

Actual production = 341.00 lbs Hg.

Losses from Furnace Ash = 35,401# X .03% Hg. = 10.62 " " Losses from Fly Ash = 2,184# X .06% Hg. = 1.31 " " Losses from Scrabber H₂0 = 719,712# X .0025% Hg. = 17.99 " " Losses from Stack Gases = $\frac{14.11 \text{ gms X 6}}{1.51}$ = .18 " "

Total production + Known Losses

= 371.10 "

The known losses plus recovery = 43.55% of the expected yield according to the raw feed analysis. Due to the difficulty of sampling it, it is very improbable that a representative sample was analyzed. Also, due to the low percentage of Hg in the sample the laboratory's limit of error maybe high.

Carbon dust was added to reduce oxygen content in furnace. After we started feeding carbon dust an analysis was made of the furnace draft. Results: Oxygen - 9.1%, Carbon Dioxide - 8.0%.

249 July 8.

- 9. Results from the above operation:
 - A. The recovery represents .9% of the dirt fed.
 - B. The recovery plus the known losses represents .98% of the dirt fed.
 - C. Based on the above, and for the above material, the furnace efficiency is approximately 91.8%.

VD:jr

				· · · · · · · · · · · · · · · · · · ·			CUMULATIV	CUMULATIVE SUPPLIED OF SOLVENT		RECOVERY FACILITY	TILLIT						
								•						=			
	ર્જી.	Druma		Pounds		Pounds		Pounds To		Pounds To			Total	Operating	Total	Unit Cost	# Coa
		Processed	Processed	Current	Pounds Decanted	Current	Condensed		Cascades	Current	Cascades	Current	Reclaimed		Cost		Per Poun
1957	Operated		To Date					- 1		Honth			TO Date	модъл	PART OF	MOTOT	TO DE CO
	5	3	3	3	31 161	1. 201	1, 201,	37. 355	35, 355	þ	þ	35,355	35,355	6,475	6,475	.183	
ADITAL	3 2	130	3	67 05	8 046	10.082	21.186	87.887	123, 24,2	þ	ဝ	87,887	123,242	15,568	22,043	.177	
June	26	198	386	36,115	135,471	56,343	80,529	92,758	216,000	þ	þ	92,758	216,000	13,019	35,062	.tho	
√LmL.	29	178	568	15.091	150.565	60.152	1/0.981	75,51.6	291,51.6	ļ	þ	75.516	291,516	12,268	h7.330	.162	
ingust	30	325	893	10.770	161,335	30, 141	171,122	40,911	327.457	þ	þ	116 '01	322,457	15,086	62,416	.369	
September	27	288	1,181	19,106	180,741	կ8,527	219,649	67.933	կ00,390	þ	þ	67,933	1,00,390	18,839	81,255	.277	
October	30	ի53	1.63\	յ <u>հ. 963</u>	195, 701	73,595	293, շևև	88,558	1.88, 91.8	þ	þ	88,858	188,948	21,901	103,156	247	
Movember	29	h27	2.051	52,494	248,198	65,483	358,727	76,368	565,316	11,609	11,609	177,977	606,929	щ,369	117,525	.122	
December	21	349	2,400	16,266	26կ.կ6կ	36,008	394.735	52,274	617,590	þ	11,609	52,274	659,199	14,433	131,958	.276	
1958					.T.												
January	26	6سا	2,186	Ju 763	269,227	50,801	July 536	þ	617,590	59.564	101.173	59.564	718,763	12,265	11111.223	200	
February	24	327	3.11/3	2,502	271.729	15.523	195,059	12,461	630,051	35.564	136,737	48,025	700,700	0,042	400°2¢T	100	
March	31	433	3,576	13.348	285,077	59.717	554.776	þ	630,051	73,065	209, 602	73,005	039,053	13,273	00000T	20Te	
April	30	125	4,001	19,797	304.874	58.770	613,516	þ	630,051	78,567	288, 369	78,567	918,420	13,094	1/9,252	, or	
May	22	253	և.25և	17,816	322,690	52,747	666,293	60,460	1115°069	10,103	2/11/062	(0,503	900,903	20106	TACENCT	e Co	
June	þ	þ	4.254	1,053	323,743	þ	666,293	1.053	691.564	þ	298,472	1,053	990,036	8,259	199,243	7.843	
July	21	335	կ.589	14,921	388,664	65.959	732,252	80,880	772.444	þ	298,472	00,000	916 0/0 T	15,370	KTO TTZ	36.	
August	11	Ь78	5.067	17.713	356,407	71.727	803,979	5.074	777,518	84,396	382,868	074,68	89,470 1,100,386	24,132	230,751	2/0	
September	28	592	5,659	37,991	394,398	82,257	886,236	99,979	877,497	20,269	403,137	120,248	120,248 1,280,634	10,939	257,090	151	
October	29	661	6,323	176,533	570,931		953,632	4,879	882,376	239,050	642,187	243,929	243,929 1,524,563	10,729	×111,411	•009	
November	ğ	737	7,060	115,306	686,237	92,869	1,046,501	188,622	1,070,990	19,555	oth, CToo	C176002	10()62()61	16,202	720,062	•0/0	
December	11	Ь75	7.535	67.612	753,849	48,583	1,095,084	32,750	1,103,928	83,445	745,005	116,195	1,848,933	15,211	305,832	.131	
1959											222	5 333	22.	676 7	23 676	3	16.
January	13	192	7,720	22,852	776,701	۴	70, 707	4	ON COLET	26,000	200,700	37 620	300 1 000 mg	2 757	215 257	10	763
February	0	0	7,727	27,630	804, 331		1,124,505	19, 69	04/ 50L L	0,702	201. XX	62 661	1 921 560	5 987	778 168	200	161
March		120	7,000	20,00	042,000	276647	1)47,79411	02,004	To Low of the		000	2,00	1		,		
			٠												·		
48) Y-12 DATA SHEET	. #I		_									-					
))	•								

INTER-COMPANY CORRESPONDENCE

(INSERT) COMPANY CARBIDE AND CARBON CHEMICALS COMPANY LOCATION OAK RIC

Mr. George Evans LOCATION Building 9204-4

DATE July 7, 1953 ANSWERING LETTER DATE

ATTENTION

COPY TO

Dr. J. W. Strohecker Mr. W. K. Whitson, Jr. SUBJECT Solvent Recovery Proces Drawings.

Enclosed you will find one (1) copy each of nine drawings; numbers E2e-15658, B2e-16236, D3f-16939a, D5f-16962a, D5f-16979a, D5f-1698la, D5f-16940a, D5f-17000, and D5f-17037. Five of these are revised drawings and the balance are drawings that were lacking in your files.

These drawings should give you one complete set of up to date drawings on the Solvent Recovery Process for your files.

R. E. Hulum

R. E. Hulme

REH: tcc

inclosure.

Here re He Arrings?



APPROVED FOR PUBLIC REL

Technical Information Office

INTER-COMPANY CORRESPONDENCE

(INSERT) COMPANY CARBIDE AND CARBON CHEMICALS COMPANY LOCATION Post Office Box P

M-810

то Ј.

J. M. Lister

DATE

July 13, 1953

LOCATION

ANSWERING LETTER DATE

ATTENTION

copy to W. K. Whitson, Jr. Y-12RC

J. A. Ebert

R. D. Williams

File

SUBJECT

Summary of Chemical Recovery from May 25.

1953 to July 11, 1953.

Y/49-0440

I. Source of information for Beta-4 alloy losses.

Bonnet losses were based on the CTF inventory figures of April 1, 1953 through April 15, 1953.

Cannisters and Crubbing losses were based on information supplied by T. p. Sprague June 5, 1753.

Blender Station losses were based on the CTF inventory of April 1, 1953 through April 15, 1953.

II. Mechanical Failures of Bonnets.

The rate of failure for Beta-4 was based on the failures in CTF from May 1, 1953 to June 9, 1953.

III. Value of Allov in Beta-4.

A cost curve was received from Dr. DeMarcus and this curve is the basis for all the cost figures that have been calculated on the losses for Beta-la.

IV. Equipment and Supplies

- (1) At the present all the tanks originally called for have been set. The piping around these tanks will have to be changed to fit the future needs.
- (2) The water scrubbers and sinks are expected to be shipped the middle of July.
- (3) A list of equipment available in change house #9723-18 has been supplied to Mr. George Jasny.
- (4) 4 acid tanks for cleaning bonnets are being made in Y-12.
- (5) 6 dollies, with a filtering system built on them for the recovery of alloy from solvent oxide at the blender station, are being made in Y-12.

(6) I dolly for salvage pick up is being made in Y-12.

(7) A list of supplies needed in Chemical Recovery has been supplied to Mr. H. Fisher.

APPROVED FOR PUBLIC RELEASE

THIS FORM FOR INTER-COMPANY TECHNICAL ON DIFFICE Date.

WCX-80 (6-51)

V. Job Break Sown and Assignments

- John Crowe (1) Calculation of losses, failure rates and loss by mixing of alloy.
 - (2) Making a note book of the information used in the calculations for Beta-4 Chemical Recovery.
 - (3) Vent gas header drain procedure.
- J. A. White (1) Forked on salvage of alloy from solvent oxide.
 - (2) Records for Chemical Tecovery Area.
 - (3) Calvaging of assay samples.
- R. Langham (1) Colvent Roaster procedure.
 - (2) Chemical Recovery tank procedure.
 - (3) alvace of plant samples.
- J. Ellison (1) Connet washing and handling procedure.
 - (2) Somet washing equipment.
 - (3) Moved family to Oak Fidge.
 - (4) Will work in CTF July 13 through July 26 as vacation relief.
- C. Whitwill (1) Maintenance training.
 - (2) Sonnet washing and handling procedure.
 - (3) connet washing equipment.
- 3. Baldwin) (1) Cannister change procedure.
- K. Kahley) (2) Jannister change equipment.
 - (3) Salvade containers for sample and other salvace in cascade area.
 - (4) alwage pick up 'r ific pattern.
- IV. The present plan for the chemical recovery group in seta-h is to separate the alloy into assay levels and store the salvage in drums until a process for purification of the salvage is worked out.

J. II. Ivans

CWE:wa

JNCLASSIFIED

INTER-COMPAN WILLIAM SECTION OF THE STREET

ASBIINE. ost Office Box P COMPANY CARBIDE AND CARBON CHEMICALS COMPAN

го	
----	--

J. M. Lister

M-810

DATE

August 10, 1953

LOCATION

COPY TO

ATTENTION

W. K. Whitson, Jr. (Y-12RC)

J. W. Ebert

R. D. Williams

File

SUBJECT.

Chemical Recovery

Progess Report Week Ending

August 9, 1953 😰

national defense of the United States. meaning of the espionage laws. Title 18 U.S. to an unauthorized person

ANSWERING LETTER DATE

HG-0413

- I. Procedures were issued on August 8, 1953, to supervision and operators.
- All Chemical Recovery operators were transferred from C.T.F. to 9204-4 during the week.
- III. Bonnet washers and pumps are set. Some delay on the finishing of the bonnet washers due to trouble in getting pipe fittings. fittings are expected in this week.
- IV. One thousand and nine (1009) pounds of solvent was recovered and returned to the solventarea.
 - V. We have had trouble with F-852 and F-853 tanks running over. This is due to a 1 1/2" line connecting F-851 through F-855 to the sewer. This line is being changed to a 3" line and a 55-gallon stainless steel drum trap is being installed between the tanks and the sewer.
- When unstopping the floor drains, we found the sewer lines are either broken or eaten up. We forced air and water through the drains and when the air was on, water would bubble through the floor over most of the area.

DEPARTMENT OF ENERGY DECLASSIFICATION REVIEW st Reviewer Rowan Determination 生 (Insert Number(s)) 1. Classification Retained HADO DADO. 2. Classification Changed To: 3. Contains No DOE Classified Information Classification Cancelled O. K. McConnell, Classified Information Bracketed (Name) 6. Other (Specify) Authority: ADDy 294

MMES OA

Y-12 Classification Office

Name: 5 Mure 00

Date: 11-29-94

W. Evans

GWE/jm

Classification changed to

APPROVED FOR PUBLIC RELEASE

nical Information Office Date

by authority of

Verified by

CORRESPONDENCE ONLY

solutions may be effective decontaminants, but their use would result in the formation of considerable amounts of calomel which would probably be carried into the creek by entrainment in the floor drain water. From the literature, it appears that iodine adsorbed on activated carbon may be quite efficient in absorbing mercury vapor from the air, and this treatment could possibly be used in isolated areas where it is not necessary to wash down the floor.

A number of industrial floor and wall coatings have been obtained or are on order. These will be tested for their ability to provide a smooth, non-porous surface, resistant to caustic solutions. It appears that a good floor surface, which could be easily cleaned, might be obtained by covering the concrete with asphalt tile. Crack fillers are also being investigated.

No solutions have been found which materially aid in washing down mercury droplets deposited on a vertical surface. Common alkali metal scaps appear to be as effective as any detergent. The possibility of cleaning the floor by using a motor driven brush is being considered. This would either be incorporated into a vacuum cleaning device or a floor washer. For cleaning the grease and oil off motors and pumps, chlorinated solvents are quite effective but somewhat toxic. A proprietary compound known as "Gunk", which is an alkaline aqueous emulsion of a small percentage of some organic solvent, shows considerable promise for this job. Since it is an aqueous dispersion it can be removed by rinsing with water.

Apparatus is being set up with which to measure the efficiency and useful life of respirator canisters and cartridges. These measurements will be made as a function of both mercury and water vapor concentration. The same type of equipment should make it possible to evaluate the remaining useful life of a partially exhausted absorption element.

A General Electric mercury vapor meter has been altered to permit the sample examination of a small sample of air over an extended period of time. It has been found that when the mercury vapor is exposed to the ultraviolet light it reacts rapidly, supposedly with oxygen. This may reduce the usefulness of the modified meter as an analytical device, but it should still be useful for measuring the rate of absorption of mercury by various materials and by breathing if proper precautions are taken.

Mercury Recovery

Additional plant-scale experiments indicate that about 50% of the mercury in filter cakes can be recovered by drying with agitation in a birdbath evaporator. Frobably a larger percentage could be recovered from the lense sludges collected from the bottoms of the filter feed tanks. A combination drying and distillation procedure carried out in a single piece of apparatus would probably result in the most economical recovery of the mercury. Such an apparatus would allow the wet sludge to be dried with gentle agitation and the separated mercury to be drained off. The temperature would then be raised, probably with the charge still gently agitated, and the remaining mercury distilled off.

If it becomes necessary to use mercury vapor control agents which result in the formation of large quantities of mercury salts, it will no doubt be necessary to thoroughly treat the floor drain water in order to remove the entrained, and perhaps dissolved, mercury.

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Pending any re-evaluation of the scope of the proposed changes in light of a reduced premium on increased production, and the recent progress made in betterment of the mercury contamination problem, process engineering work is complete.

SOLVENT RECOVERY, ALPHA-4 AND ALPHA-5, (W. O. B-7131)

The quantities of solvent contained in discard materials such as filter press solids, evaporator feed tank sludges, and floor sweepings warranted initiation of design for a recovery system. It is estimated that a minimum of 15,000 lbs/mo. of solvent can be recovered from approximately 150 drums/mo. of accumulated salvage.

The recovery process is being designed for location in Building 81-10 which was previously used for a similar function. The original installation will be revised and reactivated to process the sludge by burning in a roaster, and recovering the solvent in a water cooled condenser.

CONTINUOUS SALVAGE PROCESS, BUILDING 9212, (W. O. B-6466)

Recent changes in the scope of the planned Daffodil continuous salvage facilities are as follows:

- (1) The allowable diameter of new, low concentration safe storage tanks has been increased from 5" to 6". This change has reduced the number of new tanks required for storage capacity.
- (2) The existing inter-column metering pumps have been found to be not economically adaptable to automatic control and are to be replaced with low capacity air-motor driven positive displacement pumps in the aqueous stream and centrifugal pumps in the organic stream. Installation of the new pumps is estimated to cost less than reconditioning and converting the existing pumps for autocontrol.
- (3) The extraction column tops and bottoms are being expanded from 4 to 7 inches to provide control stability and minimum organic carryover, respectively.

BULK CHEMICAL FACILITIES, (W. O. B-6414)

Equipment design and specifications for pumps, tanks, and an ammonia mixing station were completed in February. Cost estimates based on aqua-ammonia consumption in 1955, indicated an economy in preparing aqua-ammonia at the Y-12 Plant; however, the recent downward trend in aqua-ammonia usage reduces the freight savings to a level precluding a five-year amortization period for the installation. Consequently, new handling equipment for the



solutions through the existing manually controlled system were replaced with controlled capacity, rotary pumps. The immediate benefit evolved from the pump change is operating space and the anticipated benefit is longer pump shaft-seal life.

The piping and equipment layout was directed towards a modular type arrangement, with a module consisting of an extraction column, associated pumps and controls.

EXTRACT AREA CHANGES, BUILDING 9201-5

The Alpha-5 Extract System has been modified to function as a feed salt recrystallization system with the object of preparing acceptable feed. Basic changes to the existing system are an increase in the crystallizing and centrifuging capacity, and addition of a purified feed crystal redissolving tank and transfer station.

As a result of these changes, the capacity of the Extract System has been increased from 1,500 pounds of salt per hour to 4,000 pounds per hour of redissolved purified feed.

LOW PRESSURE NITROGEN APPLICATION, BUILDING 9727-3

A material balance around the nitrogen generating station located in Building 9727-3 indicated a monthly nitrogen loss of approximately 1,500,000 cubic feet. An investigation of loss sources in the operation revealed that approximately 90% of the computed loss, results from spillage when transferring liquid nitrogen to portable containers. The remaining 10%, or 150,000 cubic feet per month, is through tank vents and could be recovered. However, the capital costs for a recovery and distribution system are such as to require three to five years operation to break even. The economy of a recovery system is still less attractive in comparison with the previously proposed nitrogen generator, utilizing waste hydrogen, as generator nitrogen can be produced with very low operating costs.

SOLVENT RECOVERY, BUILDING 9201-4 and 9201-5

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A recovery process has been designed for separating and purifying an estimated 35,000 pounds of mercury per month contained in approximately 200 drums of sludge. The contaminants are principly water, finely divided carbon, caustic salts, filter cloths and floor sweepings. The process provides for a shredder to reduce bulk contaminants to unfiform small size. The prepared sludge will be metered by a feed screw into a multiple-hearth, gas fired furnace. The contained moisture and solvent in the sludge will be vaporized and finely divided carbon will be burned. Combustion of the carbon will augment the gas-flame heat, however, no allowances in furnace capacity is being made because of the variability of carbon in the sludge feed.

Provisions are planned in the furnace to remove liquid mercury accumulation resulting from the coagulation of mercury droplets in dried sludge.

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Journal Article (Identify Journal):			
X Other (Specify): To Be Releas	sed to ChemRisk, Phas	se II	
Document will be published in proceedings	No Yes		
Document will be distributed at meeting	No 🔃 Yes		
Document has patent or invention significance	No 🔲 Yes (Identify)		
Document has been previously released	No Yes (Reference)		
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TABLE I

RELATIVE EFFICIENCY OF IMPINGEMENT-TYPE DEMISTER WITH AIRFOIL ELEMENTS AND YORKMESH DEMISTER

Ii Passed (g./hr.)	Demisting Efficiency	Gas Flow (cfm.)
1.2	15	12.6
0.7	49	12.6
0.29	80	12.6
0.19	81	12.6
0.25	82	12.6
	(g./hr.) 1.2 0.7 0.29 0.19	1.2 15 0.7 49 0.29 80 0.19 81

the voltage drop decreased to 4.7 volts in about two hours. Laboratory cells showed no difference of any kind between samples of solution taken during the two periods of operation.

Mercury Recovery

A small plate-and-frame filter press was set up to filter a portion of the waste stream which is pumped from the sump in back of Alpha-4 to the creek. The filter medium was paper and the filter effluent was sparkling clean. Pressure drop across the filter was very low and did not increase appreciably with time. The analytical results are somewhat in doubt but indicate that a good portion of the mercury can be removed by filtration.

LABORATORY AND BENCH-SCALE STUDIES

Cascade Feed

fans have been installed, six in the roof and six in the fourth floor. These fans are operating with temporary power pending receipt of the new motor control centers. These fans supply additional air to the decomposer areas. Four vaneaxial fans which serve to boost the supply air from the fan rooms are installed and operating on temporary Data for several of the tests are shown in Figure 2.

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CATALYTIC CONSTRUCTION COMPANY PHILADELPHIA 2, PENNSYLVANIA

Y/HG-0059

ALPHA 5 - PROJECT OAK RIDGE, TENNESSEE

JOB UNIT NUMBER 4140 - UCNC W. O. B-7131

SOLVENT SALVAGE FACILITY
TITLE BUILDING NO. 81-10

SPECIFICATION B-7131-L-1

DESCRIPTION MULTIPLE HEARTH FURNACE

ORIGINAL ISSUE DATE July 30, 1956

APPROVED FOR PUBLIC RELEASE

A 22/h

Technical Information Office Date

APPROVED BY CATALYTIC CONSTRUCTION COMPANY

P.S. LINDSEY, THATE 10/22/56

APPROVED BY UNION CARBIDE NUCLEAR COMPANY

/s/ G. B. Lockhart DATE 8-3-56

APPROVED BY ATOMIC ENERGY COMMISSION

/s/ R. B. Somers DATE 8-6-56

UNCLASSIFIED

TABIT 22 1966

Rev. #3 - 10-19-56 - Page 7 - As Per Meeting of 10-17-56 with Vendor's Representative and Letter of 10-19-56 Covering Changes

Rev. #2 - 9-26-56 - Pages 1, 2, 5, 6, 7; 11-A Added - To Conform to Vendor's Proposal

Rev. #1 - 8-13-56 - Pages 1, 9, 10 and 11 - Changed Item Number Prefix

CONTRACT #4100

CERTIFIED FOR CONSTRUCTION



Job No. 4140 Spec. B-7131-L-1 Page 1 of 12 July 30, 1956 Rev. #1 - 8-13-56 Rev. #2 - 9-26-56

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SECTION 1 - SCOPE:

This specification covers the design, fabrication and delivery of one (1) multiple hearth furnace complete with mechanical drive, gas combustion equipment, forced draft fan, charge feeder and hopper, calcine outlet gate and asbestos cloth dust hood and shaft cooling air fan.

SECTION 2 - EQUIPMENT INCLUDED:

Equipment	Item Number	Location	
Multiple Hearth Furnace Complete	7131-L-1	Building 81-10	(1)
Furnace Drive Mechanism:	•		
Speed Reducer Speed Reducer Motor	7131-L-1-A 7131-NL-1-A		(1) (1)
Forced Draft Fan Forced Draft Fan Motor Charge Feeder and Hopper:	7131-L-1-B 7131-NL-1-B		(1) (1)
Screw Feeder Screw Feeder Motor Charge Hopper	7131-L-1-C 7131-NL-1-C 7131-L-1-D		(1) (1) (1)
Gas Combustion Equipment	7131-L-1-E		(1)
Calcine Outlet Gate	7131-L-1- F		(1)
Asbestos Cloth Dust Hood	7131-L-1-G		(1)
Shaft Cooling Air Fan Shaft Cooling Air Fan Motor	7131-L-1-Н 7131-NL-1-Н		(2) (2)

SECTION 3 - MANUFACTURER/VENDOR RESPONSIBILITIES:

3-A Material and Workmanship Warranty

- 1. Warranty on workmanship and all material and equipment described herein shall be for one year from date of installation or two years from date of shipment, whichever occurs first.
- 2. All defective parts shall be replaced at the Vendor's expense provided such defective parts have been given normal and proper usage.
- 3. This specification calls for the purchase of new equipment throughout.

Job No. 4140 Spec. B-7131-L-1 Page 2 of 12 July 30, 1956 Rev. #2 - 9-26-56

h. This material warranty supplements any other material warranty clause included within this specification.

3-B Performance Guarantee

Unless specific exception is recorded by the Vendor in his proposal and provided such exceptions are noted in the purchase order, it shall be understood that he guarantees and agrees to the following:

- 1. The equipment described herein shall be guaranteed to meet the operating conditions and requirements as specified herein.
- 2. Performance tests, under specified conditions of service, may be conducted by the purchaser within 30 days after initial operation. If a unit fails to perform as specified after Vendor has had a reasonable opportunity to remedy any defects at his own expense consistent with Security requirements, it is hereby understood and agreed that the Vendor shall accept return of the unit and refund the full amount of the purchase price.

3-C Equipment Marking

- 1. All equipment, parts and appurtenances included herein shall be plainly labeled with a securely attached metal tag bearing the equipment item number.
- 2. Each unit shall be crated securely and independently of other units to prevent damage in shipment.
- Crates and packages shall be appropriately marked with ink, paint or indelible material.

SECTION 4 - WORK TO BE DONE BY MANUFACTURER/VENDOR:

- 4-A The Manufacturer/Vendor shall design, fabricate and deliver the equipment described herein. All special tools and equipment required for dismantling and maintenance as well as the specified drawings, parts lists, manuals, etc., shall be supplied.
- 4-B The Manufacturer/Vendor shall complete and return one (1) copy of Motor Data Sheets 4D9-283, 4D9-284, 4D9-285 and 4D9-289 with each copy of bid submitted.

SECTION 5 - WORK TO BE DONE BY OTHERS:

- 5-A Erection and installation of equipment.
- 5-B Motor starters and wiring.
- 5-C Temperature measuring instruments and recorders.

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SECTION 6 - OPERATING CONDITIONS & REQUIREMENTS:

The multiple hearth furnace shall be of vertical, self-supporting type, completely furnished with mechanical drive, gas combustion equipment, forced draft fan, charge feeder, charge hopper and calcine gate, ..., and shall be designed and fabricated in accordance with the following criteria:

6-A Operating Conditions

1. Feed

The charge material will be a wet sludge and at times will contain please of filter paper, filter cloth and graphite lumps up to 1/2-inch in size; its composition will be as follows:

-	Wt. %
Water Metal carbonates, finely divided	40.0 - 58.0
graphite and anthracite	10.0 - 12.0
vaporized in the furmace)	50.0 - 30.0
Specific heat - 0.003 Etu/lb.	
Bulk density - 75 - 200 lb/cu.ft. Feed Rate - 500 lb/hr. (2.5 to .) : 7.5 cu.ft./br.)	

Processing of the feed will involve essentially a drying operation for removal of the water and distillation operation for recovery of the other volatiles.

2. Temperatures

Hearth - Max. 1550° F Exhaust gas - 950°F - Mix.

Residence Time - 2 hrs. minimus

3. Pressure

The furnace shall be operated at a megative pressure of (0.10) inches of water as measured at the top hearth.

4. Services Available

Natural gas up to 30 psig with a calorific value of 1055 Btu/cu.ft. (dry basis) a specific gravity of 0.6, and of the following composition:

% Volume
94.51
3 .3 1
0.78
0.18
0.21
0.03
0.05
0.04
0.18
0.68

Ground elevation at job site - 1000 ft.

5. Calcine and Non-Combustibles

Bulk density - approx. 70 lb/ou.ft.
Accumulation rate - up to 60 lb/hr.

6-B Performance

When operating within the limits of the specified operating conditions, the furnace shall be capable of processing the charge materials on a continuous 24-hour basis. The furnace shall be provided with features to exclude the infiltration of air and permit the maintenance of reducing atmosphere in the hearth and. All equipment furnished shall be suitable for outdoor operation.

6-C Physical Details

The furnace/shall consist of multiple circular refractory hearths, cothe proper size, placed one above another, and enclosed of thin a cylindrical steel shell lined with suitable refractors insulating materials. Rabble arms supported on a vertical maft passing through the center of the hearths shall be employed for moving the charge through the hearths. The discharge from the bottom hearth shall pass through a scaled, gate-controlled chute into a 55 gallon drum.

Charge materials shall be fed into the furnace by means of a variable caracity screw type conveyor through a closed chute.

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1. Shell and Supports

The shell, including the bottom plate, shall be fabricated of medium carbon steel plate with all joints welded gas tight. Suitably located inspection doors, burner openings, and openings for temperature measuring instruments of the radiation pyrometer or thermocouple type shall be provided for in the shell body for each hearth. The inspection doors shall be of gas tight gasketed construction and equipped with a peep-hole having a close-fitting sliding-type cover.

Structural steel columns shall be provided for supporting the furnace together with a platform to support the shell, the bottom shaft bearing, and the speed reducer.

2. Charge Feeder and Hopper

The feeder mechanism shall be a horizontal ribbon screw type feeder, of steel construction, totally enclosed, and capable of delivering a feed quantity of 2.5 to 7.5 cubic feet per hour. Provision shall be made for varying the feed rate by means of a controlled variable speed drive. Feeder and drive shall be protected against mechanical injury in case of jamming or overloading.

Flanged connections shall be provided at both the top inlet and bottom discharge ends of the feeder. The top inlet shall be connected to a feed hopper having a capacity of at least eight (3) cubic feet. Feed hopper construction shall be of plate steel.

Supports shall be provided for mounting the feeder and hopper on top of the furnace.

The feed inlet to the furnace shall be fabricated of Type 304 stainless steel and provided with a flange to fit the flanged discharge end of the charge feeder.

3. Refractory Lining

The furnace shell shall be lined internally with a layer of super-duty fireclay brick, Harbison-Walker Brand "Alamo" or equal, and a layer of insulating brick, the combination of which should be capable of maintaining the temperature of the outside shell at less than 200° F when the inside refractory temperature is maintained at about 1600° F. Out

Job No. 4140 Spec. B-7131-L-1 Page 6 of 12 July 30, 1956 Rev. #2 - 9-26-56

drop holes should be formed of castable refractory suitable for service at temperatures of about 1600° F. Fire brick and hearth refractory shall be suitable for caustic service.

The furnace bottom shall be provided with a layer of dry sand topped with a castable refractory layer to form the bottom hearth. The top of the furnace shall be a flanged, medium carbon steel plate covered internally with a castable refractory layer and an insulating layer of Johns-Manville Superex blocks or equal.

The furnace hearths shall be constructed of castable refractory, Harbison-Walker Extra-strength castable or equal, and shall be constructed in the field on forms furnished by the Vendor.

4. Drive Mechanism, Rabble Arms and Shaft

The furnace drive mechanism shall consist of a bevel gear splined to the central shaft below the bottom hearth of the furnace. Provision shall be made for driving the bevel gear through a speed reducer with a 190 to 1 reduction. A shaft speed variation of 3 to 1 shall be provided by means of a varispeed motor pully (Reeves or equal). Provision shall also be made for a shear pin in the drive which will be set to break if the rabble arms meet with an obstruction.

The central drive shaft shall be constructed of ductile iron, Grade 80-60-03, and insulated with a castable refractory material. Shaft openings at the top and bottom of the furnace shall be provided with suitable seals to prevent gas leakage. Cast heat-resistant alloy lutes shall be provided to seal the central shaft openings at all the "out" hearths.

Four rabble arms shall be provided for each of Hearths #1 and #2 and two rabble arms shall be provided for each of Hearths #3, #4, #5, #6, #7 and #8, designed to fit into the central shaft and held by retaining pins. Pins and arms shall be removable and replaceable through the hearth access doors. The rabble arms as well as the rabble teeth or plows shall be fabricated of a heat resistant alloy of the following approximate analysis: 25% chrone, 12% nickel with the balance essentially iron.

5. Forced Draft Fan

A motor driven forced draft fan shall be provided capable of supplying the volume of free air required for combusion purposes.

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Job No. 4140 Spec. B-7131-L-1 Page 7 of 12 July 30, 1956 Rev. #2 - 9-26-56 Rev. #3 - 10-19-56

Both fan and motor shall be capable of twenty-four hour continuous duty operation. The connections between the fan and the base of the furnace shaft shall also be provided.

Provision shall be made for adjusting the quantity of air fed to the furnace.

6. Calcine Outlet and Outlet Gate

The calcine outlet shall be fabricated from a heat resistant high alloy steel and shall be connected to a positive closing calcine outlet gate through a flanged connection. A sealed connection such as an asbestos cloth hood, shall be provided between the calcine gate and an adapter ring for a standard 55 gallon drum which will be used as the calcine receiver. It shall be possible to remove and replace the drum receiver without any leakage of air into the furnace while the furnace is operating. The calcine outlet shall be located oblique to the furnace floor so as to discharge clear of furnace drive mechanism and supports.

7. Gas Outlet

The gas outlet from the furnace shall be suitably sized and provided with a flanged connection. The outlet shall be located at the top of the furnace.

8. Gas Combustion Equipment

Gas burners shall be provided and located as required. The burners shall be of a type such that firing on a hearth may be regulated independently of any other hearth, with a minimum turn-down ratio of 10 to 1. Burner boxes shall be sealed to the furnace shell. In addition to the burners, auxiliary equipment required for mixing and regulating the fuel shall be provided. The burner auxiliary equipment shall be capable of controlling combustion conditions to maintain air-gas proportions.

Combustion safe-gurarding devices shall be furnished to provide immediate shut-off of the fuel supply when power and/or combustion fails and permit fuel flow only when combustion can take place safely. The safety devices should include spark ignition of the pilot flame, pilot view-windows, "Firetron" type detectors, manual re-set shut-off safety valves, an audible alarm, and automatic purge timing. Pilot lights should be supplied through separate regulators. "Firetron" detectors are manufactured by Combustion Control Corporation.

9. Center Shaft Cooling Air Fan
A fan and motor will be furnished to provide air for cooling the
center shaft.

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Job No. 4140 Spec. B-7131-L-1 - Page 8 of 12 July 30, 1956

9. Painting and Finish

All exterior surfaces shall be given a shop coat of red lead and oil, or equivalent protective coating, before shipment. All exposed machined parts shall be given a protective coating of a rust preventative material before shipment, suitable for corrosion prevention under outdoor conditions.

10. Materials of Construction

Copper and copper alloy materials of construction shall not be employed where there is a possibility of contacting the charge materials and process vapors.

SECTION 7 - INSPECTION:

Inspection is required by the Architect-Engineer prior to shipment. The Architect-Engineer shall be advised of shipping date at least two (2) weeks prior to shipment.

SECTION 8 - REFERENCE SPECIFICATIONS:

The following Catalytic Construction Company specifications form a part of this specification:

4100-DD-1 - Welding Procedure & Quality Required 4100-N-19 - Electric Motors

Job No. 4140

Spec. B-7131-L-1 Page 9 of 12 July 30, 1956 CATALYTIC CONSTRUCTION CORev. #1 - 8-13-56 ENGINEERING DIVISION MOTOR

MOTOR DATA

	Furnace Drive - Spee	a Reducer	JOB A		
	Building No. 81-10		SHEET		3
Œ.	Continuous		DATE.	***************************************	
EQU	IRED One (1)		BY		•
		PERFORMAN	CE		
٠, ٠	•	FULL LOAD	78% LOAD	50% LOAI	
٠	EFFICIENCY PERCENT			. 30% 10/1	,
	POWER FACTOR PERCENT				
-	FOWER FACION PERCENT			-	
	•	MOTOR SPEC	SIFICATION	•	
·	MOTOR TO BE	FURNISHED IN ACCORDANCE	WITH SPECIFICATION	1 NO. 4100-N	-19
	MANUFACTURER				
	RATED H. P.		VOLTS 440	PHASE 3	CYCLES
	TYPE Totally Fncl	osed - Fam Cooled			
		- 			
					1. 74
					1. 1.
	SYNCHRONOUS R. P. M.				+ v ² + v ²
	FULL LOAD R. P. M.		·		1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1
	RISE DEGREE CENTIGRADE			·	100
	ALTITUDE		<u> </u>		100
	FRAME NO.	· · · · · · · · · · · · · · · · · · ·			15
	BERIAL NO.	OUTLINE	DWG. NO.	* .	"一个"
	FULL LOAD TORQUE			· · · · · · · · · · · · · · · · · · ·	
	STARTING TORQUE				and the second
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	INSULATION				
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	COUPLING FURNISHED BY				
	WEIGHT.			.	
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			• ••	_	
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Job No. 4140 Spec. B-7131-L-1 Page 10 of 12 July 30, 1956 CATALYTIC CONSTRUCTION CORev. #1 - 8-13-56 ENGINEERING DIVISION MOTOR Date:

MOTOR DATA

Furnace - Forced Drai N Building No. 81-1 Continuous		SHE	NO. 4140 ET NO. 419-284	
DUIRED ORE (1)	•	BY		
•	PERFORMA	NCE		
•	FULL LOAD	75% LOAD	50% LOAD	
EFFICIENCY PERCENT				-
POWER FACTOR PERCENT				
	MOTOR SP	ECIFICATION		
MOTOR TO B	E FURNISHED IN ACCORDAN	CE WITH SPECIFICATION	N NO.4100-N-19	
MANUFACTURER				
RATED H. P.		VOLTS JI	O PHASE 3	CYCLES .
TYPE Totally E	nclosed - Fan Cool	ed		- UTULLU .
	·			1. T.
200000000000000000000000000000000000000	,		· · · · · · · · · · · · · · · · · · ·	
SYNCHRONOUS R. P. M.				• v 1
FULL LOAD R. P. M				
ALTITUDE				
FRAME NO.			•	F. 2. 3
SERIAL NO.	OUTL	NE DWG. NO		100
v		***************************************		
FULL LOAD TORQUE		,		
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Job No. 4140 Spec. B-7131-L-1 Page 11 of 12 July 30, 1956
CATALYTIC CONSTRUCTION CORev. #1 - 8-13-56

ENGINEERING DIVISION

	Furnace - Screw Fe	eder	JOB NO). <u>4140</u>		
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CATALYTIC CONSTRUCTION GO. Job No. 4140 Spec. B-7131-1-1 ENGINEERING DIVISION Page 11-A of 12

MOTOR DATA

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CATALYTIC CONSTRUCTION COMPANY PHILADELPHIA 2, PENNA.

Job No. 4140 Spec. B-7131-L-1 Page 12 of 12 July 30, 1956

VENDOR DATA REQUIREMENTS

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7. MANUFACTURER'S DATA AND/OR TEST REPORTS					4
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12. RECOMMENDED SPARE PARTS FOR ONE (I) YEAR NORMAL MAINTENANCE W/PRICES			4		
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General Notes:

- Pate and Dwgs, "For Approval" are required within two (2) weeks after order is placed.
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- (C) All date and dwgs, not heshoded in [A] and [E] are required within three (I) weeks efter order is placed

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NICHOLS ENGINEERING & RESEARCH CO

INTER-COMPANY CORRESPONDENCE

(INSERT) COMPANY CARBIDE AND CARBON CHEMICALS COMPANY LOCATION OAK RIDGE, TENN.

TO

Mr. C. H. Roddy

LOCATION

Engineering - 9739

ANSWERING LETTER DATE

July 23, 1953

ATTENTION

COPY TO

Mr. R. E. Hulme Mr. J. W. Minchey

File

SUBJECT

W. O. 540703 - Bldg. 8110

Nichols Engineering and Research Corporation

We are distributing information regarding subject order as follows:

Mr. C. H. Roddy - 2 ea. of Dwg. A-5405 - Calcine Bin, dated 6-4-53,

DATE

2 ea. of Dwg. A-5406 - Asbestos Cloth Dust Hood, dated 6-5-53,

2 ea. of Dwg. A-5409 - Feed Inlet Conversion, dated 6-16-53,

2 ea. of Dwg. A-5408 - Lower Gas Seal, dated 6-10-53,

2 ea. of Dwg. A-5411 - Feeder Base Plate, dated 6-18-53,

2 ea. of Dwg. A-5407 - Calcine Outlet Gate, dated 6-5-53,

2 ea. of Dwg. A-5403 - Furnace Shell Details, revised 6-22-53

and 2 ea. of Dug. A-5402 - General Assembly, revised 6-22-53.

Mr. R. E. Hulme and Mr. J. W. Minchey have already received their

copies of the above drawings.

W.R: vb

APPROVED FOR PUBLIC RELEASE

Technical in the

INSTRUCTIONS

FOR

NICHOLS HERRESHOFF MULTIPLE HEARTH FURNACE

SIZE 54" I.D. - 8 HEARTH

FOE

MASTER FILE

CARBIDE AND CARBON CHEMICAL COMPANY

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NICHOLS ENGINTERING AND RESEARCH COFFORATION

70 FINE STREET, NEW YORK, N.Y.

JULY, 1953

NICHOLS HERRESHOFF MULTIPLE MEARTH FURNACE

SIZE 54" I.D. 8 HEARTH

These instructions relate primarily to drying out, warming up, cooling down and lubrication of the furnace.

Detailed instructions for calcining operation are not included as sufficient information regarding the materials to be treated and the operations to be performed in the furnace was not available.

THE NICHOLS HERRESHOFF FURNACE

The furnace consists of eight circular refractory hearths, 54" diameter, placed one above another and enclosed within a cylindrical steel shell. Through the center of the hearths passes a rotating vertical shaft carrying arms to which are attached rabble teeth for stirring the charge and advancing it along the hearths.

The furnace is heated by combustion gases from gas burners, admitted through ports at selected hearths.

The materials to be treated are fed onto the top hearth by means of a motor driven star feeder, with 1.5 speed variation for regulation of the feed rate. The charge material passes into the furnace through a closed chute, forming a seal to prevent gas leakage through the feed opening.

Calcined product is removed through a drop hole in the bottom hearth to a chute with a control gate.

The charge feeds onto the top (No. 1) hearth at its periphery, is rabbled in toward the center and falls to No. 2 hearth through the drop hole opening between the inner rim of the hearth and the central shaft. On No. 2 hearth it is rabbled out to the drop holes at the periphery. The material is rabbled in this manner across each of the eight hearths, to be discharged from the bottom hearth through a single outlet. It passes through a sealed, gate controlled chute to a calcined storage hopper.

On odd numbered hearths the charge is rabbled in toward the center; these hearths are therefore called "IN" hearths. Even numbered hearths are "OUT" hearths. The rabble teeth on each hearth are set at a suitable angle to the axis of the arm to turn the charge in the proper direction.

The central shaft is supported on a step bearing below the furnace and is held in line by a bearing above the top hearth. It is driven through a bevel gear attached at the lower end. The bevel pinion shaft is driven by variable speed drive for varying the speed of rotation of the shaft. A shear pin in the drive is set to break if the arms meet with an obstruction.

At the top of the furnace the shaft opening is closed by a sand seal. Beneath the bottom hearth the shaft opening is sealed by means of a packed stuffing box. These seals should be checked daily and adjusted as required to prevent leakage.

The rabble arms, two on each hearth, fit into machined sockets in the central shaft and are retained by a pin. Pins and arms can be removed and replaced through the access doors, without cooling the furnace.

The central shaft is hollow, and is provided with passages for the continuous flow of cooling air, circulated by natural draft. If temperatures above 150°F should be employed, forced draft cooling by fan will be necessary. A cooling fan can be connected to the exhaust opening in the top of the shaft.

Lute caps attached to the shaft at each of the "CUT" hearths prevent leakage of charge material through the slight clearance opening between shaft and hearth.

Rabble teeth are separate castings provided with channel shaped sides which fit over the bottom flange of the arm. They are held in place by the outermost teeth on each arm, which are fastened with alloy pins. The blades are set at an angle to the longitudinal axis of the arm, the "IN" and "OUT" teeth being opposite hand.

Gases from the burners and from the material under treatment pass up through the drop holes counter current to the solid materials, and leave the furnace through the gas outlet on the top hearth.

LUBRICATION

Before starting up the equipment for the first time or after a long shut-down, every moving part must be thoroughly lubricated.

While the furnace is in operation, each lubrication points should be serviced on a regular schedule. These points are listed on the attached chart with the type of lubricant and servicing schedule. Motors and auxiliary

equipment should be lubricated according to manufacturers instructions.

DRYING OUT THE FURNACE

The brickwork must be thoroughly dried out and brought slowly up to operating temperature to prevent damage. Particular care is necessary at the initial starting as freshly laid brickwork has a high moisture content. The following instructions should be followed.

- 1. Inspect each hearth, removing any loose brick or other foreign objects.
- 2. Check all lubrication points.
- 3. Turn the shaft by hand for a full revolution to check clearance. Rabble teeth should clear the hearth by approximately one inch.
- 4. Start' furnace and fan by power, and operate them for sufficient length of time to be sure that all moving parts are in good working order.
- 5. Build small wood fires on the hearths. The process of drying out will take several days, since there is a good deal of moisture in the brick and it must be heated very slowly. It is almost impossible to make the fires too small at the start.
- 6. During the drying out period, turn the central shaft by hand every six or eight hours to be sure everything is working freely. Be sure that the wood fires do not come in contact with the rabble arms, rabble teeth or other metal parts, nor interfere with the rabble teeth.
- 7. Move the fires around to various parts of the hearths, so the brick will be heated uniformly.

WARMING UP THE FURNACE

After the furnace is thoroughly dried out it may be slowly heated to operating temperature. Start the lower-most gas burners very slowly to heat the furnace gradually and uniformly. In starting up, care must be taken to avoid an accumulation of combustible gas in the furnace. When opening a door the operator should stand at one side to avoid a possible flare out. Operators should wear face shields when looking into the furnace.

As each burner is lighted the operator should check to see that it is properly centered in the burner tile and that the flame passes through the center of the opening without impinging on the sides.

The temperature rise should not exceed 20°F per hour on the burner hearth for the first twelve hours. It may then be increased to 30°F per hour until the furnace has reached 1200°F. Thereafter the furnace may be brought up to operating temperature at the rate of 40°F per hour.

During the drying and warming up period the gas outlet damper will require adjustment at intervals to keep a minimum draft consistent with suitable temperature rise rate.

The central shaft must be kept rotating while heat is on the furnace, to prevent warping.

STAND BY

If the furnace is to be out of operation for a short time only it is advisable to hold it at standby temperature rather than to let it cool down to room temperature.

This is done by decreasing the burner heat slowly so that the temperatures drop about 30°F per hour, until only one burner on the lower hearth, at its lowest flame, remains on. By keeping a minimum draft on the furnace during this period it can be held at temperatures high enough to enable it to be brought back to operating temperature in a few hours, and with moderate gas consumption.

During standby periods the central shaft should be kept turning.

COOLING DOWN

If it becomes necessary to cool the furnace to room temperature, this should be done carefully and at not more than 30°F per hour temperature drop. Reduce the burner flames gradually. When the last burner is shut off reduce the draft to as close to zero as is possible without permitting fumes to escape into the room.

The central shaft may be stopped when the last burner is turned off.

SHUTTING DOWN THE FURNACE

1. Stop the feed to the furnace

- 2. Continue furnace operation until all material is discharged except the permanent bed.
- 3. Reduce the temperature as outlined under Cooling Down.
- 4. When the last burner is shut off, stop the central shaft.
- 5. Partially close the dampers as burner flame is reduced. This is very important for a slow cooling rate.

EMERGENCIES

POWER PAILURE

- 1. Stop the feed immediately.
- 2. Shut off the gas burners.
- 3. Open the doors to cool the furnace.
- 4. Before starting again, turn the central shaft by hand a full revolution.

STOPPAGE OF CENTRAL SHAFT

- 1. Stop the feed immediately.
- 2. Shut off the gas burners.
- 3. Determine cause of stoppage; examine all hearths and the drive.
- 4. If shear pin in drive has broken, replace after removing cause of stoppage.
- 5. Remove any excess feed under the feed opening.
- 6. Turn central shaft by hand a full revolution before starting motor.

The central shaft drive may meet with excessive resistance if the arms sag, permitting the teeth to penetrate into the permanent bed. Normally the rabble teeth clear the hearth brick by approximately one inch. This space between teeth and hearth fills up with charge material which remains in the furnace and is called the permanent bed.

After some time the arms may sag slightly, and the depth of this bed will be reduced. When it becomes less than 1/2 inch on any hearth the sagging arm should be raised or replaced.

The entire shaft and arm assembly can be raised a small amount to maintain the permanent bed, but care must be exercised to avoid raising the assembly so much that arms come in contact with the thermocouples.

EXCESSIVE TEMPERATURES

- 1. If due to too high a burner neat, reduce the flame.
- 2. If due to excess combustibles in the feed, cut off the feed until the temperature has returned to normal. Then start feeding again but at a lower rate.

GENERAL INSPECTION

- Each shift, check all bearings and drives, lubricating as required (see lubrication chart).
- 2. Inspect all hearths at least once a shift for foreign matter lodged in hearths or rabble teeth. Open up plugged drop holes, repair broken or warped arms or teeth.
- 3. Inspect burner boxes each shift. Remove carbon clinker. Boxes must be kept clean to prevent slagging or damage to brick.
- 4. Inspect and clear burners each week.
- 5. Check drive belts each week tightening if loose.
- 6. Clean out gas outlet duct each week.

LUBRICATION CLART

NICHOLS HERRESHOFF FURNACE, SIZE 54" I.D. - 8 HEARTH

•	FITTING	LUBRICANT	CHECK	REPTIL
Top Shaft Bearing	Zerck grease fitting	High temperature Every grease * Hours	Every 4 Hours	Each Shift
Bottom shaft	011 cup	S.A.E. #30	Each Shift	Change each
Speed Reducer	011 level plug	S.A.E. #40	Each Shift	Each 3 Months
Bevel gear	Paint with brush	Cup grease and graphite	Esch week	
Pinion gear	Paint with brush	Cup grease and graphite	Each Week	

^{*} Grease having melting point of about 600°F.

W. 6 herte 1 he all Background

SOLVENT ROASTER PROCEDURE

Y/HG-0362

In order to recover pure solvent from the solvent oxide which is formed in the trays of the Cascade, a roaster has been constructed at building 8110 in Y-12. In this roaster, the solvent oxide is heated with coke and is converted to metallic solvent at such a high temperature that the solvent leaves the furnace as vapor which is then condensed. The pure solvent is then returned to the Cascade.

is doubted that enough solvent oxide will be formed in the Cascade to necessitate full-time operation of the rose BROVED FOR PUBLIC RELEASE

II. Materials

following materials are used in the roaster operation. Office

Solvent oxide, called "ore", as removed from 9204-4. This material will also contain some pure solvent which will vaporize to be recovered, pieces of filter paper which will burn up, and water.

Coke. This coke will have to be crushed and sized to particales less than 3/4 inch. The coke serves to reduce the solvent oxide and to supply a portion of the heat to the roaster.

C. Sand is used in feed batches to prevent the wet ore's sticking to the hoist bucket and feed hopper. Sand after usage will collect in the calcine hopper and the dust collector hopper during operation, and may be returned to the sand hopper for re-use.

Natural gas is used as fuel.

Water is used in cooling the solvent as it falls from the condenser and as a scrubbing agent in the scrubber.

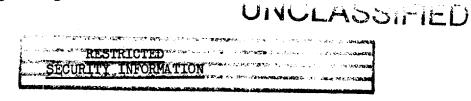
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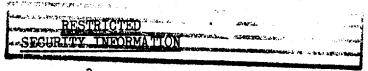
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III. Equipment

hearth to hearth.

- A. Furnace shell containing eight hearths; the two top hearths heated by heat from below, the four next hearths heated by gas burners, and two spare hearths at bottom. An arrangement of rabble arms, driven by drive motor D-882 at the bottom of furnace, moves the feed material from
 - B. Forced draft fan B-881 provides air to the burners for combustion of fuel gas.
 - C. Feed hopper and drive motor D-881 store the feed batches and continuously deliver feed to roaster furnace.
 - D. Bins H-881 is a bin with chute for delivering ore to skip hoist bucket. H-882 is a bin with chute for delivering coke to skip hoist bucket. H-883 is a storage box with hand scoop for moving sand to skip hoist bucket.
 - E. Skip Hoist 500 pound capacity bucket and track unit which moves feed batch from scales L-881, where batch is made up, to feed hopper, where batch is automatically dumped.
 - F. Cyclone Dust Collector collector with removable dust hopper for catching solid particles leaving the roaster in the flue gas stream.
 - G. Condenser four U-shaped air cooled condenser tubes in series, with outlets at the bottom of each U for passing solvent to collecting trough.
 - H. Trough H-885 located under condenser section, passes condensed solvent continuously to solvent receiving tank F-881. Water continuously flows through trough to cool solvent.

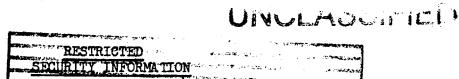




- I. Solvent receiver tank F-881 stainless steel tank with sight glass for catching solvent from H-885 until solvent is removed and transported to 9204-4.
- J. Induced air fan B-882 maintains vacuum on roaster and draws roaster flue gases through dust collector H-886 and the condenser section.
- K. Scrubber column packed with Rachig rings through which flue gas is passed counter current to water spray, the water flowing at 5 gallons per minute. Solvent collected in scrubber automatically drains from bottom into a container.
- L. Exhaust fan B-883 and stack flue gas is diluted with air and blown through stack where entrained water from scrubber settles out and drains to sewer.

IV. Safety Hazards USC

- A. The primary hazard is in the possible passage of solvent vapor from the equipment to the atmosphere. A number of safety features have been incorporated into the design of the roaster to cut down the hazard from this source. They are as follows:
 - 1. The roaster is designed to designed to operate under vacuum, so that in case of leaks, air will leak into the system instead of vapor leaking out.
 - 2. The gas supply will automatically be cut off in case of failure of the ventilating fans. This will stop the formation of solvent vapor soon after the fan stops.
 - 3. All solvent normally exposed in the open will be covered with water.
 Solvent spills will take priority over all other work and must be cleaned up immediately.



B. Secondary hazards are in (1) the danger of burns from the hot sections of the equipment, especially the roaster, the dust collector, and the first part of the condenser, and (2) the danger of strains in trying to move too large loads of the very heavy solvent and solvent oxide.

V. Operating Procedure

- A. Solvent oxide, coke, and sand will be brought to the roaster by truck. They may be loaded directly into the proper storage bins. Solvent oxide will be transported in 55-gallon drums; pure solvent will be transported in regular solvent dollies.
- B. Batches will be weighed out as follows:

Sand 37.6 pounds

Coke 15.5 pounds

Ore 346.9 pounds

The 400 pound batch will then be delivered to the feed hopper. The "A" shift will load the hopper with 5 feed batches, which should supply the roaster for a full day's operation.

C. Hourly checks will be made to make dertain all equipment is operating, and that flows are normal.

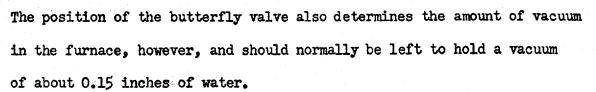
Air flow will be checked by analysis of flue gas by means of Orsat apparatus as described in "Orsat Apparatus Procedure".

A very small amount of excess air (uncombined oxygen) is desired in the flue gas, and this will be controlled by adjusting the damper on forced air pump B-881.

Feed rate will be controlled in conjunction with the butterfly valve setting between B-882 and the scrubber to give an operating flue gas temperature of about 900° F. as it leaves the roaster. For too low a temperature the feed rate may be lowered or the butterfly valve partially closed.

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The flow rate of water through trough H-885 should be sufficient to hold a temperature of 100° F. or lower at the point where the water leaves the trough. The water rate to the scrubber should be constant at about 5 gallons a minute as determined by the flow meter in the water line.

The rotation rate of the rabble arms should be the maximum speed which will give calcine completely free of solvent from the bottom of the roaster.

Gas rate will be controlled at each hearth to give a maximum temperature of about 1300° F. on hearth 6 with a temperature gradient up the furnace with a temperature of about 900° F. at the flue gas exit from the furnace.

VI. Start-up Procedure

During start-up, equipment will be turned on in the following order:

- 1. Water flow to trough H-885.
- 2. Water flow to scrubber.
- 3. Induced air fan B-882.
- 4. Exhaust fan B-883.
- 5. Furnace drive motor D-882.
- 6. Forced draft fan B-881.
- The burners will be lit.
- 8. The gas rate will be adjusted to give a temperature rise of about 100°F. per hour in furnace. When the temperature of the exit flue gas reaches 900° F., start the feed hopper motor D.881.

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9. Control temperature at some point above 750° F.

VII. General Shut-Down Procedure

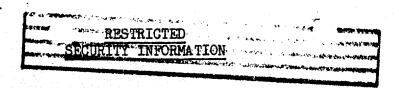
- A. During routine shut-down, the following steps will be taken:
 - 1. Shut off feed motor D-881.
 - 2. Shut off fuel gas completely, closing solenoid valve manually.
- B. When roaster temperature drops near outside temperature, proceed as follows:
 - 1. Shut off forced draft fan B-881.
 - 2. Shut off furnace drive motor D-882.
 - 3. Shut off exhaust fan B-883.
 - 4. Shut off water to scrubber.
 - 5. Shut off water to trough H-885.
 - 6. Shut off induced draft fan B-882.

VIII. Emergency Shut-Down Procedure

In case of emergency, such as the breaking of a line carrying solvent vapor or any other condition which would admit solvent vapor to the atmosphere, the feed motor D-881 should be stopped, the fuel gas and forced draft fan B-881 should be stopped, and the area evacuated, leaving the rest of the system operating.







SOLVENT ROASTER OPERATING INSTRUCTIONS

I. Start-up Instructions

A. Initial steps

- 1. Seal the solvent line between the solvent received tank F-881 and the condenser trough H-885 by pouring enough clean solvent into the trough to bring the solvent level in the solvent line just to the bottom of the trough.
- 2. Fill the condenser trough H-885 with water and leave the valve at that setting which will give about 3 gallons a minute water flow through the trough. This valve setting will be determined during the initial testing of the roaster. Check to make sure that this water overflows at the south end of the trough to the sewer line and does not flow through the solvent drain line.
- 3. Seal the lower drain line on the bottom of the gas scrubber by pouring a small amount of clean solvent into the line.
- 4. Open the valve in the water line to the scrubber and by observing the flow indicator located near the inlet to the scrubber, adjust the water rate to the scrubber to approximately 5 gallons per minute.

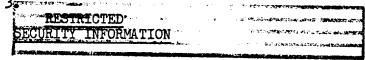
 Check to make sure that this water flows through the upper drain line at the bottom of the scrubber to the sewer.
- 5. Open the butterfly valve on the gas line at the top of the scrubber to the 3/4 open position.
- 6. Start the induced draft fan B-882 (which draws air from the condenser.



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- 7. Open an inspection port near the bottom of the furnace and allow air to flow through the system.
- 8. Start the exhaust fan B-883 at the stack.
- 9. Start the furnace drive motor D-882 and adjust the motor speed so that the rabble arms rotate at about 1/2 speed. The exact motor speed will be determined during initial roaster operation, and that speed will be used during all operations.
- 10. Check the following items:
 - a. Valve on line between cyclone dust collector H-886 and dust hopper should be open.
 - b. Flange on line above dust collector should be sealed.
 - c. The two sampling connections located near the top of the scrubber, one on the gas line into the scrubber and the second on the gas line leaving the scrubber, should be plugged.
 - d. The valve on the drain line from the solvent receiving tank F-881 should be closed.
- 11. Make certain regulating valve in gas line nearest the furnace is closed.
- 12. Activate the solenoid valve in the gas line by starting the forced draft fan B-881 at the bottom of the furnace.
- 13. Prepare a lighting torch by bending two loops in a four foot piece of #8 wire; one loop will be a handle, the other will be wrapped around a small quantity of oily waste.
- 14. Open inspection ports in the furnace at hearths 3, 4, 5, and 6. Light the torch and insert it through the inspection port to the burner on hearth 3.
- 15. Open the regulating valve in the gas line and the burner valve at hearth 3



- 16. Start the burner on hearth 3, then move down and start hearth 4, then hearth 5, then hearth 6.
- 17. Close all inspection ports tightly.
- 18. Start the L & N recording potentiometers to record the furnace temperature rise on the strip chart. Adjust the gas rate to the hearths (with the regulating valves at the hearths) to give a temperature rise of about 100° F. per hour on the hearths.
- 19. Adjust the butterfly valve in the gas line at the top of the scrubber to give a vacuum of about 0.15 inches of water.
- 20. Open the valve in the water line entering the solvent receiver tank

 F-881 and allow the water level to rise about an inch above the

 bottom of the sight glass. Close the valve.
- 21. While the furnace is warming up, batches of feed may be prepared and dumped into the feed hopper.

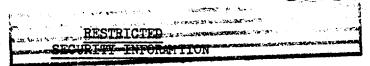
B. Preparation of Feed Batch

- 1. By using the "reverse" button, lower the skip bucket on the track until its full weight is supported by the platform of the scale L-881.
 Determine the tare weight of the skip bucket.
- 2. Using the hand scoop, weigh into the skip bicket 37.6 pounds of sand from hopper H-883; spread the sand over the bottom of the bucket.

 The amount of sand required may vary with the dampness of the ore.

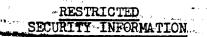
 Enough sand should be used to prevent the sticking of ore to the skip bucket and feed hopper.
- 3. By forcing the lever arm down, raise the door of the ore (solvent oxide) hopper H-881 and allow 175 pounds of solids to pour into the bucket.

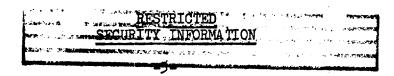
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- 4. Close the ore hopper door, open the coke hopper H-882 door, and allow 15.5 pounds of coke to pour into the bucket. (The coke should have been previously sized to less than 3/4 inch lumps.)
- 5. Close the coke hopper door, reopen the ore hopper door, and drain 172 more pounds of ore into the bucket. Close the ore hopper door.
- 6. By pressing the "start" button on the skip hoist, the skip bucket will be carried to the top of the feed hopper and will dump automatically.
- 7. By pressing the "reverse" button, return the skip bucket to the scale platform.
- 8. Dump at least two batches of feed into the hopper before starting feed to the furnace.
- 9. When the temperature of the gas leaving the furnace reaches 900° F., start the drive motor D-881 on the feed hopper. Start the feed in as slowly as possible and gradually increase the feed rate to that rate selected during initial operation of the roaster.
- carefully; it should not be allowed to fall below 750° F. In case it starts falling, cut the solid feed rate back as much as necessary to keep the temperature above 750° F. When the coke in the feed begins to burn, the temperature of the flue gas will start increasing; when this happens, lower the gas rate to the hearths. The temperature of the flue gas should be controlled at about 900° F. The maximum temperature in the furnace should be on hearth 6 and should be about 1300° F.







- 11. Uniform operating conditions will not prevail until:
 - a. Solvent flows from the condenser.
 - b. Uniform temperature conditions prevail.
 - c. Feed rate is constant.
 - d. Fuel gas flow rate is constant (at about 97.5 cubic feed per hour).
- II. Instructions for Normal Operating Conditions
 - A. Preparation of feed batches
 - 1. The day shift will make up 5 batches and dump them into the feed hopper. the 5 batches should last 24 hours.
 - 2. Batches will be made up as follows:
 - a. By using the "reverse" button, lower the skip bucket on the track until its full weight is supported by the platform of the scales L-881. Determine the tare weight of the skip bucket.
 - b. Using the hand scoop, weigh into the skip bucket 37.6 pounds of sand from hopper H-883. Spread the sand over the bottom of the bucket. The amount of sand may vary with the dampness of the ore; enough sand should be used to prevent the sticking of ore to the skip bucket and feed hopper.
 - c. Raise the door of the ore hopper H-881 and allow 175 pounds of solids to pour into the bucket.
 - d. Close the ore hopper door, open the coke hopper H-882 door, and allow 15.5 pounds of coke to empty into the bucket.
 - Note: This coke must be in 3/4" lumps or smaller. Before storing in the hopper, the coke should be crushed and sized.
 - e. Close the coke hopper door and add 172 more pounds of ore from hopper H-881 to the bucket.



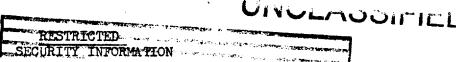
f. By pressing the "start" button on the skip hoist, the skip bucket will be carried to the top of the feed hopper and will be dumped automatically.

B. Periodic Checks

- 1. About once a day, on "B" shift, close the calcine gate at the bottom of the furnace, loosen the clamp on the asbestos hood above the waste trap H-884; remove the trap and empty the solids into the sand bin H-883. Replace the trap, tighten the asbestos cover, and open the calcine gate. Save about 100 cc of the calcine material for spec analysis.
- 2. About once a day, on "B" shift, close the valve between the cyclone dust collector H-886 and the dust hopper, open the flange above the dust hopper, and dump the solids in the hopper into sand hopper H-883.

 Replace the dust hopper, tighten the flange connection, and reopen the valve above the dust hopper.
- 3. About once a shift, analyze a sample of the flue gas in the gas line leaving the top of the scrubber as described in "Orsat Apparatus Instructions". If the carbon monoxide content is found to be above 0.1% in the flue gas, increase the amount of air passing through the furnace by slightly opening the damper on the forced draft fan B-881. If the oxygen content is found to be above 0.1% in the flue gas, decrease the amount of air passing through the furnace by slightly closing the damper on the forced draft fan B-881.
- 4. Every two hours check and record the following:
 - a. Temperature of discharge water from condenser trough H-885.

 Adjust water flow rate so that this temperature is 100° F.

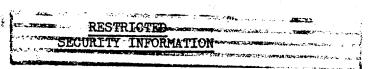




- b. Flow meter reading on water to scrubber (approximately 5 gallons per minute).
- c. Induced draft fan B-882 (on off).
- d. Position of butterfly valve between condenser and scrubber.
- e. Forced draft fan B-881 (on off).
- f. Damper position on forced draft fan B-881.
- g. Exhaust fan B-883 (on off).
- h. Damper position at exhaust fan B-883.
- i. Pressure on furnace should be a vacuum of 0.15 inches of water.
 Adjust by butterfly valve setting between condenser and scrubber.
- j. Hearth temperature (degree F.) for four hearths.
- k. Feeder D-881 speed (RPM).
- 1. Receiver tank F-881 sight glass reading (inches).
- m. Production rate (pounds solvent per hour as determined by tank F-881 calibration chart).
 - n. Fuel gas rate (cubic feet per hour).
- 5. Every day, during "C" shift, drain solvent from F-881 into a tared portable dolly for removal to Beta-4. Obtain a gross weight of the filled dolly and determine the net weight of solvent removed.
- C. General Records

Record, as necessary:

- Weight of sand, weight of coke, and weight of ore in each batch to the feed hopper.
- 2. Total weight of batch and batch number.
- 3. Time batch was dumped.
- 4. Weight of product solvent (from section B, item 5, above).



- 5. Weight of sand, weight of coke, and weight of ore delivered to the roaster, with time of delivery.
- 6. Weight of solvent from the scrubber.
- 7. Weight of solvent sent to Beta-4.

III. Scheduled Shut-Down For More Than Two Days

- A. In shutting down, a negative pressuremust be maintained on the furnace until it has cooled to air temperature to prevent harmful solvent vapors escaping to the atmosphere.
 - 1. Shut off feed motor D-881.
 - 2. When the exit flue gas temperature drops to 700° F, shut off the fuel gas completely.
 - 3. Manually close the solenoid valve in the fuel gas line.
- B. After the furnace hearths have cooled to within 50° of the outside temperature, proceed as follows:
 - 1. Shut off forced draft fan B-881.
 - 2. Shut off furnace drive motor D-882.
 - Shut off exhaust fan B-883.
 - 4. Shut off water flow to scrubber.
 - 5. Shut off water flow to condenser trough H-885.
 - 6. Shut off induced draft fan B-882.
 - 7. Remove and empty dust hopper. Replace hopper.
 - 8. Clean up area.

IV. Instructions For Short Shut-Down

- 1. Shut off feed motor D-881.
- 2. When solvent completely stops falling into trough H-885 adjust the fuel gas to maintain a flue gas temperature of about 750° F.

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- 3. Turn water flow off of trough H-885 and scrubber.
- 4. Turn off drive motor D-882.
- 5. Leave all three fans B-881, B-882, and B-883 on.

V. Start-Up After Short Shut-Down

- 1. Turn on drive motor D-882.
- 2. Turn water flow on trough H-885 at normal flow rate.
- 3. Turn water flow on scrubber at about 5 gallons per minute.
 - 4. Raise fuel gas rate to give flue gas gas temperature of 900° F. where the gas leaves the furnace.
 - 5. Start feed motor D-881.
 - 6. When the coke begins to burn, as seen by increasing temperature in the furnace exit flue gas, cut down on the flow of fuel gas to maintain an operating temperature of 900° F. in the furnace exit gas.

VI. Safety Precautions

- A. The major hazard at the solvent roaster is in the passage of poisonous solvent vapor to the atmosphere. To hold this hazard to a minimum, the following steps have been taken:
 - 1. The roaster is designed to operate under a slight vacuum so that gases would leak in rather than out.
 - 2. The condenser trough, the solvent receiving tank, and the solvent container at the scrubber, should always be partially filled with water.
 - 3. A solvent vapor meter, which indicates solvent vapor concentration in the air, has been obtained and should be used frequently as a check. The meter may be used in locating the source of solvent vapor if traces are found. Instructions for the use of this instrument will be on the instrument.

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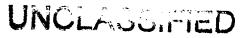
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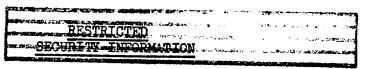
- 4. Solvent spills are to be given first priority and should always be cleaned immediately.
- 5. During operation, the furnace, the flue gas lines, and the condenser will be very hot. Extreme care should be taken to prevent burns.
- 6. Solvent and solvent oxide are very heavy materials and care should be taken to avoid strains.

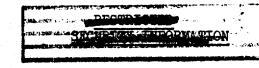
VII. Emergency Procedure

In the event of a failure or leakage in any vapor line, or any other condition which would allow solvent vapor to excape to the atmosphere, the following procedure will be followed:

- 1. Shut off feeder motor D-881.
- Shut off gas to furnace.
- 3. Shut off forced draft fan B-881.
- 4. All other equipment should be left operating.
- 5. Evacuate the area.







ORSAT APPARATUS PROCEDURE

information a fecting the hational of ension of the United states within the meaning of the espionage laws, Title 194, the transmission or reveletion of which in any mappier to an unauthorized person is prohibited by law.

"This mate:

I. Background

During operation of the solvent roaster, it becomes necessary to periodically analyze the flue gases leaving the roaster to determine whether or not the proper amount of excess air is being admitted to the roaster. For performing this analysis, an Orsat apparatus is located at the roaster.

II. Equipment

The equipment consists of a graduated tube with a leveling bottle containing mercury and the following three absorption pipettes:

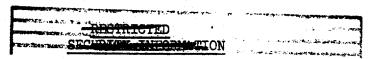
- Pipette for carbondioxide (CO₂) absorption, which contains concentrated potassium hydroxide.
- 2. Pipette for oxygen (02) absorption, which contains alkaline pyrogallol.
- 3. Pipette for carbon monoxide (CO) absorption, which contains cuprous chloride.

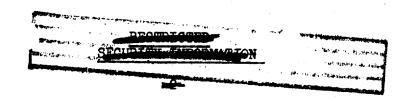
III. Procedure

- A. By lowering the leveling bottle, the mercury level in the graduate falls and gas can be drawn into the graduate from the sampling point.

 The sample is then discharged to the atmosphere, and the procedure repeated twice again, flushing the graduate out with the flue gas.
- B. After the sample is obtained in the tube (with a volume of exactly 100 ml.), it is passed in and out of the first pipette (for CO₂ absorption), three times. The volume of the remaining gas is read and the per cent CO₂ determined. This step is then repeated on the second pipette where the per cent O₂ is determined, and the third, where the per cent CO is determined. The volume of gas remaining in the graduate gives the per cent nitrogen (N₂) in the sample.

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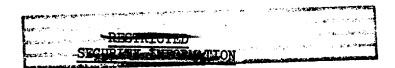


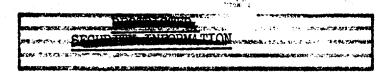


III. Safety Hazards

All three solutions used in the apparatus are strong reagents and should be handled with care.

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ORSAT APPARATUS OPERATING INSTRUCTIONS

I. Preparation of Sample

- A. Check all lines to make certain they are tight.
- B. Check each of the three absorption pipettes to make sure the level of liquid in each pipette is exactly even with the calibration mark on the pipette inlet line. If the level is off, open the stopcock on the pipette inlet line and adjust the level by very slowly raising or lowering the leveling bottle.
- C. Have the surface of the mercury in the measuring graduate just covered with clean water.
- D. Draw sample into measuring graduate as follows:
 - 1. Close valve between measuring graduate and sampling line.
 - 2. Open stopcock in end of header passing over the absorption pipette.
 - 3. By gently raising the leveling bottle, bring the top of the water over the mercury just to the zero calibration mark.
 - 4. Close stopcock in end of header.
 - 5. Open valve between graduate and sampling point..
 - 6. Slowly lower leveling bottle until the water level exactly reaches 100 ml. calibration mark.
 - 7. Repeat steps 1 through 6.
 - 8. Repeat step 7.
 - 9. Close valve between graduate and sampling point.

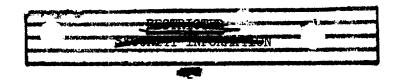
II. Analysis of Sample

A. Open stopcock to first absorption pipette (which should contain strong KOH).

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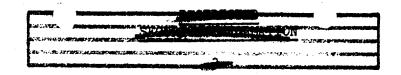
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revelation of which in any manner to unauthorized person is prohibited by I



- Raise leveling bottle until water level comes just to zero calibration mark. Be careful not to allow water or mercury to get into header or absorption pipette.
- Lower leveling bottle until liquid level in absorption pipette just reaches calibration mark on pipette inlet line. Be careful not to allow any pipette solution to enter header or measuring graduate. In case any does carefully take equipment apart, wash all contacted pieces thoroughly in water, put all apparatus back together, and start over.
- D. Repeat steps B and C. .
- Repeat step D. E.
- Close stopcock to absorption pipette. F.
- G. Read level of water in graduate to nearest 0.1 milliliter. Subtract this figure from 100. The result is the percentage of CO2 in the sample. (Example - level reading equals 82.0 ml. The CO2 percentage then equal 100 minus 82.0 = 18.0%.)
- Open the stopcock of the second absorption pipette (which should contain H. alkaline pyrogallol). until value heromes constant
- Repeat steps B and C above
- J. Close the stopcock to the absorption pipette.
- Read the level of water in graduate to the nearest 0.1 milliliter. K. Subtract the reading from the water level reading obtained in step G. The result is the percentage of 0, in the sample. (Example - level reading equals 81.8 ml. The 0, percentage then equals 82.0 minus 81.8 = 0.2%.)
- L. Open the stopcock to the third absorption pipette (which should contain Cu₂Cl₂).





- M. Repeat steps B and C above three times.
- N. Close the stopcock to the absorption pipette.
- O. Read the level of water in the graduate to the nearest O.1 milliliter.

 Subtract from the reading obtained in step K. The result is the

 percentage of CO in the sample.

 (Example level reading equals 81.7 ml. % CO equals 81.8 minus 81.7

 equals 0.1%.)
- P.. The volume reading found in step N is equal to the percentage of N_2 in the sample (in the example, this would be 81.7%).

III. Safety Hazards

Hazards are presented by the chemicals used in the absorption pipettes. The liquids in the CO₂ and O₂ pipettes contain concentrated caustics, and the liquid in the CO pipette contains concentrated acid. In case these solutions contact the skin, immediately flood the contacted area with water.

IV. Refilling Pipettes

After continued use of the Orsat Apparatus it will be necessary to throw away the pipette solutions and refill the pipettes. (The alkaline pyrogallol in the O₂ pipette will turn dark drown very rapidly. This coloring does not mean that the pipette should be refilled.)

- 1. Very gently disconnect the pipette.
- 2. Pour out old solution.
- 3. Wash out pipette thoroughly with water.
- 4. Turn pipette upside down and allow to dry.
- 5. Refill pipette with proper solution.
- 6. Carefully replace pipette.

UNCLASSIFIED



Sludge burner analyses 1957-1959

Y/HG-0/Subnumber

Sludge burner stack loss of solvent. Letter report: Morehead to Whitson,
June 18, 1957. Includes 6 air analysis reports for samples taken from March
27 to June 12, 1957. 7pp.

169/2 Analysis of sludge burner water. Letter: Gwinn to Morehead, July 23, 1957.

1p.

169/3 Sludge burner calculations for air flow for January 9-10, 1958.

169/4 Air analysis for samples taken on July 15, 1958.

169/5 Creek water analyses.

169/5 Four analytical reports on Lab. Req. 817321 for Morehead, September 22, 1959. 5pp.

INTER-COMPANY CORRESPONDENCE

UNION CARBIDE NUCLEAR COMPANY

A Division of Union Carbide and Carbon Corporation

To:

W. K. Whitson

Bldg. 9201-4

Plant:

Y-12

Date:

June 18, 1957

D. A. Jennings Copies To:

File 🗸

Subject:

Sludge Burner Stack

loss of Solvent

Y/HG-0169/1

At the request of D. A. Jennings and Leo J. LaFrance, samples were taken from the stack of the Sludge Burner to determine solvent loss and health hazards. Below are the results of these samples, before and after revision of the exhaust and condenser.

	Date of Sample	Avg.stack volume	grams per hour	everage gra		ram <u>loss</u> er day	
" sludge fied ce seed 30 min puict to completion" puict to completion?	4-18-57 4-18-57 4-18-57	1300 CFM 1300 CFM 1300 CFM	.25 .65 .37	. lı2	15.6 1	0.08	20 min Simple time
ore senser	5-6-57 5-6-57 5-6-57 5-6-57 5-6-57 5-6-57	1300 CFM 1300 CFM 1300 CFM 1300 CFM 1300 CFM 1300 CFM	.17 .43 1.30 1.05 .09	. 66	4.1 10.3 31.2 25.2 23.3 23.3	5 . 84	lcfm 1300 cfm 4"dism.
	After Re	rision					
	6-12-57 6-12-57 6-12-57 6-12-57 6-12-57	1300 CFM 1300 CFM 1300 CFM 1300 CFM 1300 CFM	.30 .144 .96 .81 1.13 .57	•70	19.4	16.8 0.16	
-m. 2.	Bark	BLIC RELEAS			mes J.	Morehead	
Technical I	nformation (0ffice Date 6-17-59 6-17 6-17	93 1.07 ,72	Indust	F. Moreb rial Hyg il Depart	iene Section	
	JFM:emm	6-17	.73	, O-1			

This form for Inter-Company Correspondence only

.89

.72

WCX-163 (8-55)

JFM: emm

6-17

6-17

normal feed rate-no smoke

hifeed rate-

9 min.

	Attn.	To
File	J. D. McLendon	L. J. LaFrance, Y12RC

The following air samples were taken to determine the concentrations of solvent being exhausted from the solvent salvage facility exhaust stack at Building 8110.

	~											
·		ω		2.	-	CON		3	2		1	Sample No
		Averag	ceased comple	The ad	Diamet	COMMENTS:		11.	=		4-18-57	Date of
	,	Average stack volume = 1300 cfm.	ceased 20 - 30 minutes prior to completion of the sampling time.	The addition of sludge to the furnace	Diameter of stack (14").			See Sample No. 1	See Sample No. 1	the outlet	In center line of stack at	Location of Sample
				And the same and t				14:44	14:20	13:42		Tin Start
	·			and the company of the second				15:04	14:40	14:02		Time of Sample
				* * * * * * * * * * * * * * * * * * *				20	20	20		nple Total Min
				1				-	1	1		Rate cim
				A CONTRACTOR OF THE PROPERTY O				20	20	20		Total Vol.3
				Commence of a last world half on a figure and don't				94	166	65		Con- taminant ug/Hg
				4	·			.37	,659	. 269		Results
				1				2	2/2	h		

GBA/eb

Inspector C. M.

Anal d by

Stack volume = 1360 cfm 78,000 cf hr 1,872,000 of day 65 mg Hg/20 cm ft 3.254 gg/h 6.08 graf day 166 pg 16/20 cm ft / am ft 2 . 648 g hy/hr 15.5 g hy/day 94 mg 48/20 cm ft 4.7 pg Hg/cuft. 8.8 g Ho/day

	Att.	To
File	J. D. McLendon	L. J. LaFrance, Y12RC

The following air samples were taken to determine the levels of mercury in the effluent stack being exhausted from the solvent salvage facility.

						-				
								Burning carbon while sampling.	urning c	·
								One condenser not in operation.	ne conde	2. (
										1
									COMMENTS:	сом
	·									
	١	< 10	1	1	T 8 T	1	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	See Sample No. 7	=	œ
		14	E = 5	ï	1 6	3 B 1 2 B		BLANK	**	7
	. 93	239	20	panal .	20	14:55	14:35	See Sample No. 1	11	6
	,09	22	20	-	20	14:31	14:11	See Sample No. 1	=	5
	1.05	268	20	_	20	14:08	13:48	See Sample No. 1	11	4
ang .66.	1.30	333	20	 	20	13:43	13:23	See Sample No. 1	11	ω
	.43	109	20	-	20	13:20	13:00	See Sample No. 1	=	2
	. /7	43,	20,		20	12:50	12:30	outlet		
	9/h							Center line of stack at the	5-6-57	}
	Results	Con- taminant µg_of.Hg.	Total	Rate cim	Sample Total Min.	Time of S	Start	Location of Sample	Date of Sample	Sample

GBA/eb

Inspector C. M. West

Special Tection

2.15 17 12 30 50 5.45 .43 1200-20 # 1 43 #2 109 16.65 1.301323.43 F2 333 13.40 1.05 1348 26 268 #4 1.10 -09141/43, 22 #5 11.95 :9343555 #6 239 - 7 Blank . 055 14 #7 Blank -# 8 <10 takery / 5/6/57 12:30 <> 255 1300 cuft/m 78000 cuft/hr

...

<u>.</u>

-

AIR ANALYSIS

To J. F. More head y-12 RC Attn. J.D. MCKendow

The Following Ain Som plus were Taken tevels of Mercury In Ethlant Stack From The ドセベルナメ.

	-	-	_	 _									
				•	8	7	9	ر د	H	\sim	b	/	Sample No.
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							14:34 14:54	W:13 14:33	13:52 14:12	13,30 13,50		12	Time
						1	14:54	IH:33	14:12	13:50	13:04		Time of Sample
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				The state of the s	0	0	0.54/	2900	2075	247.5	112.5	77.5	Con- taminant
				A company of the second			. 67	1.13	.81	,96	44,	9,30	Results
											i de presentados		

Inspector_

Analyzed by

Remarks

Remarks

Remarks

16.89 day

16.89 day

istomus)

... 1. D. dmotes it stack 14," 5. Assidge Stack volume =

Att. J. D. McLendon J. F. Morehead, Y12RC

mercury in the effluent stack at the solvent sludge facility. The following air samples were taken to determine the levels of

	1		1		T ~	7	7	_								
9	*		3	2.	1.	COMI		8	7	6	5	4	ယ	2	H	Sample No.
1/12	7/12	Ÿ.	Furn	Feeding	Burn	COMMENTS:		"	=	3	=	11	=	=	6/17/57	Date of Sample
Stack	stack	uccal	се уасишту	furnace	Burning graphite			BLANK	BLANK	See Sample No.	See Sample No	See Sam	See Sample No.	See Sample	Center line	Loca
not smoking	Smoking		Furnace vacuum/range: 0.46 - 0.	at approximately	in furnace while					ole No. 1	ple No. 1	Sample No. 1	ple No. 1	ple No. 1	ine of stack	Location of Sample
7	9:26		0.54 inches	30 min.	sampling			8 8 1 1 1	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	14:25	14:01	13:40	13:16	12:53	12:25	Start
9:55			of water	intervals	ů.			## ## ep ep ep	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	14:45	14:21	14:00	13:36	13:13	12:45	Time of Finish
q	9							l I	1 5	20	20	20	20	20	20	Sample Total Min.
'	,							!	î .	 	-	3-1]1		—	Rate C.f.m
9	9							1	1	20	20	20	20	20	20	Total
210	330							167.5	0	185.0	227.5	187.5	185.0	275.0	237.5	Con- taminant #g_of Hg.
										.72	,84	.73	.72	1.07	. 93	%esults
73.3	36.7×						N.			9.13	11.4	9.4	9.2	13.75	11.9 qu	

GBA/eb

Inspector. C. M. West

Analyzed by

Special T

173 - 93

esting Lab

	Attn.	To
File	J. O. McLendon	L. J. LaFrance, Y12RC

Burning of Solvent contaminated combustible material at Y-12 Burning Ground.

JSB/eb

Inspector C. M. West

Analyzed by

Jim

No. 1 was taken in smoke re; smoke very heavy; anged the direction of the requently.

m Morehea

																				_
BY:	SIGNED:			رد مهر	7.00	GRAM U /GRAM	ANALYSIS I	AT DT A	ASSAY REQUESTED	1 // 00	The maleral of	Hamilian M	DESCRIPTION OF MATERIAL:	BUILDING NO.		REPORT TO:		BATCH NUMBER R	·	_
DATE				3/0/mg-	2 20 holy		REPORTED ANSWERS	AT CODE NO.		my	Media	Dan		/	PHONE: 77/C	Thompson	1	REQUISITION NUMBER	010400	_

INT COMPANY CORRESPONDENCE

Burner

UNION CARBIDE NUCLEAR COMPANY

A Division of Union Carbide and Carbon Corporation

To:

John Reece

Bldg. 2201-4

Plant:

Y-12

Date:

January 17, 1958

Copies To: Ton

Tony Caputo

File

Subject:

Building 8110 Stack Loss

Air Samples were taken at the Sludge Burner exhaust stack to determine the average solvent loss per cay.

The following results were made using a traverse figure of 1225 cubic

feet per minute velocity.

Date	Time	Samle	ug Hg/ft.	g Hg/day	Average
1-9-58	1:30-2:40 P.M. 2:45-3:45 P.M. 3 10:40 A.M 3:2	1 2 OPH 3	2.35 10.10	7.l3 4.15 17.02	9.80 g Hg/day

James J. Morehead Industrial Hygiene Section Medical Department

JFM: emm

7-15-58

1) probe Sinsifer 4.5
5.2
7.7

J.82g/d avg.

1300 cfm

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Conditions/Remarks:

OAK RIDGE Y-12 PLANT INFORMATION CONTROL FORM

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(2090-1H-9)			
Author(s) Requestor: Steve Wiley			
TYPE: Formel Report Informal Report	Progress/Status	Report Co-Op Repor	Thesis/Term Paper
Oral Presentation (identify meeting, sponsor, loc		-	
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APPROVED FOR PUBLIC RELEASE

Technical Information Office Date

SOLVENT AIR - SLUDGE BURNER

To J. F. More head The Following Stack Samples were taken at Building - To determine the Amount of Hg. giving of From the recovery process.

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							8		7	le xxx	5 xxx	k k //	x X X	ال ×	>	Sample No.		
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ح	cal Inform	2 800	WED FO			1-6			7		"		inside S		vside S	Location of Sample		
	Technical Information Little		R PUBLIC			were					, ,		Stack		inside Stack (Probe)	Sample		
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Much									·		4.43	2000	703	3.67	272			1200
كرا	~	***								1) III	Y hw					Sim	Will

Analyzed by_

1.728 = 7.69 pm/24h.

1.728 = 7.69 pm/24h.

1.728 = 7.69 pm/24h.

1.728 = 8.829 pm/24h.

Solvent air - sludge burner - Building 8110 1957, 1959

Y/HG-0/Subnumber

172/1 Recommendations for sludge burner from health standpoint. Letter: Morehead to Jennings, August 28, 1957. 1p.

172/2 Sludge burner readings. Twenty-four data sheets, January-December 1959.

INTER-COMPANY CORRESPONDENCE

UNION CARBIDE NUCLEAR COMPANY

A Division of Union Carbide and Carbon Corporation

To:

D. A. Jennings Bldg. 9201-4 Plant:

Y-12

Date:

August 28, 1957

Copies To:

Dick Brothers

Subject:

Recommendations for Sludge Burner from Health Standpoint

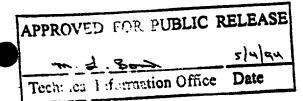
Y/HG-0172/1

1. All cracks should be sealed in the concrete floors around the area.

- 2. The tile floor in the office, toilet and eating area should be removed or cleaned a minimum of once per shift with "clerex" or NaClO and water. Special emphasis should be placed for clean-up on Saturday and Sunday. This area will be more hazardous with the doors closed during cool weather.
- Install sprinkler pipes around the perimeter of the concrete slabs to maintain a constant wet surface and reduce the mercury vapor-pressure.
- h. Engineering should be asked to design some type of alarm system to prevent blow-outs from the furnace.
- 5. Personnel should refrain from placing contaminated gloves and other equipment in the lockers or other facilities should be provided for storage of coffee, sugar, etc.
- 6. Fans should be made available to dispel the contaminated air in the vicinity of the desk. Natural ventilation is not adequate at all times.

Mr. James F. Morehead Industrial Hygiene Section Medical Department

JFM:FW:emm



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get dury Sq shoots conditioned higher sed

INTER-COMPANY CORRESPONDENCE

UNION CARBIDE NUCLEAR COMPANY

A Division of Union Carbide and Carbon Corporation

To:

Mr. J. F. Morehead

Building 9706-2

Plant:

Y-12

Date:

July 23, 1957

Copies To: W. A. Pfeiler

V. C. Jackson

File, Y-12NoRC

Subject:

Analysis of Sludge Burner

Y/HG-0169/2

The effluent water from the sludge burner which discharges into Poplar Creek was sampled on July 10, 1957. The first sample was taken during a typical discharge and the second sample was taken after the deposited sediment had been stirred up thoroughly. The flow rate of the stream was measured to be approximately 40 gallons per minute. The solids were separated from the solution with a centrifuge and the mercury content in each phase was measured on the mercurometer. The results are tabulated below.

Sample	Mercury in Solution (µg/ml)	Mercury in Solids (µg/ml)
Normal discharge	4	8
Stirred discharge	10	190

It will be noted that the major portion of the mercury content is located in the solid phase. It would therefore seem that a sedimentation pit would be a logical manner for decontaminating the discharge water.

VCJ:fd

12 pg/ml 40 gel/min 1200cpg/L 151 L/min 1.8 g/min 5.7/8/1/day

APPROVED FOR PUBLIC RELEASE

chnical Information Office Date

Sludge Burner

Tome total page 45 123 page 3 g/day

1-9-58 1:30-240FM 236 56 4.21 7.43

I

1-9-58 2:46-3:45PM 113 48 2.35 4.15

II

1-10-58 10:40-3:207M 3071 304 10.1 17.82

avg 9,80g/da

Y/HG-0169/3

APPROVED FOR PUBLIC RELEASE

1494

Sechnical Information Office Date

LPHN-4 LUXILLARY INVENTORY 5-1-52

Feed solid solution in storage 9201-5: 4.721 gals. or 691 Lbs. salt

135 drums Feed solids on hand 9 drums Extract solids on hand

Jludge on hand. 42 drums Dirt screened 73 drums 400 drums Dirt not screened - about

Joivent delivered to 9201-4 from 01-10, from 1-1-62 50 5-1-62

		Cond.	Decant	Total
January		22.744	0.314	29 . 050
Tebruary		32.619	13.312	75.931
March		39.505	43,003	ú2.50u
_pril		12.762	41.077	27.752
Total Tor	Year .			225.233

Anthracite added to feed filters 5-2-62 as follows:

G-211-1) 51.0 Bags (1 G-211-2) - 20.5 Bags - ji2 --20. Dags //3 1. Bag 12.5 Bags 76 Total 13.0 Bags

.nthracite on hand 250 Bags "1.

Activated carbon on hand -- 100 drums coroximate weight - 145 lbs. WG 10-30.

Pillows plexiglass 16 drums - size 5/8" x 1".

Stored-in Bldg. 9720-1 🐭

IR 120 Cation 49,336 1bs. 265 1bs. per drum = 5 cu. ft.

lC lbs..per drum = 5 cu. ft.

M-54

UNION CARBIDE

NUCLEAR DIVISION

INTERNAL CORRESPONDENCE

W 172 0000

OST OFFICE BOX Y- OAK RIDGE, TENNESSEE 37830

December 7, 1070

Date

December 7, 1970

To (Name)

Mr. V. B. Gritzner

Division

Location

Building 9201-5

75

Originating Dept.

Answering letter date

Subject

Mercury Recovery

Copy to

D. W. Smith J. N. Turpin

J. S. Klobe (NoY-12RC)

*3,5000

A preliminary investigation of Building 81-10 was made by John Turpin on December 4, 1970, to determine the condition of the equipment and the inventory available for processing. This will be followed by a more detailed Engineering estimate initiated by Mark Grim. The results of this investigation are as follows:

There is an estimated 1,200,000 pounds of feed stored in 1600 drums at the site. Almost all drums are open. About 3% of the drums are unsound.

Based on past experience:

 $\frac{1 \text{# of Hg.}}{20 \text{# feed}} \times 1.2 \times 10^6 \text{#/feed} = 60,000 \text{# Hg.}$ (est.)

1162

Hg. Wt. Estimate Decomposer graphite - 500 drums ; 20# Hg./drum

Dirt and gravel - 200 drums - 10# Hg./drum

e Sludge and filter cake - 500 drums - 20# Hg./drum
Solids, salt, and carbonates - 400 drums - 20# Hg./drum

(Based on D. W. Smith's letter of 7-14-66: 81-10 inventory = 75,000# Hg.)

LABOR (This is estimated with a fairly large contingency)

Electrical - 120 Man-days

Relamp, replace four cubicles in motor control center, remove and replace 10 motors, rewire control panel, remove and replace 15 electrically operated valves and all new wiring for N-H roaster. Replace miscellaneous switches, wire, receptacles, etc.

Instrument Mechanic - 80 Man-days

Calibrate control instruments; install thermocouples, flame rods, control valves for N-H roaster. Repair and adjust instruments in central control room tune system.

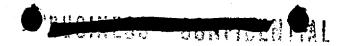
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APPROVED FOR PUBLIC RELEASE

P. K. M. House Technical Information Office

Date

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Comment with be distributed at meeting No Yes	<u> </u>	6-0263	2366000 3	9/8/95
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INTERNAL CORRESPONDENCE

NUCLEAR DIVISION

POST OFFICE BOX Y, OAK RIDGE, TENNESSEE 37830

To (Name)

Mr. R. D. Williams

Division Location

Building 9212

Date

March 12, 1971

Originating Dept.

Answering letter date

Subject

81-10

Copy to

J. R. Barkman

M. S. Grim

V. B. Gritzner

H. A. Keen

J. S. Klobe

R. J. McAlister

D. W. Smith

J. N. Turpin (NoY-12RC)

Work is in progress to transfer all of the mercury-contaminated materials stored at 81-10 into sound drums. The main objective of this work will be to prevent mercury contamination of the local environment and prepare the materials for either long-term storage or sale to an outside buyer.

It is estimated that about 1200 man-hours direct labor will be required to transfer and consolidate the 1600 open drums into about 1200 closed drums. We will probably purchase about 600 drums with lids and an additional 600 lids and clamps. About 600 of the existing drums would be reusable if they had covers. All drums should be suitable for safe handling and truck shipment.

A minimum of 200 man-hours of maintenance labor will be required to provide water, electricity, drinking fountain, toilet facilities, equipment modification, scales repair, and air sampling stations.

The recommended available equipment that may be used consists of the following:

- 1. 3000# fork truck
- 2. Drum squeezer
- 3. Fork truck with drum handling attachment
- 4. Drum dumper
- 5. One screener
- 6. Miscellaneous hand tools (shovels, hoes, mattocks, crow bar, pliers, wrenches, hammers, screwdrivers, sledge hammer, water hoses, mercury containers, vacuum cleaner, brooms, dust pans)

- SIMPLE MINAL

from	2. A. Swith 2. A. Pluhar Jim Sykes		UNION \RBIDE PURCHASING DIV P. O. BOX M OAK RIDGE, TEN Area Code: 615	VISION
SUBJECT			2-30-71	Reply Message
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RECIPIENT RETURNS THIS COPY TO SENDER

droplets of mercury metal. It contains less than 5% ash and is combustible. The graphite ranges in a size of egg and smaller, but nothing less than 2-mesh. Three random samples of the carbon were submitted to the Plant Laboratory for mercury content and they were reported as being 20%, 22%, and 30% by weight.

Carbonate Filter Solids. This is a moist to dry mixture of lithium carbonate, lithium hydroxide, and finely divided mercury. It is mostly fusible lithium hydroxide and lithium carbonate with about 20% water. This material would probably melt in a roaster. Two random samples were submitted to the Plant Laboratory for mercury content and they were reported as being 2.4% and 11.1% by weight.

Process Filter Solids. This is a process filter cake which contains finely dispersed mercury in a cake of miscellaneous dirt, sludge, lithium carbonate, and about 10% ash. These solids were found to be heavily contaminated with mercury but a practicable method to separate the mercury was not found. Decanting and de-sludging were attempted but were not very successful. Three random samples were submitted to the Plant Laboratory for mercury content and they were reported as being approximately 30%, 40%, and greater than 50% by weight.



UNION CARBIDE CORPORATION

NUCLEAR DIVISION

P. O. BOX M, OAK RIDGE, TENNESSEE 37830

Gentlemen:

The Company (Union Carbide Corporation, Nuclear Division) has available for sale 1274 drums of Government-owned mercury contaminated material described below. The material is to be purchased by the bidder; that is, recovered mercury is not to be returned to the Company.

	Drums	Gross Weight	Approx.Mercury Content		
Material	(55 gal.)	(lbs.)	8	Pounds	
Carbon	534	296,820	25	74,205	
Carbonate Filter Solids	252	83,160	6	4,990	
Process Filter Solids	104	76,237	40	30,495	
Process Sludge	156	98,945	14	13,852	
Sump Sludge	156	72,410	3.7	2,679	
Mixed Rock, Dirt, Sweeps, etc.	72	44,259	8	3,541	
Total	1,274	671,831		129,762	

Carbon. This coke-like graphite is fairly dry and is saturated with very fine droplets of mercury metal. It contains less than 5% ash and is combustible. The graphite ranges in a size of egg and smaller, but nothing less than 2-mesh. Three random samples of the carbon were submitted to the Plant Laboratory for mercury content and they were reported as being 20%, 22%, and 30% by weight.

Carbonate Filter Solids. This is a moist to dry mixture of lithium carbonate, lithium hydroxide, and finely divided mercury. It is mostly fusible lithium hydroxide and lithium carbonate with about 20% water. This material would probably melt in a roaster. Two random samples were submitted to the Plant Laboratory for mercury content and they were reported as being 2.4% and 11.1% by weight.

Process Filter Solids. This is a process filter cake which contains finely dispersed mercury in a cake of miscellaneous dirt, sludge, lithium carbonate, and about 10% ash. These solids were found to be heavily contaminated with mercury but a practicable method to separate the mercury was not found. Decanting and de-sludging were attempted but were not very successful. Three random samples were submitted to the Plant Laboratory for mercury content and they were reported as being approximately 30%, 40%, and greater than 50% by weight.

Process Sludge. This is a wet slurry cake of miscellaneous solids, including grease and oil. It contains about 60% water and accumulations of rust and dirt. The mercury is finely divided and cannot settle out. It probably includes about 15% ash. All of this material was decanted and run through the de-sludger with significant quantity of mercury being recovered. Two random samples from the desludged material were submitted to the Plant Laboratory for mercury content and they were reported as being 10.3% and 18.6% by weight.

Sump Sludge. This is a wet slurry of very fine non-metallic sedimentary sludge, having a dispersion of mercury throughout. The gross weight includes about 60% water. It probably includes about 15% ash. Two random samples were submitted to the Plant Laboratory for mercury content and they were reported to be 1% and 10% by weight.

Miscellaneous Rock, Dirt, Sweeps, etc. (Mixed). This material is a somewhat non-homogeneous mixture of floor sweeping compound, gravel, paper, fine wire, dirt, and other miscellaneous materials containing a finely dispersed quantity of mercury. It is usually fairly dry and includes about 85% ash.

In his recovery process the successful bidder must comply with all State, Local, and Federal Regulations applicable to air and water pollution. Prior to entering into a contract the Company will require evidence in the form of permits or other documents which indicate that the responsible Government agencies have reviewed and approved the successful bidder's recovery operation.

At the present time we are considering sale of the material under one of the following described arrangements. Both of these have disadvantages. We solicit your recommendations involving other arrangements under which the material can be sold or provisions under which the designated problem areas can be resolved.

ARRANGEMENT I. Sale of the material on the basis of recovery of contained mercury at a price per pound for mercury recovered. The problems associated with this arrangement are two-fold:

- (a) The difficulty of evaluating bidder's method of recovery to reflect variations in yield possibilities. We understand in the retort recovery method 99% of the contained mercury can be extracted.
- (b) The second problem involves accounting. As this material is Government-owned, it is necessary to positively account for all mercury which is recovered. At this time it appears that a Company representative would have to check the operation at the work site 100% of the time. This is expensive. From your experience perhaps you can suggest other methods of accounting which will satisfy strict auditing requirements.

ARRANGEMENT II. Sale of all the material on a unit price per pound basis, with delivery to be made upon written notice from Purchaser in lots of 30,000 to 35,000 pounds (truck-load lots). Both parties to the contract would have the right to cancel any undelivered quantities by giving written notice at any time. This arrangement entails considerable risk. The risk is minimized somewhat for the Purchaser in that he is buying in truck-load lots and can cancel should he find recovery of mercury

Page 3.

falling below his expectations. For the bidder's pre-bid evaluation, this arrangement would involve delivery of samples of the material selected by the Company as directed by the bidder. Bidders would be charged for the samples at rates mutually agreed upon. We will appreciate any comments you have regarding Arrangement II, your ideas regarding sampling of the material, the quantity you would expect to receive in a sample, and a fair price which you would expect to pay, FOB Oak Ridge, Tennessee, for the sample.

If you are interested in bidding on this material, we will appreciate receiving your reply to this letter by September 15, 1971.

Please indicate your estimate of the time required to recover mercury under a contract using your process.

Yours very truly,

Sales Office Government Property

DRMcCammon/mm



INTERNAL CORRESPONDENCE

E You Into Whote & Return

RECEIVED

4.4

NUCLEAR DIVISION

SEP 2 | 00 PH 17 POST OFFICE BOX Y, OAK RIDGE, TENNESSEE 37830

Liklobe

R.D. WILLIAMS

To (Namo) Mr. D. M. Smith

Division
Location Building

Copy to

Building 9201-5

V. B. Gritzmer ≺

File (NoV-12RC)

Dato August 27, 1971

Originating Dept.

Answering letter date

subject Core Samples 81-10 Area RECEIVED
AUG 27 1971 5 E

Core samples were taken at three locations in the immediate vicinity of the 81-10 hercury salvage facility on August 25-27, 1971. Individual samples of one to two feet were taken of the same location to a depth of 6 to 14 feet. The samples showed that mercury exists underground near the 81-10 facility. The results of the sampling are given below. No analytical results were taken.

(3) 81-10 FACILITY (1)

1 8 ft. 1 ft.
2 13-1/2 ft. 1 ft., 1-1/2 ft.

RESULTS

Between 3 and 5 feet slight amounts of mercury were evident.

Very slight amounts of mercury were evident in the top foot. The 2nd foot showed no evidence. At 3-1/2 feet very slight evidence was found. Between 4 and 2=1/2 feet no evidence was noticed. At 9 feet mercury was very much in evidence. There was no mercury at 10-1/2 feet. At 12 feet mercury was again very evident. From 12 to 13-1/2 feet down the evidence of mercury dissipated to nothing at 13-1/feet.

3 6-1/2 ft. . 1 ft., 1-1/2 ft.

No evidence whatsoever of mercury.

P. D. Guettner



INTERNAL CORRESPONDENCE

NUCLEAR DIVISION

POST OFFICE BOX Y, OAK RIDGE, TENNESSEE 37830

To (Name)

Mr. V. B. Gritzner

September 21, 1971 Date

Division

Building 9201-5 Location

Alpha-5 Processing Originating Dept.

Answering letter date

Copy to

R. D. Williams File (NoY-12RC)

Subject

Building 81-10 Core Samples

The composited core samples from the general area at Building 81-10 were analyzed and the following results were reported:

Sample Location	Req. #	% Hg by Weight
South of storage pad #1	354273	0.014
North of furnace area in drainage ditch #2	354274	0.052
North of storage pad #3	354275	0.020

If any further details are desired, contact the writer or J. N. Turpin.

DWS: sa

PAGE 1 OF 2

TIPES OF STUDGE ON DEC. 16, 1970 A.D. DUNCAN, COU WITH THE HS REINC SEPARATED FROM THE SLUDGE THIS SLUDGE Kitosb 0 SLUDGE 99,402 WHEN COOLED. PERATION ESTIMATES/ N. BOW & E. H. Johnson FURNACE ESTIMATE RECOVERED GRASS WEIGHT OF OF PURE HS CHULD BE RECOVERED. WOULD BE FILTERED FOR 130,000. FUCINEARING. 70 FROM THE 0051-Hs VERTICAL FURNACE PURE SLUDGE SINCE DECIG 1970, COST ESCALATION IS ESTIMATED RECOVERY 671.831# 17 15 THEREFULE AN ENGINEERING 274 DRUMS DF THRU A VERTICAL mmm 1 800T OLIO TOTAL CUST WOULD BEINS PIODO されが 20002 N TIMPHED ON THE VAPOR MOLTI- HAARTA, WAS MADE COCATAD N AND BASIS OF BY RIM KEMPER LAB

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Condition -1274 drums stored at BHg. 81-10 671831 Shart Buch wight 99 400 its Hg.

Cost to repoir by facility = "150,000 a 1.50/sh Spending Costs - 200,000 - 2,000

Out of Porket Cost_

1,50/et cepting - (40% of facent)

2.30/et

Approx, Value, Contained Hy - 1270,000 (2.70/ce)

11 Recommy Cost - 230,000 (2.30/lb)

Pifference - 40000

I we can get \$40,000 or Mar [see



NUCLEAR DIVISION

INTERNAL CORRESPONDENCE

Y/HG-0057/28

January 22, 1982

D. E. Brashears, 9736, MS-1

Removal of Building 81-10 and the Mercury Recovery Facility

The request has been made for Industrial Hygiene to assess the extent of mercury contamination in Building 81-10 and to make recommendations on its demolition and removal.

Background information reveals this facility to be grossly contaminated. On January 21, 1982, Industrial Hygiene conducted a survey of the following location and found the airborne concentration to exceed the scale on the mercury meter.

- 1. Cracks in concrete slab of Building 81-10.
- 2. All drain lines.
- 3. Sump pit.
- 4. Valve north of furnace.

It is Industrial Hygiene's understanding that the entire structure is to be removed. Considering the above sampling results and background information on operation of the facility, the industrial hygiene recommendations for the subject removal include the following:

- When removing piping from the recovery facility, prepare to catch and contain significant amounts of residual mercury. Special considerations should be given the large condensing columns.
- 2. Break and remove all concrete slabs.
- 3. The sump pit contains water and must be contained before removing concrete pit.
- *4. Remove soil approximately 3-4 ft. in depth under all slabs and within 10' parimeter.
 - 5. Fill with uncontaminated soil or gravel.
- **6. Remove asphalt and approximately 5-8' of soil under the facility.

y war

D. E. Brashears Page 2 January 22, 1982

- 7. Remove all drain lines and valves.
- 8. The drain line under the road leading to the holding pool should be opened and filled with concrete.
- Remove water from holding pool and decontaminate pool (should pool not be removed).

*Excavating below this depth for mercury is usually not cost effective.

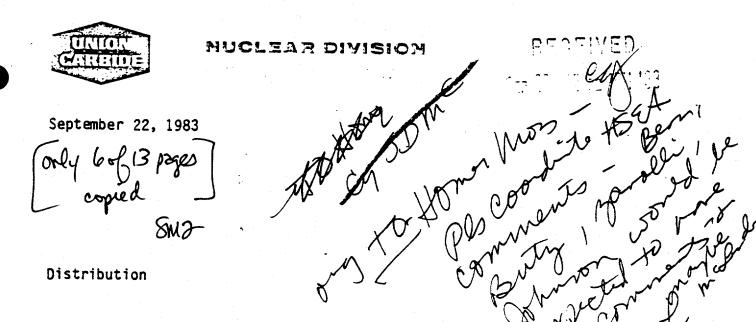
**NE of the furnace, the soil was removed to this depth and asphalt replaced it in order to eliminate seepage through the mound.

All material removed from the area should be disposed of as contaminated. Special checks can be made for those items with questionable contamination. Industrial Hygiene will conduct sampling surveys during demolition and will have additional personal protective recommendations for operating personnel.

Should you have any questions concerning this matter, please call 4-1594.

G. L. Bean, 9706-2, MS-2 (4-1594) Industrial Hygiene Group

GLB:sc cc: Fille - GLB - RC



Stripping Plan for Building 81-10

Enclosed is a draft of the Stripping Plan for Building 81-10. Building 81-10 will be stripped as a pilot project to develop criteria and methods for the stripping of Alpha-4. The current start date for stripping Building 81-10 is November 1, 1983.

Please review this plan and return comments to J. S. Anderson, Building 9201-5, MS-4 by October 7, 1983.

F. V. Tilson, 9201-5, MS-4

FVT:JSA:ssa

Enclosure: Draft - "Stripping Plan for Building 81-10 Mercury Recovery

Roasting Furnace"

Underwood -See zeur responsablece, such as og 12. -Pla pervide comments, on on 10/0483

Distribution Page 2 September 22, 1983

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DRAFT NO. 1 Page 1 September 20, 1983

STRIPPING PLAN FOR BUILDING 81-10 MERCURY RECOVERY ROASTING FURNACE

1

INTRODUCTION

Plans are being formulated at this time to strip and dispose of the process equipment located in Building 9201-4 of the Y-12 Plant. This equipment was used in the Lithium Isotope Separation Process in the late 1950's and early 1960's. Bulk mercury was removed from the equipment in 1977, and the columns were flushed with water. The water was treated to remove mercury to required levels and discharged to the industrial ditch leading to New Hope Pond.

To assist in obtaining pertinent data and in developing methods to be used in the Alpha-4 stripping campaign, it is desired to proceed first with the stripping of Building 81-10 as a pilot project. This report presents the plan to be used for stripping Building 81-10.

FACILITY DESCRIPTION

The Building 81-10 Mercury Recovery Roasting Furnace was installed and operated from March 1957 through July 1962 to recover raw mercury from various filter sludges, sump and tank cleanings, and other waste materials generated in the Lithium Isotope Separation Processes. The original facility consisted of a vertical, eight-hearth Nichols - Hershoff furnace fired by natural gas; feed preparation and loading equipment; a condenser system; and other auxiliary equipment required to operate the furnace. Steel support structures provide access to the top of the furnace as well as support for various pipes, conduit, and other control equipment.

The process involved feeding mercury contaminated sludge mixed with crushed coke and sand to the top of the furnace. The coke aided in reducing mercury oxide and also supplied a portion of the heat to the furnace. The sand was used to prevent the wet sludge from sticking to the feed mechanism. Rabble arms driven by a motor at the bottom of the furnace moved the feed material across the top of each hearth. The hearths contained holes that allowed the feed material to pass down to the next hearth. As the material passed from hearth to hearth, it was burned to ashes; and the mercury was released as a vapor. The mercury vapor was fed through a condenser and salvaged as a liquid. The mercury was returned to the Lithium Isotope Separation Process, and the ashes were discarded as solid wastes.

STRIPPING PLAN

Assumptions

Based on the present Environmental Protection Agency (EPA) Regulations for Identifying Hazardous Wastes (40 CFR 261) and the Tennessee Hazardous Waste Management Rules (Chapter 1200-1-11), the definition of a hazardous waste is determined by the results of an Extraction Procedure Toxicity Test (leach test) performed on the waste material. Solid wastes may be classified as nonhazardous if the EP test results in mercury concentrations <0.20 mg/L. Preliminary tests made on various types of equipment in Alpha-4 indicate that most of the solid wastes fall into the nonhazardous category. Disposal of these wastes can be made in a demolition landfill or perhaps be sold to a licensed salvage dealer. 1

¹R. B. Bustamante, J. M. Napier, and P. F. Meredith, <u>Preliminary Report</u> Decontamination Recommendations of Building 9201-4, Y/DZ-68, March 1, 1983.

If the above guidelines are adopted, cleaning efforts on the equipment removed would probably be reduced to removing any visible mercury, sludge, and loose scale found during disassembly by mychanical means such as vacuuming, brushing, or scraping. This process would require disassembling the equipment to a point at which any visible mercury, sludge, or loose scale could be seen and removed. If these guidelines are not adopted and more stringent guidelines result, more extensive cleaning methods will have to be developed. These methods would probably involve complicated mechanical and/or solution cleaning. The effluents would have to be treated to remove the mercury prior to discarding. All materials stripped from Building 81-10 will thus be stripped as outlined in the following sections of this plan and stored until the final sampling plan, disposal guidelines, and disposal methods are determined.

Stripping Requirements

- 1. All drains will be sealed with removable plugs during stripping activities to prevent a loss of mercury to the creek. These drains will be opened during off shifts to allow rainwater to drain. Underground drain lines will not be removed or decontaminated at this time. Visible mercury and sludge will be removed from drain openings and sumps both during and at the end of the stripping activities.
- 2. All types of insulation materials will be checked to determine if asbestos is present. All insulation will be removed prior to stripping any equipment. All insulation will be identified, placed in plastic bags, placed in drums, and stored for eventual disposal.

- 3. All materials will be cleaned by mechanical means such as vacuuming, brushing, or scraping. An attempt will be made to keep liquid cleaning methods at a minimum to avoid having contaminated water to treat for disposal.
- 4. All paint chips, rust, scale, sludge, and sweepings will be loaded in plastic bags, placed in drums, and discarded with drums of like materials now awaiting disposal in Alpha-4. All water used for cleaning will be retained for disposal at Alpha-4.
- 5. Decisions concerning the best place to remove or disassemble the equipment will be made jointly in the field by Maintenance and Operations supervisory personnel.
- 6. Equipment not in direct contact with the process materials and not suspected to contain visual mercury will be stripped first. Examples are electrical conduit and wires, motors, electrical controls, water and natural gas lines, and safety shower and eyewash stations. Equipment in direct contact with the process materials or equipment suspected of containing mercury will be removed last. Examples of this type equipment are the furnace, the slurry making and loading equipment, and the off-gas and condenser system.
- 7. As the equipment is stripped it will be cleaned, separated, and stored in three piles under the shed. One pile will contain equipment where no visible mercury was found and that was not in direct contact with the process materials. The second pile will contain equipment that was in

direct contact with the process materials but which contained no visible mercury. The third pile will contain equipment in which visible mercury was found.

Stripping Operations

Since the stripping operations involved with this project require continuous field decisions to be made, a detailed stripping procedure governing the removal and cleaning of each piece of equipment is not practical to write. Only the generalized procedure that follows, which is governed by the requirements stated in this stripping plan as a whole, is therefore the procedure that will be used in this particular effort.

Process operators will perform all cleaning activities and all sorting, packaging, and storing activities. Maintenance craft personnel will do the actual stripping of equipment. Other Plant support groups such as Utilities, Industrial Hygiene, Health Physics, Safety, and Engineering will provide services as requested by Operations supervisory personnel.

Generalized Procedures

- 1. All drains will have temporary plugs installed.
- Utilities and electrical services to the equipment will be deactivated by the appropriate Plant group.
- Insulation material will be removed, cleaned, and packaged for disposal in plastic bags and drums.

- Equipment not in direct contact with process materials will be removed,
 cleaned, sorted, and stored.
- 5. Remaining equipment will be removed, cleaned, sorted, and stored.
- 6 Drain openings and sumps will be cleaned.
- 7. The pad areas and adjacent shed area will be cleaned.

Abnormal Conditions and Personnel Training

Major abnormal conditions are not anticipated; however, all personnel will be thoroughly trained in all phases of the stripping operation, including the proposed work and job assignments, the potential hazards, and the protective measures to be used. The training material is documented in the "Health and Safety Training Instructions for Mercury Stripping Operations."

HEALTH AND SAFETY CONSIDERATIONS

Mercury Hazards

Toxicity - Mercury and its compounds may be absorbed through the skin, the gastrointestinal tract, and the lungs. The principal hazard is by inhalation, but skin absorption must be taken into consideration when evaluating the overall hazard. The adverse effects of mercury absorption have been investigated by many researchers and are well documented.

Acute poisoning has the symptoms of tightness in the chest, difficulty in breathing, coughing, and pain in the chest. In chronic poisoning, psychic and emotional disturbances are characteristic: fine tremors may affect the

PROJECT SUMMARY

ARCHEOLOGICAL AND HISTORICAL REVIEW (AHR) FOR BUILDING 81-10 DEMOLITION, Y-12 PLANT

PROPOSED ACTION: The U. S. Department of Energy Oak Ridge Operations Office (DOE-ORO) proposes to demolish Building 81-10 at the Y-12 Plant. The building structure, which consists of an open shed with a roof supported by wooden columns, would be removed and the concrete foundation would be left intact. No ground-disturbing activities would be associated with the proposed action.

LOCATION OF ACTION: The proposed action would take place at the Y-12 Plant on the DOE Oak Ridge Reservation in Anderson County, Tennessee (Fig. 1). Building 81-10 is located at the intersection of "G" Road and Third Street in the south central portion of the Y-12 Plant (Fig. 2).

DISCUSSION: Building 81-10 is an approximately 90-foot-long by 30-foot-wide open storage shed structure with a roof supported by wooden columns and a partial masonry wall at its east end. The building was originally constructed in 1943 as a tin shop and subsequently modified in 1957 to house a mercury roaster. In the later 600 the mercury roaster was removed from the building, after which the building was used to temporarily hold mercury-contaminated soil. Its use as a temporary mercury-contaminated soil holding area was discontinued in the early 1980s, and the building has not been used since (see Table 1 for a comprehensive list detailing the chronological events at Building 81-10). Some of the support columns have been damaged or have deteriorated, portions of the roof and gutters are loose and unsecured, and the structure has been deemed to be unsafe for occupancy or use. DOE-ORO has determined that it is not practicable to implement alternatives to the demolition of Building 81-10 (such as adaptive use) in accordance with Section 111(a), 16 U.S.C. § 470h-3(a), because the structure is surplus and poses a considerable safety hazard to personnel due to a lack of structural stability. Photographs of Building 81-10, shown in Figs. 3 through 9, have been taken as a record of the existing site conditions at and around the structure. The proposed action would take place in a developed area and would not involve ground-disturbing activities.

DETERMINATION: DOE-ORO, pursuant to 36 CFR 800.4(c) and in consultation with the State Historic Preservation Officer (SHPO), has determined that Building 81-10 is eligible for inclusion in the National Register of Historic Places (National Register) and therefore has determined that the proposed demolition of Building 81-10 would have an adverse effect on a historic property that is eligible for inclusion in the National Register. In addition, DOE-ORO has determined the proposed action would have no effect on any archeological sites, relics, or structure included in or eligible for inclusion in the National Register.

APPROVED

Technical Info

MARCH 18, 1995

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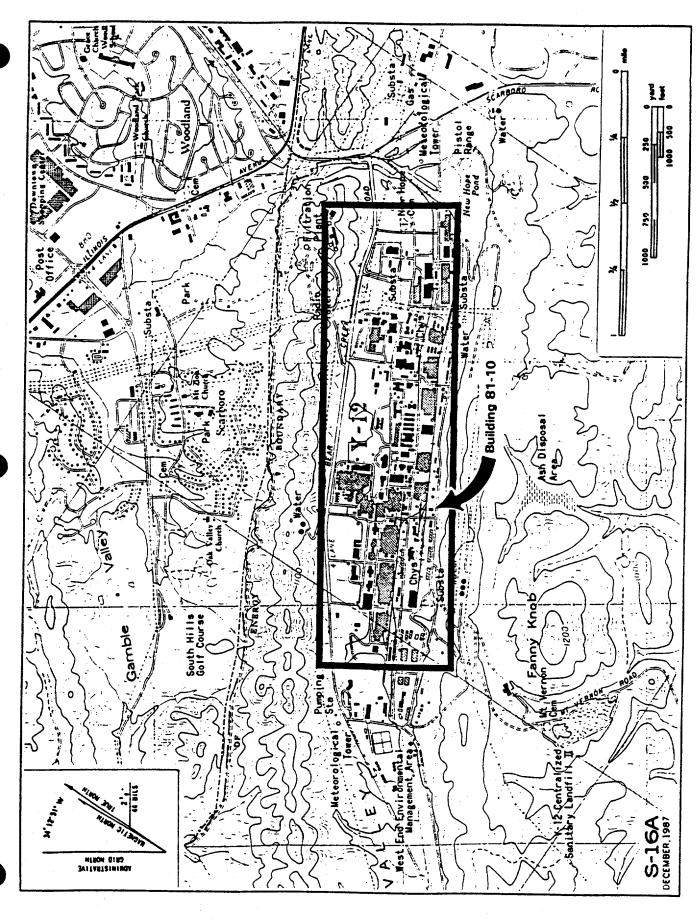


Fig. 1. Location of the Y-12 Plant on the Department of Energy Oak Ridge Reservation.

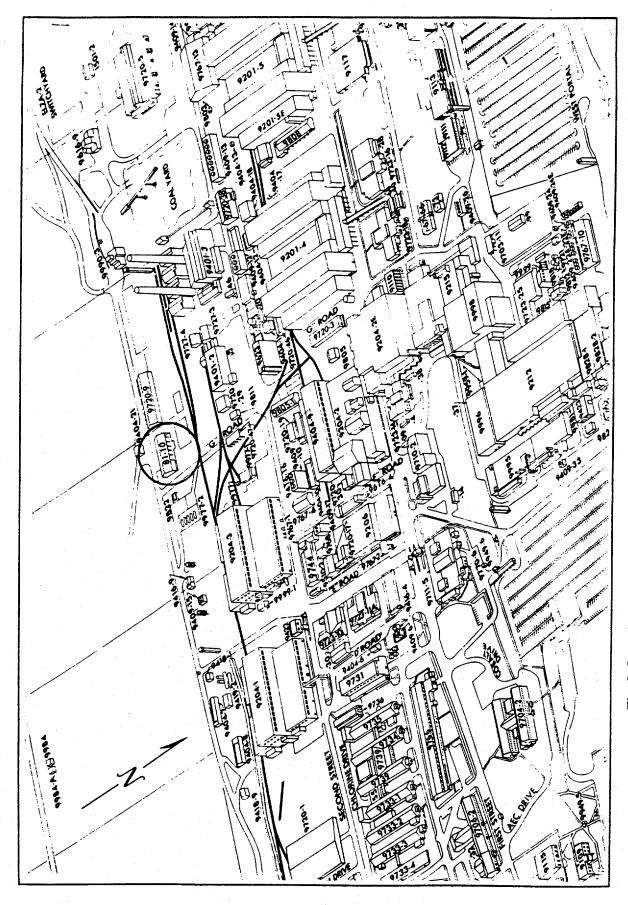


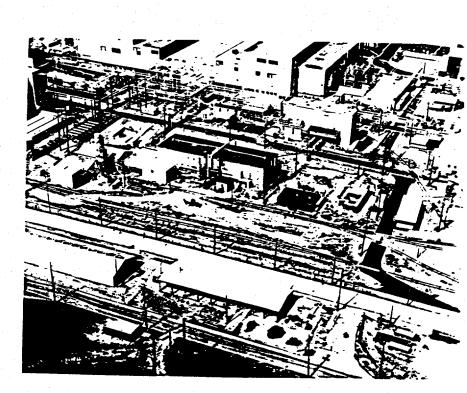
Fig. 2. Location of Building 81-10 in the south central portion of the Y-12 Plant.

Table 1. Chronological events at Building 81-10.

Year	Events
1943	Building 81-10 was constructed and used as a tin shop. The building was constructed over the original East Fork Poplar Creek channel. The creek channel was moved to the north of Building 81-10 and left as an open ditch until it was filled sometime between 1958 and 1963.
1957-1962	Building 81-10 was used for the operation of a mercury roasting furnace (mercury vapor extractor) that recovered mercury from sludges, wastes, contaminated soils, scrap from dismantled equipment, and other similar materials used at the Y-12 Plant (Union Carbide, 1983). During this time, soil from spills that occurred at Building 9201-2 between 1951 and 1955, some from the ramp area north of Building 9201-5 on July 17, 1956, and soils from an area between Building 9204-5 and 9201-5 in mid-1956 were processed at Building 81-10 (Comprehensive Environmental Response, Compensation, and Liability Act Phase II Report, January 1988).
1962	Mercury roasting furnace operation ceases (Wiggins, 1988a) (Y/TS-412).
1971	Building 81-10 and its sump were cleaned to secure the mercury-contaminated materials and recover loose mercury. An estimated 91,451 kg of mercury was removed from Building 81-10 and its sump with an estimated 32,270 kg mercury recovered and returned to Building 9201-4. The remaining mercury was unrecovered and disposed of in drums as scrap (McAlister, 1971). Three soil borings indicated evidence of mercury in subsurface (letter from P. D. Guettner to D. W. Smith, August 27, 1971).
1971-1984	Building 81-10 was used to store scrap metal and drums of sludge (Wiggins, 1988a) (Y/IS-412).
1983-1984	A two-phase site investigation study was conducted by the Oak Ridge National Laboratory (ORNL) to investigate subsurface mercury concentrations at Building 81-10. The investigation included installation of well nest 56-5 and the drilling and sampling of eight soil borings. Soil samples collected during the Phase I monitoring well installation process detected mercury on the order of hundreds of ppm as deep as 17 feet. During this phase, small beads of visible mercury were noted in samples at 6 feet below ground surface. Phase II soil samples indicated that two locations (B-3 and B-4) had total mercury concentrations greater than 1000 ppm. Water samples obtained from the monitoring wells indicated that the mercury was not mobile in the aqueous phase (Rothschild et al., 1984a) (ORNL/TM-9092). The Phases I and II sampling localities have since been excavated as part of the Perimeter Intrusion Detection Assessment System (PIDAS) and East Fork Poplar Creek tile replacement projects.
1984	Building 81-10 was used to stockpile mercury-contaminated soil [Remedial Feasibility Investigation (RFI) Report, November 1988]. The use of Building 81-10 to stockpile soil was discontinued and the soil was removed; however, the date of removal is unknown. Also, sometime after 1983-1984 the mercury roaster was dismantled and removed from the site.
1987	Approximately 8,400 (± 500) cubic yards of soil (fill) material was removed from the area north of Building 81-10 between November 1987 and April 1988 for the Utility System Restoration Phase 3 (USR III), creek tile replacement, and PIDAS corridor projects. Monitoring wells 56-5 A, B, and C were plugged and abandoned due to construction (Wiggins, 1988a) (Y/TS-412). In addition, boring localities B-3, B-4, B-2, and B-7 were excavated or partially excavated.
1988	An RFI Plan was issued for Building 81-10.
1990	The Building 81-10 RFI Work Plan was implemented. The results of the RFI activities are summarized in a site characterization prepared by Earth Technology Inc. (draft report).

Building 81-10 Demolition, Y-12 Plant

Aerial view of Building 81-10 and surrounding facilities looking in a north-northwest direction.



Building 81-10 Demolition, Y-12 Plant

Aerial view of Building 81-10 looking in a northwest direction. Notice the metal frame structure at the east end of the building. This is the mercury roaster which was dismantled and removed from the site sometime after this photograph was taken on Nov. 29, 1983.

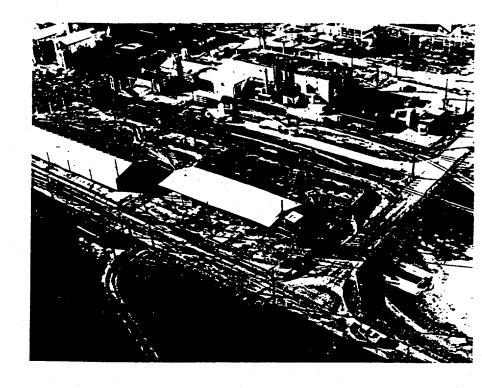
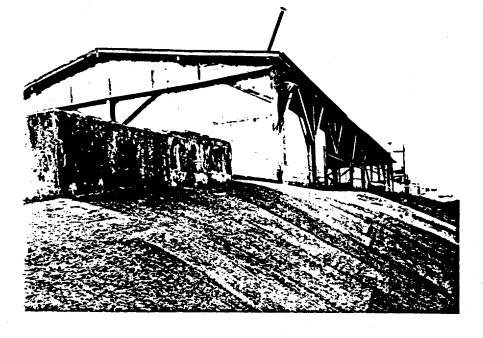


Fig. 3. View 1 - Aerial view of Building 81-10 and surrounding facilities looking in a north-northwest direction.



Building 81-10 Demolition, Y-12 Plant

East facade of Building 81-10.



Building 81-10 Demolition, Y-12 Plant

Northeast corner of Building 81-10.

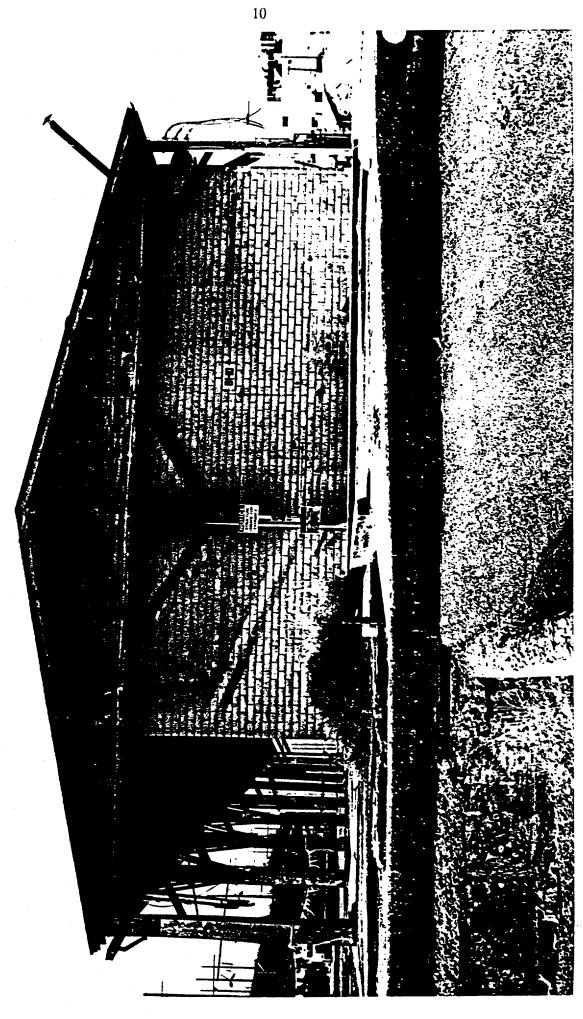


Fig. 8. View 6 - East facade of Building 81-10.

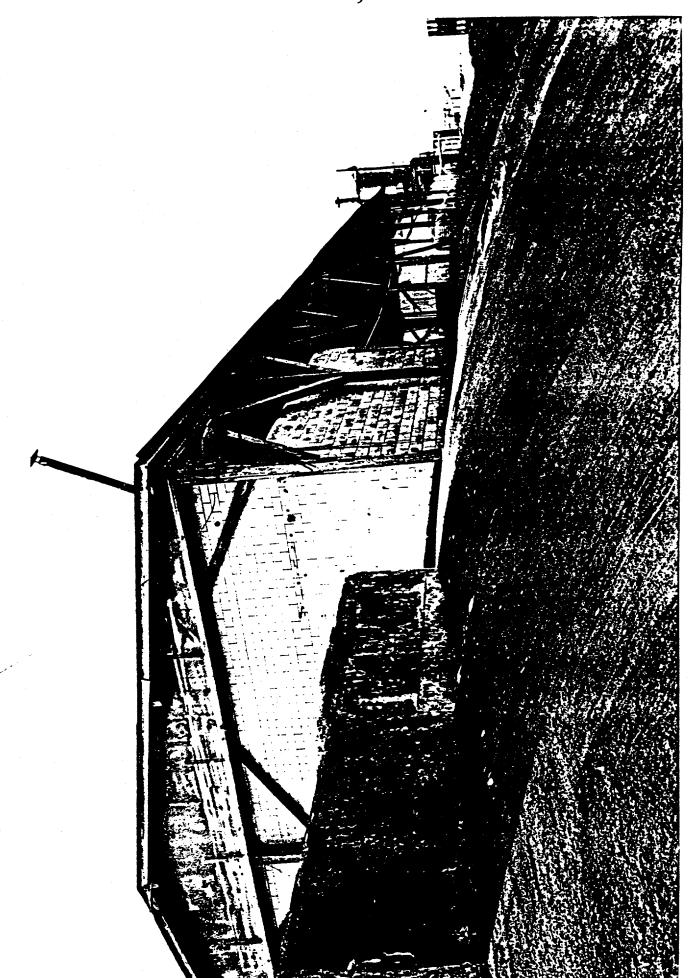
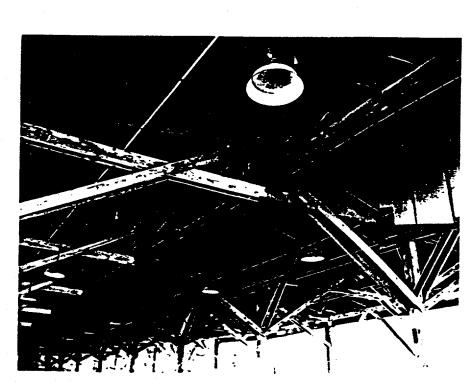


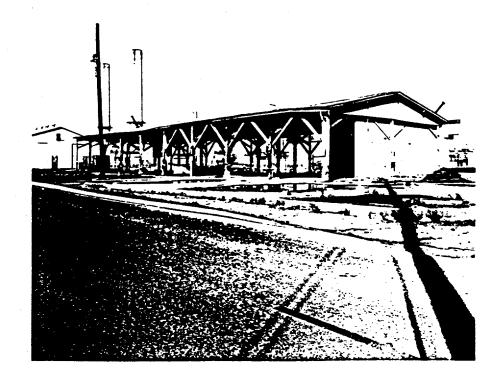
Fig. 7. View 5 - Northeast corner of Building 81-10.

Building 81-10 Demolition, Y-12 Plant

Interior view of rafter and roof support structures in Building 81-10.



Building 81-10 Demolition, Y-12 Plant Southeast corner of Building 81-10.



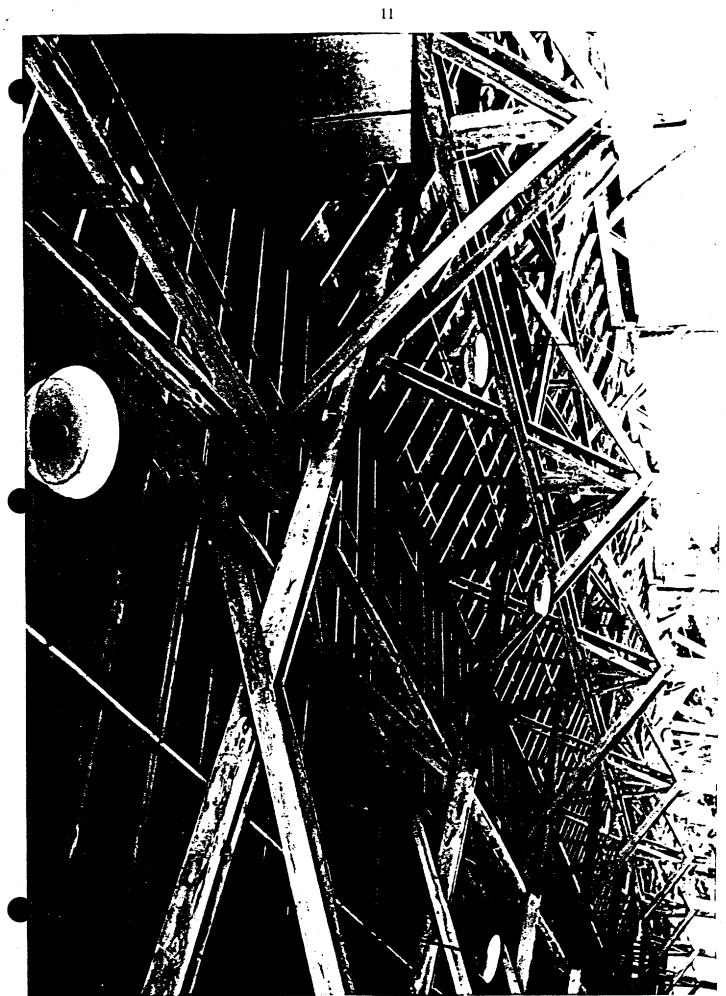
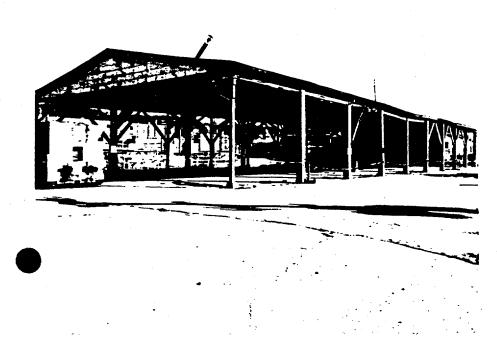


Fig. 9. View 7 - Interior. Rafter and support structure configuration of the Building 81-10 roof.



Building 81-10 Demolition, Y-12 Plant

Southwest corner of Building 81-10.



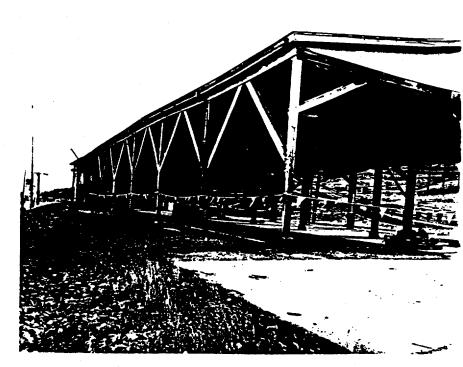
Building 81-10 Demolition, Y-12 Plant

South facade of Building 81-10. Notice the sway in the roof line near the center of the photograph.

Fig. 5. View 3 - Southwest corner of Building 81-10.

Fig. 4. View 2 - South facade of Building 81-10. Notice the sway in the roof line near the center of the photograph.

Building 81-10 Demolition, Y-12 Plant Northwest corner of Building 81-10.



Building 81-10 Demolition, Y-12 Plant

Southwest corner of Building 81-10.

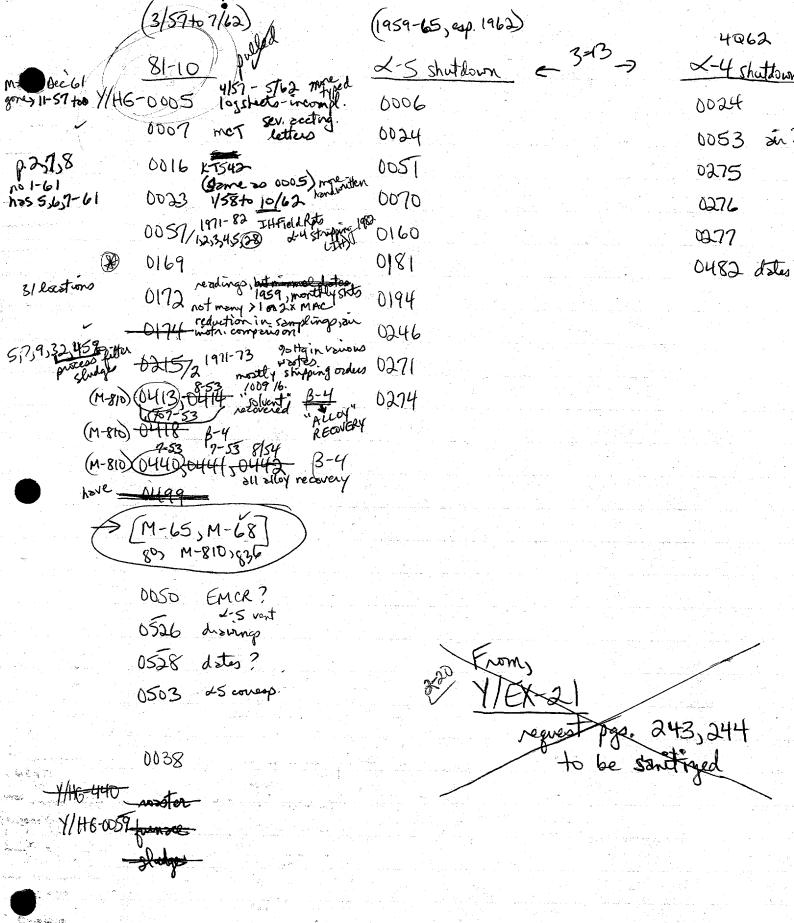


Fig. 6. View 4 - Northwest corner of Building 81-10.

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	195 Annrill	1957 Op prill arthaniar squat	1957 Days Crum 1957 Operated Mont Proc Operated Mont In 13 13 14 15 15 16 15 15 15 16 16 17 16 17 16 17 17 17 17 17 17 17 17 17 17 17 17 17	Drums	Drums	Drums	Drums	Drums Drums Drums Pounds Document Document	Drums Drum	Press Pres	Dys Prums Prums	Dyes Dress Dress	Days		Press	State Present Presen	Press Pres

			,	-	_	_			_	_ 1						_		
				· · · · · ·				COMULAI	CUMULATIVE SUMMARY OF	OF SOLVENT	SOLVENT RECOVERY FACILITY	FACILITY		·				
										Pounds To	Pounds To	Pounds To 1	Total Pounds	Total 0		Total U		
			Drums	Drams	Pounds Decanted		Condensed	Pounds					<u>g</u>	Pounds C		ting	Per Pound U	Unit Cos Per Pour
				s ed		" <u>B</u>		Condensed To Date	Month	To Date h	Month	L	Month	To Date Month		te	1	To Date
	-//			\sqcup)	,	4	× ×	k	76.1.3	181	E31
Ap.	April	ಚ	53	53	31,15	TRILLE	4,204	1,201	35,355	35,355	, 6	,	97 887	193 91.0	14 669	22.013	777	179
THE O	⋖	16	139	382	67,905	99,056	19,982	24,186	87,887	123,212	þ	, }	10001	2000	מאלפנים	2 26	1 1	7.55
June	8	8	196	390		135,1/12	56,343	80,529	92,758	216,000	þ	þ	92,70	210,000	emerican series	30,000	ome.	25T
July]₩	29	178	\$68	15,094	150,565	60,452	140.981	75.51.6	291,546	þ	þ	75,546	291,540	12,200	75.00	2 2	10.
an	Angust	ષ્ટ્ર	325	893	<u> </u>	161,335	30, 1\lambda	171,122	10,911	327,457	þ	þ	116,01	322,457	2000	OTT 20	307	275
Se	September	27	288	1,181	19,406	180,741	18,527	219,649	67,933	μ00,390	þ	6	07,933	uco, syo	4C0 07	CC26TD		203
Oc.	October	8	<u>l</u> :53	1,634	14.963	195,704	73,595	293, 2luh	86,558	1,88,948	þ	\$	86,858	846 881	21,901	103,156	133	
Ma Mo	November 1	29	L17	2,051	161,25	248,198	65,483	358,727	76,368	565,316	11,609	11,609	177,977	26,000	TIL LES	830 tet	27%	3
D	December	23	34,9	2,400	16,266	264,464	36,008	394,735	52,274	617,590	ķ	11,009	112625	4476460	CCTOTT	0666767	*10	• 20.
																		Same of
	1958					200	2 83	763 041	þ	617.500	195-65	101.173	59.561	71.8.763	12,265	223 واللا	206	206 20
- La	January	2 8	330	2 11.2	3 2 2	271.729	h5.523	195.059	12,461	630,051	35.554	136,737	18,025	766,788	8,642	152,865	J80	192 -13
K 17	Yearch	23 5	1.33	3.576	8ولا ور	285,077	59,717	554,776	þ	630,051	73,065	209,802	73,065	839,853	13,293	166,858	Zar.	189 13
A	April	8	15cm	կ,001	19,797	304,874	58,770	613,546	þ	630,051	78,567	288,369	78,567	918,420	13,094	179,252	\perp	
*	Нау	23	253	4,254	17,816	322,690	52,747	666,293	60,460	690,511	10,103	296,472	70,563	988,983	27,72	190,904		179 12
<u>.</u>	June	þ	þ	կ.254	1,053	323,743	þ	666,293	1,053	691,564	þ	298,472	1,053	990,036	0,259	27, 200		203
S	ժովջ	21	335	և,589	14,921	338,664	65,959	732,252	80,880	772,11111	e p	27,000	00,000	ork 01/0 1 088 08	2 200	226,75	270	
ıv	August	32	178	5,067	17,743	356,407	71,727	803,979	5,074	OTC 111	04,5%	302,000	9,470	30 91.8 7 980 631.	18 030	257 600	157	
Se	September	28	592	5,659	37,991	394.398	82,257	886,236	99,979	877,497	20,269	101,137	017,021	TCO-002 T OIZ-072T	11 476	317 72	./6	
Q	October	29	664	6,323	176 33	570 931	67.396	953632	7 574	8823/6	2000	692/11	241/27	1227 283	/c /2/	797/7/	36.	
×	November	30	737	7060	115,306	696237	16.367	1074,501	18162	1010751	17.00 P	46/, 170	9.5	1,124,120	10.00	5,0	, ,	
Б	December												- 1					
₹.																		

		-		1					-	-									-												
					December	Kovember	October	Soptember	August	July	June	Hay	April	iarch	Pebruary	January	1962	December	Novembe:	Octobe:	Sept ember	August	July	June	l'iey	April	Harch	February	January >	1961	
										0	0	/2	30	30	38	20							С	0	0	30	3/		28		Days Operated
										0	0	72	171	249	318	102							0	0	0	329	273		/77		Drums Processed Current Honth
																													,		Founds Drums Decanted Processed Current To Date Fronth
										C	o	8,580	24,977	43,003	43.313	6314							0	0	0	33,930	32,493		21377		
																															Pounds Decanted To Date
										С	0	2615	12.762	39,505	32,619	441,22							c	0	0	35,089	21,912		7358		Pounds Condensed Current Fonth
																															Pounds Condensed To Date
																							0	0	٥	0	0		٥		Pounds To Alpha-4 Cascades Current Month
																															Pounds To Alpha-4 Casaades To Date
-																					_		0	0	0	67.019	54,405		28,735		Pounds To Alpha-5 Cascades Current
	1																														Pounds to Alpha-5 Cascades To Date
										\downarrow	0	16.195	37.739	82,508	75.631	29.058							0	0	0	67.019	504 405		28,735		Total Pounds Reclaimed Current Month
	-	_							09/7/200	35.09 74.1																					Total Pounds Reclaimed To Date
	-								1000	482	1900	4787	1663	11074	7454	2418							ردهن	5,645	878	6104	6295		8844		Operating Cost Current Month
								-						-																	Total Operating Cost To Date
											200	000	70 70	/36/	950	280									1700	20/	. ///.		147		Whit Cost Per Pound Current Month

		-																4		,			
			E 60067	The Bure	. A total		Cost Per Bo		Cost Per Pe	Total Cost to Date	Total Bottles to Date	Pounds Bott	Cost Per Pe	1 SOUT TENOT	3	Number of P	Number of B	Pounds Bott				ACCOUNT 2686-100	
			1700, and / pointes on same 12, 1700.	The Bureau of Standards 13 bottles on March 18	A total of 20 bottles (1520 lbs) was shipped to		Cost Per Bottle to Date (\$)		Cost Per Pound to Date (\$)	to Date (\$)	es to Date	Pounds Bottled to Date	Cost Per Pound This Month (\$)	TOTAL COST TITLE HOLLM (4)	75- Kan+1 (4)	Number of Pallets (25 Bottles)	Number of Bottles (76#)	Pounds Bottled This Month			1	1	-
			900 TANG	13 bottles o	O lbs) was sh								-)						SOLVENT BOTTLING	
				n Harch 18,	tpped to		8.68		.113	2,579	300	22,800	.113	2000	2.570	12	300	22,800	Jan. 160				
							2,90		.038	4,415	1,520	115,520	.020	2 / 2 / 2	1.836	8. 84	1,220	72,7au	Feb. 160				
:							3.13		.041	4,761	1,520	115,520			976	0	0	c	8				
							2.33		1E0.	6,557	2,820	214,320	\$10		1.7%	52	1,300	%	Dec. 160			· · · · · · · · · · · · · · · · · · ·	
				-			 1.35		\$TO.	16,418	12,170	924,920 1,572,820	71 0•		9.861	374	9,350	ora for	_1_				
							1.34	: :	*018	27,825	20,695		8t0*		11.407	#£	8,525	0,420			+		**************************************
-		-					10177	i	•015	37,959	32,420	2,463,920 3,356,920 3,801,520 3,801,520	to.		10,134	469	11,725	001 676					•
							100	1 100	•015	18,947	44,170	356,920 3	_012		10,988	۵۲,	11,750	+-+	-1-		'		
							COO.T	4	,51¢	53,794	50,020	801,520 3	110.		4.847	234	5,850	9000	\rightarrow		····		
						5	1,001	1 039	710-	53,874	50,020	801,520	-		8	0	0	-	Jme 161	}			
					-																		
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Pill Porcing

Typor life expositions Get all available flasks How floor cost \$9 19359 bottles To 65A in Box Pallets (3656 Order Florhe gsa sc Valuts 25 Billes

y								
				APRIL	1957	_		
				Account	2686		X1+6-00	
			(Sc		overy Facil:	ity)	X140-00	<i>دم</i>
	1.							
				Amount	Unit Cost	t		
-	GOMAT TADO							
	TOTAL LABO	<u> </u>		2,923	083			
	Direct			708	.020			
	1-2-9 4-6-7-10-	1.	 	730	.021			
	4-0-1-10-			1,485	.042			
	TOTAL MATE	RTAT.		2113	•007	 		
	Direct			-0-	-0-	 	<u> </u>	
	1-2-9			180	•005		 	
	3-4-5-6-8	-13-50		63	•002			
					1002			
	TOTAL LABO	R & MATERI	AL	3,166	•090			
	APE			3,296	•093			
	. ^				,			
	TOTAL WORK	ED MATERIA	(Natural Gas)	13	.0003			
·	1,							
	TOTAL COST	я		6,475	.183		·	
				,				
	TOTAL SOLV	ENT RECLAIM	ED (Lbs.)	35,355	1			
				·	<u> </u>			
			1	4	peration 1			
		· · · · · · · · · · · · · · · · · · ·			were proce			
	· ·	-	total amou	nt reclaim	and 1,021	Lbs. were		
				The state of the s	productio	n was trans	ferred	
			to Alpha-L	Cascades.				
								(
				7-1				
<u> </u>				A	PPROVED I	OR PUBLIC	RELEASE	
	1	_	· · · · · · · · · · · · · · · · · · ·		M		10/- 1	
					echnical Info	rmation Off	e Date	
					ormitoat mil	madon Oill	Date Date	
1CY DOE / 1- 140	Y-12 DATA SH			* * * * * * * * * * * * * * * * * * * *				

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				MAY	1957				
4				k		7			
				Account					
			(:	Solvent Rec	overy Facil	. t y)			
				Amount	Unit Cost				l
					5222 5 5 5 5				
	TOTAL LABO	R		6,873	078	 		+	
	Direct			2.571	.029		- 	+	\dashv
-	1-2-9		·	2,708	.031			 	-
	4-6-7-10-	11	·	1,594	.018				\dashv
								 	\dashv
	TOTAL MATE	RTAL	+	1,518	.01.7				\dashv
	Direct			64	.001		•		十
	1-2-9			1.075	.012				
	3-4-5-6-8	-13 - 50	<u> </u>	379	.00li				1
· ************************************									
	TOTAL LABO	2 & MATERT	AT.	8,391	-095				
	4200								
	APE			7,155	.081				
	TOTAL WORK	30 344077774	(Natural Gas)						_
	TOTAL WORK	ALTERTAN CO	Gas)	22	_001				\bot
	TOTAL COST	 		24 440					
	TOTAL COST			15,568	.177				
	TOTAL SOLVE	ENT RECTAIN	ED (The)	97 995		· · · · · · · · · · · · · · · · · · ·			
			LIUS.	87,887					4
			This proce	70 200 40			<u> </u>		+
			during the	month 33	peration 1	days		10%	+
·			Of the tot] amount	9 drums wereclaimed, 6	e process	าว % ·	10 10	+
			were separa	ted physic	ally and 19	082 15-	23%		+
			by condens	tion. The	total prod	ection was	0.0		+
			transferred	to Alpha	Cascades	NO.			+
-									十
									†
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WCX-885 (Jan'48)	Y-12 DATA SU								
	. 44 DAIA SHEE			i			T		Γ

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				JUNE	1957				-
				Marie House			1		ĺ
•				Account					
			(Solvent Red	covery Facil	ty)			
	1			_					
				Account	Unit Cost				
	TOTAL LABO	<u> </u>							
	Direct	,		5,473	•059		,		\bot
	1-2-9			2,052	•022			<u> </u>	\bot
	14-6-7-10-	1.		1,702	.018				\bot
				1,719	.019			 	4
	TOTAL MATE	RIAL		1,349	.015				4
	Direct			-0-		 		-	+
	1-2-9			890	-0-			 	+
	3-4-5-6-8	-13-50		459	.010			 	+
				427	•005				+
	TOTAL LABO	R & MATERT	AT.	6,822	.074				+
				0,022	•074	·		,	+
	APE			6,155	•070		•		+
-				1	.010				+
	TOTAL WORK	ED MATERIA	(Natural Gas)	1,2	200 JT				+
					001		 		┿
	TOTAL COST			13,019	ווינר				十
				#2 3 012	• 1/1/1				+
	TOTAL SOLV	ENT RECLAID	ED (Lbs.)	92,758					╫
									+-
· · · · · · · · · · · · · · · · · · ·			This proce	ss was in c	peration a	proximate	v		+
					nth. 198				+
-					tal amount				+
			36,415 lbs	. Were sepa	rated physi	cally and			+
			56,343 lbs	by conder	sation. To	e total			T
			production	was transf	erred to Al	pha-4 Caso	ades.		1
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			4						
WCX COS (1)									
WCX-885 (Jan'48)	TTIZ DATA SHE	ET	. }	İ	l	·			

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				JULY	1957				
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<u> </u>		j .		Account	2686				- 1
	٠		(5	dlvent Rec	overy Facil	itv)			
				1	.				1
		 	 	Amount	Unit Cost				\perp
	TOTAL LABO	1		(00/		<u> </u>			
	Direct			6,036	.080	<u> </u>			4
	1-2-9			2,069	.027	 	<u> </u>		4
	4-6-7-10-			2,392	.032				_
				1,575	.021				_
	TOTAL MATE	RTAT.		770		·	+		-
	Direct			772	.010				+
	1-2-9			-0-	-0-				4
	3-4-5-6-8	13-50		504 268	.007				4
				200	•00/4			,	+
	TOTAL LABO	R & MATERT	AT.	6,808	000			 	- -
				0,000	•090		 		\bot
	APE	·		5,395	077			· ·	+
				2,275	.071			<u> </u>	+
	TOTAL WORK	ED MATERTA	(Natural Gas)	65	007	· · · · · · · · · · · · · · · · · · ·		-	+
			yas/	- 05	.001				+
	TOTAL COST			10.069	7/0				4
		:		12,268	•162			<u> </u>	4
	TOTAL SOLV	ENT RECLATI	ED (Lbs.)	75.546					+
		110011111	IID (IIUS)	13.540					+
			This proce						┿
	· ·		This proce					1 0 77	+-
			month. 17					68%	+-
			amount rec	armed, 15,	UYL lbs. we	re separat	ed		+
			physically The total	roduction	TOS DY CO	ngensation	1. 1		+
			Cascades.	TOURCE TON	was cransie	rred to Al	pha-4		╁
									+
	,								+
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WCX-885 (Jan'48)	Y-12 DATA SHE	ET							-
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					1771	-			
				Account	2686				
					ecovery Faci				
					702,7 120.				-
				Amount	Unit Cost				•
	TOTAL LAB	OR		7,111	.17				\dashv
	Direct			3,266	.08				\dashv
	1-2-9			2,193	.05				\dashv
	4-6-7-10	-1/1		1,652	.04				\dashv
									\dashv
-	TOTAL MAT	TRIAL		1,191	•03			 	+
	Direct			-0-	-0-		-	 	+
	1-2-9			670	.02		+		+
6,	3-4-5-6-8	3-13-50		521	.01				+
					1		<u> </u>	+	+
	TOTAL LABO	R & MATERI	AL	8,302	•20		1		+
				1 0,502				 	+
	APE			6,738	.16		 	 	+
				0,130	•10		<u> </u>	-	4
	TOTAL WORK	ED MATERIA	(Natural Gas)					<u> </u>	\bot
		- IMIMUA	uas .	46	•01.				_
	MODELT GOOD								\bot
	TOTAL COST			15,086	-37				丄
	TOTAL COLU	This December							丄
	TOTAL SOLV	ENT RECLAIM	ED (Lbs.)	40,977					\bot
									丄
			This proce	ss was in o	peration 3	days dur	ing		
			the month.	325 Drums	were proce	ssed. Of	the	2%	
			total amon	nt reclaime	d, 10,770	bs. were	eparated		
		-	physically	and 30,7/17	lbs. by co	ndensation	The		\prod
			total prod	ction was	transferred	to Alpha-	L Cascades		\prod
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WCX-885 (Jan'48)	Y-12 DATA SHE	ET	- T						

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				SEPTEMBER	1957				
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				Account	2686				1
			(;	Solvent Rec	overy Facil	ty)			
				Amount	Unit Cost				
	TOTAL LABO	DR.		9 025					_
	Direct			8,935	.132				_
	1-2-9	 		4,066	.060			_	4
	4-6-7-10-	11.		2,472	.036		 		
				2,397	.035		-	<u> </u>	_
	TOTAL MATE	RIAL		1.835	007				
	Direct			-0-	.027		 		+
	1-2-9			930	-0-		 		\dashv
	3-4-5-6-8	-13-50		905	.013				
				70)	•013			+	
	TOTAL LABO	R & MATERI	AL.	10,770	.159			·	
								-	+
	APE			7,936	.117			+	+
-					•±±/	 	+	 	+
	TOTAL WORK	ED MATERIA	(Natural Gas)	41	•0006			-	+
				44	•0000			+	+
	FROM	2620		92	707				+
				76	•001		 	 	+-
	TOTAL COST			18,839	.277				+-
				20,017	- 11				+-
	TOTAL SOLV	NT RECLAIM	ED (Lbs.)	67.933		`	 		+-
					-				+
			This proce	s was in	peration 27	dame des	na		+
			the month.	288 drums	were proces	seed of	the	3.8%	+
			total produ	ction. 19.	106 lbs. wer	e senerat	otte	7.0 /0	+-
			physically	and 48.527	lbs. by con	densation	<u>u</u>	 	+-
			The total b	roduction w	as transfer	red to Al	nha li		+
			Cascades.		- Vadiot Ct	LUA UU AJ	Mrg_ft		+-
									+-
			·						+
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WCX-885 (Jan'48)	Y-12 DATA SHE	ET							+
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1				Account	2686	·			
				(Solvent Rec	every Faci	lity)			
	_1			Amount	Times Const				
				AMOUNIC	Unit Cost				
	TOTAL LAB	CR		10,304	.12	 			
	Direct			4.332	.05				\dashv
	1-2-9			2,382	•03		-		\dashv
	4-6-7-10	1)4		3,590	.04				-
				2,770	- •04		_		
	TOTAL MATI	RIAL		1.957	.02				-
	Direct			-0-	-0-				+
	1-2-9			796	.009	<u> </u>			+
-	3-4-5-6-8	-13-50		1,161	.01				+
	•								+
	TOTAL LABO	R & MATER	TAIL .	12,261	.14				+
								-	+
	APE			9.573	,m				-
-		·							+
	TOTAL WORK	ED MATERIA	(Natural	18	•005				+
									\top
	FROM	2620		19	.002	-			+
			,						十
	TOTAL COST	·		21,901	.25		·		十
	TOTAL SOLV	ENT RECLAI	MED (Lbs.)	88,558					1
		~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~							十
			This proce	ss was in o	peration 30	days dur	ing		$\prod$
***************************************			the month.	453 drums	were proce	essed. Of	the	3%	
			total amou	nt reclaime	a. 14963 11	os. Were s	sparated		
			physically	and 73,595	lbs. by co	ondensatio	a		
-				production	was transfe	erred to A	lpha-li		
			Cascades.						
		·							
									<u> </u>
		_						<b></b>	_
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WCX-885 (Jan'48)	Y-12 DATA SUE	FT							<u> </u>
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				DECEMBER	1957				
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				Account	2686				
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				Amount	Unit Cost				<u> </u>
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	TOTAL LABOR	1		7.095	.14				$\vdash$
	Direct		<u> </u>	3,462	.07		ļ		-
	1-2-9			2,236	-Oli		ļ		_
	<u> 11-6-7-10-</u>	<u>),                                     </u>		1,397	.03				_
	TOTAL MATE	RIAL		762	.01				_
	Direct			-0-	-0-				
	1-2-9			557	.01				
	3-4-5-6-8	-13-50		205	<b>200</b> Jr				
	TOTAL LABO	R & MATERIA	L	7.857	.15			·	
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	APE			6.474	.123				
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	TOTAL WORK	D MATERIAI	(Natural Gas)	92	<b>_</b> 002		·		
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	FROM	2620		10	.001				
	TOTAL COST			71, 1,33	276				
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	TOTAL SOLV	SNT RECLATM	ED (Lbs.)	52.274					
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	1-2-9			1,346	.023				$oldsymbol{oldsymbol{\perp}}$
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	1-2-9			635	.011	· · · · · · · · · · · · · · · · · · ·		<u> </u>	-
	3-4-5-6-8	-13-50		303	.005			<del> </del>	╄
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	TOTAL SOLV	GNT RECLAIN	ED (Lbs.)	59,564					├
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	APE			3,618	•08				+
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	Direct	<del> </del>		2,469	•035			
	1-2-9	<u> </u>		2,467	•035			
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	APE			5.150	.073			
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	TOTAL COST			11,732	.1663			
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	TOTAL LABOR			5,684	.081	1.57			
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	1-2-9			612	.009				<b>_</b>
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· ·				Account	2686	1.			
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•			,	Amount	Unit Cost				
									+
	TOTAL LABOR			3,643	3.460		1		+
	Direct			283	.269				+
	1-2-9			3,129	2.972				+
	4-6-7-10-1	4		231	.219				+
				5/-	9647				+
	TOTAL MATER	IAL		1.860	7 774				+
	Direct			1	1.776				+
<del></del>	1-2-9			7 785	-0-				+
<del></del>	3-4-5-6-8	13 <b>-</b> 50		1,785	1.695			· · · · · · · · · · · · · · · · · · ·	+
	7 7 7 -0-0-	-J-J0		75	.071				$\vdash$
	TOTAL LABOR	& MATERIA							Ļ
	LATER MEDUL	- w maintiA	<b>.</b>	5,503	5.226		<del> </del>		$\vdash$
<del></del>	APE								L
	ALD			3.135	2.977				L
	MODEL TENE		•	_		*			L
	TOTAL WORKE	MATERIAL	(Natural Gas)	(379)	(.360)				L
									L
	TOTAL COST			8,259	7.843				
	TOTAL SOLVI	NT RECLAIM	ED (Lbs.)						
-								-	
			Days Operat	ed:	-0-				
			Drums Proce	ssed:	-0-				
			Lbs. Conder	sed:	-0-				
			Lbs. Decant	ed:	1,053				
				Cascades:	1,053		181116		
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	TOTAL LABO	E MATERIA	į.	5,503	5.226				
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	TOTAL WEEK	D MATERIAL	(Natural (as)	- (379)	(360)				
	TOTAL COST			8, 259	7.843		·		
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	Other			3,601	-045	<del> </del>		
	·			903	.011	<del> </del>		
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	TOTAL WORK	D MARKOTAT	(Natural, Gas)					
_	MANA	MINIMA	Gas)	59	•001			
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	TOTAL COST		<del> </del>	15,376	.190	· .		
	TOTAL BOTT	Mu Dave	2	1 22 22			+	
	TOTAL SOLV	at Reclaim	(Lbs.)	80,880			+	
							+	
			Down A			•		
			Days Operat		21			
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		1	Lbs. Conder		65,959	<del>/</del>	211F//0	
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				Cascades:	80,880	-13	HEGE/VE	
			Lbs. To A-	Cascades:	-0-	8. 4	AUG 29 1958 A. WALKER	
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		· · · · · · · · · · · · · · · · · · ·	Lbs. To A-L		80,880				
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	Direct			4,058	•045	\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\	R. A. WALK	ER /-/
	1-2-9	·		5,571	.062	7	*	1/2/
<del> </del>	Other			1.383	.015	† ·	67/1211	8
·								
	TOTAL MATER	IAL		2.836	.032		<b>†</b>	
<del></del>	Direct			-0-	-0-			
	1-2-9			2,425	.027	,		
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	APE			10,202	.11).			
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· · ·				,				
	TOTAL COST			24,132	•270			
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<del></del>			Days Operat	ed:	31			
			Drums Proce		1478			
			Lbs. Conden		71,727			
			Lbs. Decant	ed:	17,743			
				Caspades:	5.074			
		·	Lbs. To A-5	Cascades:	84,396			
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·	1-2-9			2.425		.02.7			-
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	TOTAL LABOR	A WATERTA		13.848		.155			
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	1-2-9			3,508	.029	9	R 1241	50
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	TOTAL MA	TERIAL		2,658	.022		X///	2)
<del></del>	Direct			0-	-0-			
-	1-2-9		-	2,283	.019			
	Other	-		375	•003			
	MOMAT TAX	202						
***************************************	TOTAL LA	BOR & MATER	LAL	11,174	•093			
	APE		<del></del>					
	APE	-		7,573	•063	,		
-	TOTAL WOL	RED MATERIA	(Natural					· · · · · · · · · · · · · · · · · · ·
<b>***</b>	· ·			74	.0006			
	i	SERVICES (2	791)	118	.001			
	TOTAL COS	24		18,939	.157			
	TOTAL SOL	NENT RECLA	OCED (The )	700 010				•
	JOIAN DOZ	PALL RECLA	MED (Tos.)	120,248				
			Days Operat					
			Drums Proce	1	28			
			Lbs. Conder		592			
			Lbs. Decant	i T	82,257			
		i	Lbs. To A-	1	37,991	·		
		1	Lbs. To A-		99,979			
			LUS 10 A-	Uascades:	20,269			
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WCX-865 (Jan'48	Y-12 DATA SI	HEET						

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	1-2-9			2.283	.019				_
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~ <del>~~~</del>	TOTAL LABOR	R & MATERIA	L	11,174	,093				
_	APE			7.573	.063				
-			Metaval						
	TOTAL WORK	ED MATERIAL	(las)	74	.0006				-
	Special Se	rvices (2	791)	118	.001		·		
	TOTAL COST			18,939	.157				_
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·	TOTAL SOLV	ent risclad	Kn (198*)	120,248	4,008				
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<del></del>			Days Operat	ad :	28	•			
<del></del>			Drums Proce	1	592				_
<del></del>			Lbs. Conder		82,257				
		í	Lbs. Decant	F	37,991	•			
·			Lbs. To A-						
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885 (Jan'48	) Y-12 DATA S	HEET						<u>}</u>	

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	TOTAL LABOR	<b>S</b>		7,313		<b>-030</b>	_\	
	Direct			4,227		_017	8	1101110
	Other			2,250 836		•009		7 101
				050		<b>.</b> 003		
	TOTAL MATE	IAL		2.742		.011		
	Direct			-0-		-0-		
	1-2-9			2,504		•010		
	Other			238		.001		
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	4.000						·	
	APR:	).		6,523		-027		
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	Natural C			151 82	·	.0006		
	Special S		(2791)	69		_0003		
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-	TOTAL COST			16,729		-069		
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	TOTAL SOLVE	NT RECLAIM	D (1bs)	2113,929				
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			lays Operat	1 1	29			
			rums Proce	1 1	664	690		
		•	bs. Conden		67,396			
			Da. Decant	ł I	176,533			
			_	Cascades:	· 1			
			LOS. TO A->	Cascades:	239,050			
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	Direct			4.227	1.017		•		
	1-2-9			2,250	.009			-	
	Other			8.36	.003			•	
	TOTAL MATER	TAL		2,742	.011				
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	Other			238	. 001		ļ		<del>                                     </del>
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	TOTAL WORKE	D MATERIAL	•	151	.0006				-
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	TOTAL COST			16,729	.069	·			<del> </del>
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	TOTAL BOLVE	NT RECLAIM	D (Lhe.)	243,929			<u> </u>	<b></b>	-
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			Days Opera		29				+-
<u> </u>	<del>  </del>		Druma Proc		12201				<del>                                     </del>
			Lbs Conde	'	176,533				
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<del></del>	TOTAL LABO	<b>1</b>		0 770			
	Direct	1		8,118	.039	ļ	
·	1-2-9			5,108	.025		
	Other			2,437	.011		
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	TOTAL LABO	R & MATERIA	NL.	8,246	.040		
	A TOP						
	APE			7,834	.038		
	MODAT HODE						
	TOTAL WORK			122	.0006		
	Natural C			80	.0004		
		ervices (2	791)	40	.0002		
	TOTAL COST			16,202	.078	····	
	BODAY COTT						
	TOTAL SOLV	ENT RECLAIM	ED (Lbs.)		208,175		
			Days Opera		30		
			Drums Proc		737		
			Lbs. Conde	1	92,869	·	
		***	Lbs. Decan	ted:	115,306		
			Lbs. to A-A	Cascades:	188,802		
			Lbs. to A-	Cascades:	19,373		
WCX-885 (Jan'48)	Y-12 DATA SH	EET	·				

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··		<u> </u>	i	Amount	Unit Cost				
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·	Direct		<u> </u>	5,108	•025			ļ	4
	1-2-9		<u> </u>	2,437	.011	1			4
	Other	-		573	,003				+ 1
·			. !	7.28	2226				+ 1
	TOTAL MATE	RIAL	· · · · · · · · · · · · · · · · · · ·	128	,0006				+ 1
	Direct		·	(2.22)	.0	•			-
	1-2-9 Other			(122)	.0012		<del> </del>		<b> </b>
<del></del>	Caner	-		1	-002-	<b> </b>			-
<del></del>	TOTAL TABO	r & Materia		8,246	.040				
	IOIND Trees	C 135 2120 Carry	<u>,                                    </u>	٥٫٨٠٠	• 040		<del> </del>		<b> </b>
	APE			7,834	.038				
	354			,,			·		
	TOTAL WORK	ED MATERIAL	<del></del>	122	.0006				
,	Natural C	<del> </del>		80	.0004				
		ervices (2	<b>191)</b>	40	.0002				
	TOTAL COST	<del>, , , , , , , , , , , , , , , , , , , </del>	l	16,202	.078				
			<u></u> I						1
	TOTAL SOLV	ENT RECLAIM	ED (Lbs.)		208,175				+
I	1				<u> </u>				+
· · · · · · · · · · · · · · · · · · ·			Days Operat	ted:	30		ļ		-
			Drums Proce		737	<u> </u>	<u> </u>		+
			Lbs, Conder		92,869				+
	!	1	Lbs. Decant		115,306				+
	<u> </u>	1 1	•	Cascades:	l .		ļ		+
i			Lbs. to A-	5 Cascades:	19,373		-		+
l ———			<u> </u>		-				+
	<u> </u>		<u> </u>						+
								<del>                                     </del>	+
-			L						H
					<del> </del>				-
-									+
/ 1- n*H									+
. A-885 (Jan +e	8) Y-12 DATA S	HEE!	1	1	4	1	1	. ,	•

4				,						
					December _	1958				
					Account	2686				-
				S	lvent Reco	very Facili	ty			-
										1
			<del>-</del>		Amount	Unit Cost				
	MOMAT TADA									$\Box$
	TOTAL LABO	<b>*</b>			7,528	.065				$\perp$
	Direct	<del> </del>	<u> </u>		4,484	.039				
<b>4———</b>	1-2-9	<del> </del>		<del></del>	1,992	.017				$\perp$
	Other				1,052	.009				
<del></del>	TOTAL MAT	TRIAT								
*****	Direct	- INTERIOR	+		1,392	.012				4
<del></del>	1-2-9	<del>                                     </del>			-0-	-0-				$\perp$
			<del> </del>		1,029	.009				$\perp$
	Other				363	.003			<u> </u>	$\perp$
-		<u> </u>							<u> </u>	
	TOTAL LABO	R & MATERI	AL		8,920	.077	**************************************			
	A THE	<u> </u>	<del> </del>						·	
<b>—</b>	APE		<del> </del>		6,262	.054				
	MODAY TENNY									
	TOTAL WORK		<u> </u>		29	.0002				$\perp$
	Natural G		<u> </u>		1	-0-				
<del></del>	Special S	ervices (2	791)		28	.0002				
-				$\dashv$						I
	TOTAL COST				15,211	.131				Τ
<del> </del>										Γ
	TOTAL SOLV	ENT RECLEA	RD (lbs.	)		116,195				T
				_						
			Days. Ope			30				$\prod$
			Drums Pr			475				L
		· · · · · · · · · · · · · · · · · · ·	Lbs. Cor			48,583				
N.A.			Lbs. Dec	_		67,612				
			Lbs. to	A-4,	Cascades	32,750				Γ
			Lbs. to	<b>A</b> -5	Cascades	83,445				Γ
										$\Gamma$
										$\prod$
	-			$\bot$						
				$\perp$						
		· · · · · · · · · · · · · · · · · · ·		1						
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WCX-885 (Jan'48)	Y-12 DATA SH	FFT		1.				1		_

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	•	-		December -	1958			, ,	
•									
			So	Account	yery Facili	ty			
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				Anount	Unit Cost				$\downarrow$
							<u> </u>		+
	TOTAL LABO			7528	.065		<u> </u>		+
	Direct	·		4,484	.039				+
	1-2-9			1,992	.017				+
	Other			1.052	.009				╁
									+
	TOTAL MATE	RIAL		1392	.0/2				+
	Direct			-0-	-0-			<del>                                     </del>	+
	1-2-9			1.029	.009			<del> </del>	+
······································	Other			363	003				+
				0.015	-0				+
	TOTAL LABO	r & Materia	l. ·	8920	.077		<del> </del>		十
	A 2:072			6,262	.054	·			+
	APS			6,262	, 83 7				†
	TOTAL UCRY	ED HATERIAI		29	.0002				1
	Natural G			1	-0-				T
		ervicos (27	91)	28	,0002				
	Special o	B1 12000 (21	74,	20	, 0000				
	TOTAL COST			15,211	.131				
	10020			10,211	1.7.9.1				
	TOTAL SOLV	ENT RECLEAR	KD (1bs.)		116,195				
					11.4/1.				_
			Days Opera	ted:	30				$\bot$
			Drums Proc		475				_
			Lbs. Conde		48,583				1
			Lbs. Decan	red:	67.612				_
· · · · · · · · · · · · · · · · · · ·	-		Lbs. to A-	Cascades	32,750				+
			Lbs. to A-	Cancades	83,445				_
				,					
						ļ			$\dashv$
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					<u>:                                    </u>	ļ	·		$\dashv$
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JA-885 (Jan'W	48) Y-12 DATA	SHEET							

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*				January	<u> </u>	1		
			_	Accou	nt 2686			
				Selvent Rec	overy Facil	ty		
				Amount	T-44 0			
				AMOUNT	Unit Cos			
	TOTAL LAB	rie de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition de la composition della composition della composition della composition della composition della composition della composition della composition della composition della composition della composition della composition della composition della composition della composition della composition della composition della composition della composition della composition della co		3,334	.064			
	Direct			2,274				
	1-2-9			744	.044			
	Other			316	.006			
								+
	TOTAL MATE	RTAL		337	.006			
	Direct			2	.000			+
	1-2-9			286	.005			
	Other			49	.001	,		
					1002			
	TOTAL LABO	R & MATERI	AL	3.671	.070			
								<del> </del>
	APE			3,043	.058			
							<del></del>	
	TOTAL WORK	ED MATERIA	1,	44	.001			
	Natural G			44	.001			
	Special S	ervices (2	791)	0	.000			
					.000		<del></del>	
	TOTAL COST			6,758	.129			
	TOTAL SOLV	ENT RECLAI	ED (lbs)		52,333			
					2,355			+
			Days Opera	ted:	16		+	<del>                                     </del>
			Drums Prec		192			+
			Lbs. Conde		29,481			
			Lbs. Decan		22,852			+
				4 Cascades				•
				Cascades:				<del>                                     </del>
							<b>†</b>	<del>                                     </del>
				:			<del>                                     </del>	
				·			† .	
							<b>T</b>	<del>                                     </del>
WCX-885 (Jan'48)	Y-12 DATA SH	EET						<del>                                     </del>

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				January -	1959			in the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of th	
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			S	Accoun	very Facili	ty		•	
	·			Amount	Unit Cost	<u>i</u>			
									-
	TOTAL IABO	۹	··	3.334	.064				-
	Direct			2,274	.011				$\vdash$
	1-2-9			744	.014		,		$\vdash$
	Other			3/6	.006				+
-					,		·		+
	TOTAL MATE	RIAL		337	.006	<u>`</u>			+
	Direct			2	.000		·		+
	1-2-9			286	.005				+
	Other			49	. 00/				+
	mcmay TADO	D • 346 97773 T.4	<b>Y</b>	2/1/	074				+
	TUIAL DUBG	r & Materia	<u> </u>	3,67/	,070				<b>†</b>
	AFE			3,643	.058				†
				3,070	1000	-			T
	TOTAL WORK	ed Materiai	4	44	.00/				T
	Natural C			44	,00/				
		ervices (2	791)	-8 -	-0 -				
	TOTAL COST			6,758	./29	·			
									$\perp$
	TOTAL SOLV	ent reclai	ED (lbs)	4 T	52,333				
									1
			Days Opera	teds	16			<u> </u>	1
			Drums Proc	essed:	192				+
			Lbs. Conde	nsedi	29,481			ļ	+
			Lbs. Decar	ted:	22,852				+
	-			4 Cascades	-0.				+
			Lbs. to A	5 Cascades	52,333				+
					·				+
									+
				<u> </u>				•	+
· · · · · · · · · · · · · · · · · · ·									+
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									+
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				February	- 1959			
						-		
				Solvent Reco	unt 2686			
				TODAY RECO	Aera raciti	LTY		
				Amount	Unit Cost			
	<del>-</del>							
	TOTAL LA	BOR		1,021	.04		·	
	Direct			340	.01		<u> </u>	
	1-2-9			610	.02			
	Other			71	.01			
			1					<del> </del>
	TOTAL MAT	TRIAL		612	.02			<del>                                     </del>
	Direct			0	0			
	1-2-9			527	.019			
	Other			85	.001			
					.001			
	TOTAL LAB	dr & MATERI	AL	1,633	.06			
	APE			1,101	.04			
					10.4			
	TOTAL WOR	ED MATERIA	Ł	23	0			
	Natural (			0	0			
	Special S	ervices (2	791)	23	0			
·				1 2				
	TOTAL COST			2,757	70			
				2,721	.10			
·	TOTAL SOL	ENT RECLAI	MED (The )		ST (22			
		THE IMPLIES	(LOS.)		27,630			
			Dave Carre					
			Days Opera	<u> </u>	0			,
			Drums Proc		0			
			Lbs. Conde		0			
			Lbs. Decar		27,630			
				4 Cascades	18,868			
			Lbs. to A-	5 Cascades	8,762	·		
<u> </u>								
WCX-885 (Jan'48)	Y-12 DATA SHI	EET						

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. •		-		-a •	- 1959		A Comment	214.13.74	
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		•.	. 90	Accou	nt 2686 ory Facili	-the		•	
			S <b>Q</b> .	radit vecta	ery racital	wy .			
, , ,				Amount	Mit Cost				
	TOTAL LABO	R		1,021	,64				
	Direct			340	.0/	·			
	1-2-9			610	.02				$oldsymbol{\perp}$
	Other			71	.0 /				$\bot$
									_
	TOTAL MATE	CIAL		612	. 02				-
	Direct			0					$\perp$
	1-3-9			527	.019				$\perp$
	Other			28	00)				-
						· · · · · · · · · · · · · · · · · · ·			$\perp$
	TOTAL LABO	r & Materia	L	1,633	.06	<del></del>			+
• .				. 157					+
	APE			1,10/	, 0 4				+
-	(\$140.19 11591)								+
	Notural C	ed material		23	,60				+
			m2 \	0	٥				+
	special a	ervices (2	(NT.)	23	0				+
	tropay aran			0000					+
+	TOTAL COST		•	2757	./٥				+
	TOTAL SOLL	INT RECLAIS	en (the )	0.7	07/2				+
	TOTAL SOL	oni navimi.	ED (JARI)	27,	27630				$\dagger$
			Days Opera	tedt	(2)				†
			Druma Froc		O				†
			Dos. Condo	<del> </del>	0				†
· · · · · · · · · · · · · · · · · · ·			Lbs. Decan	<u> </u>	27,430				1
				4 Cascades	10 9/9				†
	-		Lbs. to A-	5 Cascades	18,868			1	
					0,165	·			1
	<u> </u>		<u> </u>						
									T
						,			$\Gamma$
	<u> </u>								I
X-885 (len'HR	) Y-12 DATA S	HEFT	,						T
- N-603 (Jan 40	I IZ DAIR G	TIGE !		•	•	1	•	•	•

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						ļ		
	•			MARCH	<b>-</b> 1959			
				ļ				
			S	Account Record	t 2686 Very Facilit			
					very recrisi		·	
				Amount	Unit Cost		1	
	TOTAL LAB	OR.		2,929	.047			
-	Direct			1,791	.029			
	1-2-9			994	.016			eg:
	Other			144	.002			·
-								
	TOTAL MATE	RIAL		363	.006			
	Direct			0	0			
. ————	1-2-9		<u> </u>	233	.004			
·	Other			130	.002			
-								
	TOTAL LABOR	& MATERIA	<u>t                                     </u>	3,292	.053			
		<u>,                                      </u>						
	APE			2,663	.042			
	TOTAL WORKE			32	.001			
	Natural Ga			32	.001			
	Special Se	rvices (27	91)	0	0			
	70747							
	TOTAL COST			5,987	.096			
	TOPAT COTTO	NIM TOWAR A TO	77 (70			· · · · · · · · · · · · · · · · · · ·		
-	TOTAL SOLVE	NT RECLAIM	GD (Lbs.)		62,664			
			Do- 0					
	-		Days Opera		13			
			Drums Proce		158			·
			Lbs. Conder		24,912			
			Lbs. Decant		37,752			
	·			Cascades:	62,664			
			u∪3. TO A-;	Cascades:	0			
WCX-885A (11-58) Y-12	2 Data Sheet							
		1	1		1		į.	

		-	So	Account	- 1959 2686 Pery Facilit	<b>-</b>		
				Amount	Unit Cost		Condensed Unit Cost	
				<u> </u>				
	TOTAL LABO	R .		2,929	.047		.118	
·	Direct			1.791	.029		1072	
	1-2-9			994	.016	·	.040	
	Other		-	144	.002		.006	
	TOTAL MATE	DTAY		<del> </del>	ļ			
	Direct	NIAL		363.	.006		.614	
-	1-2-9					,		
-	Other			233	.007		.009	·
	04.01			130	.002		.005	
•	TOTAL LABOR	& MATERIA		200-				<b>—</b> .
				3,292	, 0 5 3		./32	
	APE			2//2	. 40		1. 0	
				2,663	.042		. /07	<del></del> -
	TOTAL WORKS	D PATERIAL		32	00/			
	Natural Ga			32	.00/		.00/	 
	Special So	rvices (27	91)	0	0		. 60 /	 
		•		0				
	COTAL COST	<del></del>		5,987	. 0 /			
				J, 78 /	.096		.240	
	POTAL SOLVE	RT RECLAIM	ID (Lbs.)		(2,664			
		1	eys Operat	od t	/ 2		-	
			rums Proce		/3 /58 24912			 
-			bs. Conden		758			 
			bs. Decant		24912			 
			bs to A-4		37.752 62,664		`	 
			bs. to A-5		62,667			 
					U			
			-					 
-A (11-58) Y-1	2 Data Sheet							• • • •

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			G-1	APRIL - 1  Account 2  t Recovery	586	RE RE	DEIVED	4
			Solver	Amount	Unit Cos	t Con R.	23 (39 g	[-5] 2
							0	
	TOTAL LAB	)R		6,247	i			
	Direct			4,160	.022	· · · · · · · · · · · · · · · · · · ·		
•	1-2-9			1,361	.007	······································		
	Other			726	-004			
	TOTAL MAT	7DTΛT		627	.003	· · · · · · · · · · · · · · · · · · ·		
		31/17-17		0	0			
	Direct			193	.001			
	1-2-9 Other			434	.002			
	orner				• • • • • • • • • • • • • • • • • • • •			
<del></del>	TOTAL LAB	OR & MATERI	AL	6,874	.036			
							·	
	APE			5,970	.032			
						-		
	TOTAL WOR	CED MATERIA	L	99	.001			
	Natural	Gas		60	.0003			
	Special	Services (	2791)	39	-0002			
	TOTAL COS	1		12,943	069			
-								
·	TOTAL SOL	VENT RECLAI	MED (Lbs.)		186,506			
-								
<u> </u>			Days Opera		30			
			Drums Prod	essed:	423 <u>급</u>			
			Ibs. Conde		30,391			
k			Ibs. Decar	į	156,115			
			1	4 Cascades	1	<del> </del>		
			Ibs. to A	5 Cascades	: 176,897			
	-			1			-	
<u></u>								
P								
WCX-885A (11-58)	Y-12 Data Shaar	<u> </u>						
WCX-885A (11-58)	Y-17 TARIN PUGGI		1	l	i	1	1	1

	·	APRIL - 1	959		TO TO
		Account 2	686		727
	Solve				
		Amount	Unit Cost		1
				7112 0032	
TOTAL LABOR		6247	7 27	. 206	
		T			
		T			
		T T T T T T T T T T T T T T T T T T T			
TOTAL MATERIAL		1.27	1003	.021	
				_	
				. 006	
TOTAL LABOR & M	ATERIAL	6874	, 036	, 227	
APE		5970	.032	.196	
TOTAL WORKED MA	TERIAL	99	.001	,003	
Natural Gas		60		.002	
Special Servi	ces (2791)	39	,000%	,00/	
TOTAL COST		12,943	,069	,424	
TOTAL SOLVENT R	ECIAIMED (1bs.)		186,506		
	Days Open	ated:	30		
	Drums Pro	cessed:	4/235		
	lbs. Cond	ensed:	30 39/		
	Ibs. Deca	rted	156,115		
	Ibs. to A	4 Cancades	9.609		
	Lbs. to A	5 Cascades	: 176.897		
	_				
			·		
	APE  TOTAL WORKED MA  Natural Gas  Special Servi  TOTAL COST	TOTAL LABOR  Direct  1-2-9 Other  TOTAL MATERIAL  Direct  1-2-9 Other  TOTAL LABOR & MATERIAL  APE  TOTAL WORKED MATERIAL  Natural Gas Special Services (2791)  TOTAL COST  TOTAL SOLVENT RECIAIMED (1bs.)  Days Oper Drums Pro Lbs. Cond Lbs. Deca	Account 2 Solvent Recovery  Amount  TOTAL LABOR  Direct  1-2-9  Other  TOTAL MATERIAL  Direct  1-2-9  Other  TOTAL LABOR & MATERIAL  APE  TOTAL LABOR & MATERIAL  APE  TOTAL LABOR & MATERIAL  APE  TOTAL WORKED MATERIAL  Natural Gas  Special Services (2'(91)  TOTAL COST  TOTAL COST  TOTAL SOLVENT RECIAINED (lbs.)  Days Operated:  Drums Processed:  Ibs. Condensed:  Ibs. Condensed:  Ibs. Condensed:  Ibs. to A-5 Cascades	TOTAL LABOR	Account 2586 Solvent Recovery Facility  Amount Unit Cost Condensed Only Cost Cost Cost Cost Cost Cost Cost Cost

	1	1	ı	1	<b>)</b>	1	1	
				May -	1050			
			Sol	Account vent Recove	2686 ry Facility			
			·				·	
				Amount	Unit Cost			
	TOTAL LABO	R		5,638	.036		<u> </u>	
	Direct			3,338	.021			
***************************************	1-2-9			941	.006		·	
	Other			1,359	.009			
		<u> </u>						
	TOTAL MATE	RIAL		621	.004			
	Direct							
	1-2-9			558	•004			
<del></del>	Other			63	.000			
<del></del>								
	TOTAL LABOR	R & MATERIA	L	6,259	.040			
	APE			5,243	.033			
-	mom : T : I to D :				500			
	Natural G	ED MATERIAL		141	.001			
	<del> </del>			108	.001			
	Special Sc	ervices (27	91)	33	.000			
	TOTAL COST			11,724	.074			
******	TOTAL COST			11,124	.014			
·	TOTAL SOLVI	יוויי סטיר א דא	en (th. )		158,389			
	TOTAL SOLVI	PILL UPOTHTM	עם (LDS.)		170,707			
			Days Opera	ted.	30			
			Drums Prod		350			
			Lbs. Conde		20,327			
			Lbs. Decar		138,062	•		
				4 Cascades				
				5 Storage:				
			····					
		-						
WCX-885A (11-58) Y-	12 Data Sheet					,		

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•					050				-
				Mev -					
			Solv	ent becover	y Facility		·	•	
						•	Condensed		
				Amount	Unit Cost		Unit Cost		+
						<u> </u>	_		+
	TOTAL LABOR	}		5638	.036		, 277		+
	Direct			333%	02/		,169		+
	1-2-9			94/	.006		.094		+
	Other			1,359	.009		. 067		+
	COLUMN A W. A S. COLO.			1 21	.004		103/		十
	Direct	TAL		621			1.0,		
<u> </u>	1-2-9			558	.004		,628		T
	Other			43	- 0		,003		I
<u> </u>									$\perp$
	TOTAL LABO	& ATERIA		4,259	.340		.308		
									$\bot$
	AFE			5,243	.033		. 258		
									+
	TOTAL WOUK	D MATERIAL	,,	14/	,00/		. 00 7		+
	Natural C	as		\28	. 22/		: 665		+
	Special S	ervices (27	91)	3,3	_0-		. 602		+
					.0.1		107		-
	TCTAL COST			11,724	.074		.577		_
	momes gori	TELETI ENDOYATIA	co (Thu )		100 209				1
	TOTAL SOLV	THE RECLAIM	D (LOS.)		158,389				
			Days O or	ated:	37				
			Drum Pro		350				_
			The. Cond		25 327				_
			Lbs. Deca	u <b>t</b> ed	138,062				_
			Lbs. to A	4 Cascades	7,907			_	_
			Lbs. to A	5 Storage:	153, 485	•			-
									+
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				1					-
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					<u> </u>				
'X-885A (11-58)	Y-12 Data Sheet					ì	l	l	•

June - 1952   Account \$495     Solvest Recovery Facility   Amount   Unit Cost     TOTAL LABOR		1	ı	ſ	1	Y	•		
Account 8688 Solvest Recovery Facility Amount Unit Cost  TOTAL LABOR 6,237 .162 Direct 3,832 .100 1-2-9 1,234 .032 Cther 1,171 .030  TOTAL RETERIAL 991 .026 Direct -00- 1-2-9 775 .020 Cther 216 .006  TOTAL LABOR 8 MATERIAL 7,228 .188  AFE 5,959 .155  TOTAL LABOR 8 MATERIAL 150 .004 Natural Gas 117 .003 Special Services (2591) 33 .001  TOTAL COST 13,337 .347  TOTAL COST 13,337 .347  TOTAL SOLWENT RECLATED(Ibe) 38,397  Days Operated 31 .000  Drums Frocessed: 382									
Account 8688 Solvest Recovery Facility Amount Unit Cost  TOTAL LABOR 6,237 .162 Direct 3,832 .100 1-2-9 1,234 .032 Cther 1,171 .030  TOTAL RETERIAL 991 .026 Direct -00- 1-2-9 775 .020 Cther 216 .006  TOTAL LABOR 8 MATERIAL 7,228 .188  AFE 5,959 .155  TOTAL LABOR 8 MATERIAL 150 .004 Natural Gas 117 .003 Special Services (2591) 33 .001  TOTAL COST 13,337 .347  TOTAL COST 13,337 .347  TOTAL SOLWENT RECLATED(Ibe) 38,397  Days Operated 31 .000  Drums Frocessed: 382									
Solvent Recovery Facility   Amount   Unit Cost					June -	1959			
Solvent Recovery Facility   Amount   Unit Cost					Account	D686			
TOTAL IABOR				Solve	nt Recovery	Facility	†		
TOTAL IABOR					A	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,			
Direct   3,832   .100					Amount	Unit Cost			ļ
Direct   3,832   .100	<del> </del>	BORAT TADO	<u> </u>		( 007	5/0			-
1-2-9	<del></del>	1	τ		1				
Cther		† <del></del>			7	<del>                                     </del>			
TOTAL BATERIAL   991   .026     Direct  0-   .0-0     1-2-9   775   .020     Cther   216   .006     TOTAL LABOR & MATERIAL   7,228   .188     AFE   5,959   .155     TOTAL WORKED MATERIAI   150   .004     Natural Cas   117   .003     Special Services (2791)   33   .001     TOTAL COST   13,337   .347     TOTAL COST   13,337   .347     TOTAL SCLUENT REGIATRED(Ibs)   38,397     Days Operated   31	44			<del> </del>	,				<del>                                     </del>
Direct	-	Collet		<u> </u>	1,171	.030			
Direct		JUNE AT MY THE	PTAT	-	007	026		<b></b>	
1-2-9					<del> </del>			<del> </del>	<del>  </del>
Cther	<del></del>				<del>                                     </del>				
TOTAL LABOR & MATERIAL 7,228 .188  AFE 5,959 .155  TOTAL WORKED MATERIAL 150 .004  Natural Gas 117 .003  Special Services (2791) 33 .001  TOTAL COST 13,337 .347  TOTAL SCLVENT RECLAIRED(Ibs) 38,397  Days Operated 31					<del> </del>				
APE 5,959 .155  TOTAL WORKED MATERIAL 150 .004  Natural Gas 117 .003  Special Services (2791) 33 .001  TOTAL COST 13,337 .347  TOTAL SOLVENT RECLAIMED(Lbs) 38,397  Days Operated 31		otner	-	<u> </u>	216	.006		ļ	
APE 5,959 .155  TOTAL WORKED MATERIAL 150 .004  Natural Gas 117 .003  Special Services (2791) 33 .001  TOTAL COST 13,337 .347  TOTAL SOLVENT RECLAIMED(Lbs) 38,397  Days Operated 31	<del></del>	MOMAT TARO	0 10 0000		7 000	n d d		<u> </u>	
TOTAL WORKED MATERIAI 150 .004  Natural Gas 117 .003  Special Services (2791) 33 .001  TOTAL COST 13,337 .347  TOTAL SCLVENT RECIAINED(Ibs) 38,397  Days Operated 31		TOTAL LABO	R & MATERIA	<u> </u>	7,228	•188			
TOTAL WORKED MATERIAI 150 .004  Natural Gas 117 .003  Special Services (2791) 33 .001  TOTAL COST 13,337 .347  TOTAL SCLVENT RECIAINED(Ibs) 38,397  Days Operated 31		AFTS							
Natural Gas		APE			5 <b>,9</b> 59	.155			
Natural Gas	-								·
Special Services (2791)   33 .001					150	.004			
TOTAL COST 13,337 .347  TOTAL SOLVENT RECLAINED(Ibs) 38,397  Days Operated 31 www. Drums Processed: 382  Libs. Condensed: 23,384 www. New Years force Libs. Decanted: 15,013 www. Libs. to A Cascades: 14,289  Libs. to A Storage: 24,108  Total Ibs. Recovered to Date: 2,435,345 www.					117	.003			
Days Operated 31 wary Drums Processed: 382 Lbs. Condensed: 23,384 wary served page Lbs. Decanted: 15,013 wary Lbs. to A- Cascades: 14,289 Lbs. to A-5 Storage: 24,108 Total Ibs. Recovered to Date: 2,435,345 wary		Special S	ervices (27	91)	33	.001			
Days Operated 31 wary Drums Processed: 382 Lbs. Condensed: 23,384 wary served page Lbs. Decanted: 15,013 wary Lbs. to A- Cascades: 14,289 Lbs. to A-5 Storage: 24,108 Total Ibs. Recovered to Date: 2,435,345 wary									
Days Operated 31		TOTAL COST			13,337	.347			
Days Operated 31									
Days Operated 31 warmy Drums Frocessed: 382  Lbs. Condensed: 23,384 warmy xerous page Lbs. Decanted: 15,013 warmy Lbs. to A-4 Cascades: 14,289  Lbs. to A-5 Storage: 24,108  Total Lbs. Recovered to Date: 2,435,345 warmy	****	TOTAL SOLV	ENT RECLAIN	ED(Lbs)		38,397			
Drums Frocessed: 382  Lbs. Condensed: 23,384  Lbs. Decanted: 15,013  Lbs. to A-4 Cascades: 14,289  Lbs. to A-5 Storage: 24,108  Total Ibs. Recovered  to Date: 2,435,345  Total Cascades: 2,435,345								·	
Lbs. Condensed: 23,384 Wany Serect Page Lbs. Decanted: 15,013 wany Lbs. to A-4 Cascades: 14,289 Lbs. to A-5 Storage: 24,108 Total Lbs. Recovered to Date: 2,435,345 wany	-		M	Days Opera	ed	31	www		
Lbs. Decanted: 15,013   Ving				Drums Proce	ssed:	382			
Lbs. to A-4 Cascades: 14,289  Lbs. to A-5 Storage: 24,108  Total Lbs. Recovered  to Date: 2,435,345 wmy				Lbs. Conde	nsed:	23,384	Money-Secret	t page	
Ibs. to A-5 Storage: 24,108  Total Ibs. Recovered  to Date: 2,435,345			~	Lbs. Decan	ted:	15,013	wing		
Total Ibs. Recovered  to Date: 2,435,345 wmy				Lbs. to A-	Cascades:	14,289			
to Date: 2,435,345 wmy				Lbs. to A-	Storage:	24,108			
				Total Ibs.	Recovered				
				to Date		2,435,345	mond		
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WCX-885A (11-58) Y-12 Data Sheet			-						
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WCX-885A (11-58) Y-12 Data Sheet			***						
	WCX-885A (11-58) Y-	12 Data Sheet							

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•		,		June -	1959			
			0.3	Account	2686			
			POTAGE	t Recovery	racility			
				Amount	Unit Cost		Condensed Unit Cost	
	TOTAL LABO	R .		4,237	./63		.248	
	Direct			3, 832	.063	·	.152	
	1-2-9			1,234	.020		. 649	
	Other			1,171	.020		. 647	
		· · · · · · · · · · · · · · · · · · ·						
	TOTAL INTE	RIAL		99/	016		.040	
	Direct				-		1	
<u></u>	1-2-9			7.75	.013		.031	
	Other			216	.003		.009	
	TOTAL LABO	R & MATERIA	7.	722	.119		, 288	
				7228	117,		, 200	
	AFE			5,959	.099		. 237	
	TOTAL WORK	d ateriai		150	.002		.006	
	Natural G	ກລ		117	.012		که ه .	
	Special S	ervices (27	91)	33	. oc 0		,00/	·
	TOTAL COST		·	/3,337	,220		.531	
	TOTAL SCLV	GIN RECLAIN	ED(Lbs)		60,493	·		
				•				
			Days Operat Drums Froce		30			
			Lbs. Conder		382	/		
•			Lbs. Decan		25,140	1		
			The to A-		35,353 			
-			Lbs. to A-		60,493			
			Total Ibs.		<i></i>			
			to Date:		-2,435,345			
					2,435,345 2,396,948	V		
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:-885A (11-58) Y-	12 Data Sheet							

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						<u>- 1959</u>				
				S	Account Reco	t 2686			į	
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-					Amount	The state of a				
			+		Alloune	Unit Cos	814 /0Î-7	4		4
	TOTAL LAB	OR.			5,694	.148		Abeni de la	<u> </u>	$\dashv$
	Direct				4,017	.105	10	Van market		$\dashv$
	1-2-9				845	.022	+		1	$\dashv$
•	Other				832	.021				$\dashv$
										+
	TOTAL MAT	RIAL			300	.008				+
-	Direct				-0-	-0-				$\dagger$
	1-2-9				123	.003				$\dagger$
	Other				177	.005				+
-									<del>                                     </del>	$\dagger$
	TOTAL LAB	OR & MATER	IAL		5 <b>,9</b> 94	.156				$\dagger$
	APE				5,799	.151		-		
										$\dagger$
	TOTAL WORL	CED MATERIA	L		205	.005				†
	Natural (	as			147	.004				$\dagger$
	Special S	ervices (2	791)		58	.001				十
										†
	TOTAL COS	1	<u></u>		11,998	.312				T
										T
	TOTAL SOL	ENT RECLAI	MED (	lbs)		38,397				†
										T
			Days (	Opera	ed:	31				T
		<del></del>	Drums	Proce	ssed:	386				T
			Lbs. (	Conde	sed	23,384				T
			Lbs. I	Decant	ed:	15,013				
			Lbs. 1	To A-2	Cascades:	14,289				
			Lbs. t	to A-5	Storage:	24,108				Γ
			Total	Lbs.	Recovered					
			to I	Date:		2,435,345	V			
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WCX-885A (11-58) Y-12	Data Sheet	ļ				<u> </u>				

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			July -	1959			
		So1	vent Recov	ry Facility	•		
			Amount	Unit Cost		Condensed Unit Cost	
				1.46			
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				1			
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Other			832	. 021		,035	
TOTAL 'AT	RIAL		300	.008	<del></del>	. 6/3	
Direct				- 0		-	
1-2-9				,003	······································	.065	
Cther			177	.005		.008	
TOTAL LAB	P & MATERI	/L	5,99+	.154		,256	
APE			5,799	.15/		.218	
TOTAL WOR	PD TATERIA	l,	205	. 005		. 009	
Natural (	ចន	· ·	147			:006	
Special	ervices (2	791)	58	. 00/		,093	
TOTAL COS			11,998	, 3/2		1.5/3	
				50 611			
TOTAL SOL	TENT RECIAL	ÆD (lbs)		38,37/			
				7.1	<del></del>		
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		Dy ( Ia x 1	(1)				
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	Direct 1-2-9 Other TOTAL MATE Direct 1-2-9 (ther TOTAL LABO APE TOTAL WORN Natural Special S	Other  TOTAL MATERIAL  Direct  1-2-9  ('ther  TOTAL LABOR & MATERIA  APE  TOTAL WORKED MATERIA  Natural Cas  Special Services (2  TOTAL SOLVENT RECIAI	TOTAL LABOR  Direct  1-2-9 Other  TOTAL WATERIAL  Direct  1-2-9 Cther  TOTAL LABOR & WATERIAL  APE  TOTAL LABOR & WATERIAL  Natural Cas Special Services (2791)  TOTAL COST  TOTAL SOLUTION RECIAL ED (1bs)  Days Operat Drums Proce Lbs. Decant Lbs. Decant Lbs. To A-A Lbs. to Date:	TOTAL LABOR  Direct  1-2-9  Other  TOTAL WATERIAL  Direct  1-2-9  (Ther  TOTAL MATERIAL  APE  TOTAL LABOR & MATERIAL  APE  TOTAL LABOR & MATERIAL  Solvent Recovered  TOTAL MOTERIAL  Solvent Recovered  Days Overaged:  Drums Processed:  Ibs. Condensed  Lbs. Decanted:  Total Lbs. Recovered  Total Lbs. Recovered  Total Lbs. Recovered  Total Lbs. Recovered  Total Lbs. Recovered  Total Lbs. Recovered	TOTAL LABOR	Solvent Peccery Facility   Amount   Unit Cost	Solvent Recovery Facility   Condensed   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost

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				August	- 1959				
			So	olvent Reco	nt 2686 very Faci	lity			
				Amount	Unit (	Cost	and the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of th		
	TOTAL LABOR		_	5 050				).	
	Direct			5,253	.132	1/3/	11/2	1	
	1-2-9			3,709	.093		RE EIVED		
	Other			447	.011	<del>- 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1</del>	1 1 2 3 1 2	s	
				1,097	.028	17.57	$T_{X}$	4	
	TOTAL MATER	TAT.		0/5		-			
	Direct			865	.022		6111		
_	1-2-9				-0-				
	Other			682	.017				
				183	.005				
***************************************	TOTAL LABOR	& MATERI	A	6,118	751				
		G. PATEMET	BL -	0,110	.154				
	APE		<del> </del>						
				5,432	.136				
	TOTAL WORKE	D MATERIA:		7(0				<del> </del>	
	Natural Gas		U ·	168	.004				
	Special Ser		707)	140	.004				
	Prozes Do	VICES (Z	(AT)	28	.000				
	Total Cost	<del></del>		77 770					
				11,718	. 294				
	TOTAL SOLVE	TO DECTATA	47D (21 )						
		AT THIOTHTI	TD (TDS)		ļ	39,890		ļ	
			Down O	<u> </u>	ļ			<del></del>	
			Days Opera		ļ .	31			
			Druis on I	and - Begi	nning:	1,216	203	<b></b>	
			Drums Prod	and - Endi	ng:	1,013	4	<del> </del>	
		2		essed: sferred to	02.20	368	203	<b></b>	
					81-10:	165	<del></del>	<u> </u>	
			Los. Conde			28,268			
			Lbs. Decar			11,622			
				4 Cascades		34,890			
		_		5 Storage:		5,000			
			Total Lbs.	Kecovered	to Date:	2,475,235	V		
					·				
WCX-885A (11-58) Y	-12 Data Sheet								
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		,		August -	1959			
				Account				*
			Solv	ent Recover	y Facility			
				Amount	Unit Cost		Condensed Unit Cost	
······································								
	TOTAL LABOR			5,253	./32		. 186	
<del></del>	Direct		· ·	3,709	.093		./3/	
	1-2-9			447	. 0//		016	
· · · · · · · · · · · · · · · · · · ·	Other			1,097	. 028	·	.039	<u> </u>
	TOTAL MATER	IAL		865	.022		. 031	
	Direct							
· · · · · · · · · · · · · · · · · · ·	1-2-9			682	. 0/7		.024	
	Other			183	.005		. 007	·
	TOTAL LABOR	& MTERIA	L	4.118	.154		.2/7	
	APE			5432	./34		,192	
•	TOTAL WORKS	D MATTER TAT		168	.004		. 006	
·	Natural Ga			148			.005	
	<del></del>	rvices (27	91)	28	.007		.00/	
	Total Cost			11,718	.294		. 415	
				,				
· · · · · · · · · · · · · · · · · · ·	TOTAL SOLVE	INT RECLAIM	ED (lbs)			39,890		
			Days Opera	ted:		3/		
*** ***			Drums on I	and - Begi	nning:	1216		
			Drums on I	and - Endi	ng:	1013		
			Drums Prod	essed:		368		
			Drums Trai	sferred to	81-10:	165		
			Lab. Conde	nsed:		28268		
			Lbs. Decm	ted:		11,622		
			Lbs. to A.	4 Cascades		34890		
			Lbs. to A.	5 Storage:		5,000		
			Total Lbs.	Recovered	to Date:	2,475,235		
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						1	]	

Septembor - 1959   Account 2686   Solvent Recovery Facility   Amount Unit Cost		1	1	1		Ĭ	1	t	
### Solvent Recovery Facility  #### Account Unit Cost  #### Cost  ### Direct  ### 1,120  ### 1,120  ### 1,120  ### 1,120  ### 1,120  ### 1,120  ### 1,120  ### 1,120  ### 1,120  ### 1,120  ### 1,120  ### 1,120  ### 1,120  ### 1,120  ### 1,120  ### 1,120  ### 1,120  ### 1,120  ### 1,120  ### 1,120  ### 1,224  ### 1,224  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234  ### 1,234							1		
### Account 2686   Solvent Recovery Facility									
Solvent Recovery Facility   Amount Unit Cost	, •• <b>4</b>				_				
Amount   Unit Cost				Sol	Accour	t 2686			
TOTAL IABOR 5,916 .128  Direct 4,071 .088  1-2-9 725 .016  Cther 1,120 .024  TOTAL MATERIAL 919 .020  DirectCC-  1-2-9 707 .015  Cther 212 .005  TOTAL IABOR & MATERIAL 6,835 .148  AFE 6,810 .148  TOTAL IABOR & MATERIAL 131 .003  Natural bas 131 .003  Special Services (2791) -CC-  TOTAL CCST 13,776 .299  TOTAL SOLVERT RECLARED (1bs.) 46,146  Druss on Hand - Endirg: 725  Druss on Hand - Endirg: 725  Druss on Hand - Endirg: 725  Druss Transferred to 81-10: 28					100000	J racerro	1	8 Company of the second second	
TOTAL IABON   5,916   .128   .128   .129					Amount	Unit Cost		(6) JE	$\mathcal{A}_{i,j}^{k}$
Direct	<del></del>						j		Δ,
1-2-9		TOTAL LABO	<u> </u>		5,916	.128	/:	200	
Cther		1	ļ		4,071	.C88	<u>l</u>	1 6 1 12	
### COTAL MATERIAL 919 .020    Direct						.016			
Direct		Other	<u> </u>		1,120	.024		y's	
Direct	•							1.7	1
1-2-9		OTAL MATER	IAL		919	.020			
Other		Direct			-0-	-0-			
TOTAL IABOR & MATERIAL 6,835 .148  AFE 6,810 .148  TOTAL WORKED MATERIAL 131 .003  Natural cas 131 .003  Special Services (2791) -00-  TOTAL CCST 13,776 .299  TOTAL SOLVENT RECIATED (1bs.) 46,146  Days Operated: 30  Drums on Hand - Beginning: 1,013  Drums on Hand - Ending: 725  Drums Processed: 316  Drums Transferred to 81-10: 28	<del></del>	1			707	.015			
AFE 6,810 .148  TOTAL WORKED MATERIAL 131 .003  Natural Gas 131 .003  Special Services (2791) -CC-  TOTAL CCST 13,776 .299  TOTAL SOLVENT RECLAIRED (1bs.) 46,146  Days Operated: 30  Drums on Hand - Beginning: 1,013  Drums on Hand - Ending: 725  Drums Processed: 316  Drums Transferred to 81-10: 28		Other			212	.005			
AFE 6,810 .148  TOTAL WORKED MATERIAL 131 .003  Natural Gas 131 .003  Special Services (2791) -CC-  TOTAL CCST 13,776 .299  TOTAL SOLVENT RECLAIRED (1bs.) 46,146  Days Operated: 30  Drums on Hand - Beginning: 1,013  Drums on Hand - Ending: 725  Drums Processed: 316  Drums Transferred to 81-10: 28	-								
TOTAL WORKED MATERIAL 131 .003  Natural Gas 131 .003  Special Services (2791) -00-  TOTAL CCST 13,776 .299  TOTAL SOLVENT RECLAIRED (1bs.) 46,146  Days Operated: 30  Drums on Hand - Beginning: 1,013  Drums on Hand - Ending: 725  Drums Processed: 316  Drums Transferred to 81-10: 28		TOTAL LABO	R & MATERIA	L	6,835	.148			
TOTAL WORKED MATERIAL 131 .003  Natural Gas 131 .003  Special Services (2791) -00-  TOTAL CCST 13,776 .299  TOTAL SOLVENT RECLAIRED (1bs.) 46,146  Days Operated: 30  Drums on Hand - Beginning: 1,013  Drums on Hand - Ending: 725  Drums Processed: 316  Drums Transferred to 81-10: 28									
Natural Gas   131	<del></del>	APE			6,810	.148			
Natural Gas   131									
Special Services (2791)		TOTAL WORK	ED MATERIAI		131	.003			
TOTAL CCST 13,776 .299  TOTAL SOLVENT RECLAINED (1bs.) 46,146  Days Operated: 30  Drums on Hand - Beginning: 1,013  Drums on Hand - Ending: 725  Drums Processed: 316  Drums Transferred to 81-10: 28		Natural	Gas		131	.003			
TOTAL SOLVENT RECIAINED (lbs.)  Days Operated:  Drums on Hand - Beginning:  Drums on Hand - Ending:  Drums Processed:  Drums Transferred to 81-10:  28		Special	ervices (2	791)	-C-	<b>-</b> 0-			
TOTAL SOLVENT RECIAINED (1bs.)  Days Operated:  Drums on Hand - Beginning:  Drums on Hand - Ending:  Drums Processed:  Drums Transferred to 81-10:  28									
Days Operated: 30		TOTAL COST			13,776	. 299			
Days Operated: 30									
Drums on Hand - Beginning: 1,013		TOTAL SOLV	ENT RECLAIM	ED (lbs.)			46,146		
Drums on Hand - Beginning: 1,013									
Drums on Hand - Ending: 725				Days Opera	ted:		30		
Drums Processed: 316 Drums Transferred to 81-10: 28				Drums on H	ınd - Begir	ning:	1,013		
Drums Transferred to 81-10: 28				Drums on H	and - Endin	g:	725		
	W			Drums Proc	es <b>s</b> ed:		316		
Lbs. Condensed: 24.037	-			Drums Trans	ferred to	81-10:	28		
				Lbs. Conde	nsed:		24,037	:	
Lbs. Decanted: 22,109				Lbs. Decan	ted:		22,109		
Ibs. to A-4 Cascades: 23,055				Lbs. to A-	Cascades:		23,055		
Lbs. to A-5 Storage: 23,091	-			Lbs. to A-	Storage:		23,091		
Total Lbs. Recovered to Date: 2,521,381 V			-	Total Lbs.	Recovered	to Date:	2,521,381	V	
WCX-885A (11-58) Y-12 Data Sheet	WCX-885A (11-58) Y-	12 Data Sheet							

		Sep <b>tembor</b>	1959	,			
•		Veconi.					
	Solv	ent Rocove	y Facility				
					Condensed		ļ
	·	imount	Unit Cost		Unit Cost		-
			_				<del> -</del> -
TOTAL IABOR		5,916	./28		. 296		-
Direct		4,071	.088		.169		-
1-2-9		725	.016		. 030		+
Other		1,120	.024		. 047		+
TOTAL MATERIAL		010	. 7 ^	·	A 2 ()		+
Direct		919	.020		.038		+
1-2-9		7.7	. 15		.029		+
Other		707 212	. 0/5		.009		<b>†</b>
		210	, 000				
TOTAL LABOR & 3	WIERIAL	6.835	. 148		. 284		ŀ
		10,000					
AFE		6.810	,/48		. 283		
							<u>.</u>
TOTAL WOPKED W	TERIAL	13/	.003		,006		_
Natural Cas		/3/	.003		.006		+
Special Servi	lces (2791)						+
						<u> </u>	+
TOTAL COST		13,776	.299		, 573		+
	PROTATION (1)						+
TOTAL SOLVERT	RECIAINED (1bs.)		<u>                                     </u>	46,146			+
	Days Opera	tedi		2.			+
	Drums on H		nningi	36			+
		und - Endi		10/3			$\top$
	Drung Proc	<del> </del>		316			1
		pferred to	81-10:	28			
	Lbs. Conde	<u> </u>		24,037			
	Ibs. Decar	ted:		22,109			
	Ibn. to A-	Cascades	1	23,055			
	Lbs. to A-	Storage:		23,091			4
	Total Lbs.	Recovered	to late:	2,521,381			
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			<u> </u>		<u> </u>		+
X-885A (11-58) Y-12 Data Sheet							

	ı		3	1	ì	,		
				October -	1959			
				Account	2686		·	
	,		Sol	ent Recove	ry Facility	1		
				Amount	Unit Cost			
	momar rane			. (50				
	TOTAL LABOR	į.		4,633	.156			
•	Direct			2,637	.088			
•	1-2-9			1,470	•050	,		
~	Other			526	.018	**		
<del>~ : </del>						·	7 ) 22	
	TOTAL MATER	IAL		457	.016			٠,
•	Direct			-0-	-0-		./ a. X. M.	
	1-2-9			325	.011		1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	
	Other			132	.005			
•								
	TOTAL LABOR	& MATERIA	L	5,090	.172			
	APE			3,720	.125			
	TOTAL WORKE	D MATERIAL		139	.005			
	Natural (			139	.005		<b>†</b>	
		ervices (2	791 )	-0-	-0-			
			, , _ ,					
	TOTAL COST			8,949	202			
	20112 0001			0,949	.302			
	MORAT COLUM	NO DOCTATA	an (a)			00 (()		
	TOTAL SOLVE	MI RECLAIM	PD (IDS.)			29,664		
			n ^	1 - 3 -				
			Days Opera			20		
		·		and - Begi	i .	725		
				and - Endi	ng:	747		
			Drums Prod			108		
				sferred to	81-10:	130		
			Lbs. Conde	nsed:		8,166		
			Lbs. Decar	ted:		21,498		
			Lbs. to A-	4 Cascades		-0-		
			Lbs. to A-	5 Storage:		29,664		
		-	Total Lbs.	Recovered	to Date:	2,551,045	$\checkmark$	
WCX-885A (11-58) Y-	12 Data Sheet							
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4				-				
				October -	1959			
<u>*</u>				Account				·
			Solv	ent Recover	y Facility			
		·		Amount	Unit Cost		Condensed Unit Cost	
							DATE COSE	
	TOTAL LABOR			4,633	. 156		. 547	
<del></del>	Direct			2,637	. 088		.323	
	1-2-9			1,470	. 050		. 180	
	Other			526	. 0/8		. 644	
	TOTAL MATE	IVL		157	. 016		. 656	
	Direct					,		
	1-2-9			325	011		.040	
	Other			132	,005		.016	
	TOTAL LABOR	& MATERIA	L	5,098	.172		. 623	
* ***	AFE			3,720	. 125		.456	
					- 54			ļ
	TOTAL WORKS	D MATERIAL		139	. 005		.017	
	Hatural (	<del> </del>		139	.005		.017	<u> </u>
	Special S	ervices (2	791)				-	<u> </u>
	TOTAL COST			8,949	.382		1.096	
	TOTAL SOLV	HT RECLAIM	ED (1bs.)			29,664		<del>                                     </del>
						2		
			Days (perc	1		20		
			1	and - begi	T	725		-
			Drums Frod	and - Endi	4 e; •	747	<u> </u>	
				<del></del>	d3 10.	108		
			Lbs. Conde	sferred to	01-101	130		
				<del> </del>		2/66		
	-		Ibs. Docu	4 Cascades		21, 498	<del>                                     </del>	
-			ļ	5 Storage:		29,66A		
			<del> </del>	Focovered		I .	<del>                                     </del>	+
			TOULL LUS.	. recovered	1 00 14001	2,551,045	<u>'</u>	
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(-885A (11-58) \	(-12 Data Sheet	÷		1	1	1	1	1

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			November	1959			
			Account	2686			
		Sc	vent Reco	very Facili	-ty		
			Amount	Unit Cost	t.		
	*	<del> </del>	2,537	.128		$\rho$	194
			0				Mr. V
			2,537	.128		1 10 10 2	}
Other			-0-			1 4 A	Th.:
						MX_	1 /3/
	RIAL		1,356	.068		177.7	
Direct			-0-				
1-2-9			1,349	.068			
Other			7				
TOTAL LABO	R & MATERI	L	3,893	.196			
APE			2.375	-120			
TOTAL WORK	ED MATERIA	l,	71/	707			
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	061 (1000	171/	1.2	·UUL			
TOTAL COST	1		7 000	2777		<del></del>	
120,222	<del>                                     </del>		6,200	.317		<del> </del>	
monat goty	ADENTA DENTAT	777 (3ha )		-	70.000	<b>  </b>	
101BD GODA	ENT RECEAL	ED (IDS.)	<b></b>		19,820	-	
+	<del>                                     </del>	<b></b>		-		<del>                                     </del>	
				-	-0-		
-	1	· T			747		
+			·	<u>rg:</u>	1,024		
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1			f	81-10:	277		
	· ·	Lbs. Conde	nsed:		-0-		
		Lbs. Decan	ted:		19,820		
		Lbs. to A-	4 Cascades	f	19,820		
					-0-		
	!					V	
	Direct 1-2-9 Other  TOTAL MATE Direct 1-2-9 Other  TOTAL LABO APE  TOTAL WORK Natural Special TOTAL COST	Other  TOTAL MATERIAL  Direct  1-2-9 Other  TOTAL LABOR & MATERIA  APE  TOTAL WORKED MATERIAL  Natural Gas  Special Services (;  TOTAL COST  TOTAL SOLVENT RECIAI  TOTAL SOLVENT RECIAI	TOTAL IABOR  Direct  1-2-9 Other  TOTAL MATERIAL  Direct  1-2-9 Other  TOTAL LABOR & MATERIAL  AFE  TOTAL LABOR & MATERIAL  Natural Gas Special Services (2791)  TOTAL COST  TOTAL SOLVENT REGIATED (1bs.)  Days Opera Drums on H Drums on H Drums on H Drums Tran Lbs. Gonder Lbs. Decar	Account Solvent Reco  Amount  TOTAL IABCR Direct 1-2-9 2,537 Other -0-  TOTAL MATERIAL 1,356 Direct -0- 1-2-9 1,349 Other 7  TOTAL LABCR & MATERIAL 3,893  AFE 2,375  TOTAL WORKED MATERIAL Natural Gas 1 Special Services (2791) 13  TOTAL COST 6,280  TOTAL SOLVENT RECIATED (lbs.)  Days Operated: Drums on Hand - Endir Drums Transferred to Lbs. Gondensed: Lbs. to A-4 Cascades Lbs. to A-5 Storage:	Account 2686   Solvent Recovery Facilia   Amount   Unit Cost	Account   2686   Solvent Recovery Facility	Account 2686   Solvent Recovery Facility

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•					!	1			
,	·			November -	1959				
				Account					
			50	vent Pecov	ery Facili	ty _.			
				Amount	Unit Cost				
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	TOTAL LABO	(1)		2,537	.128				<b></b> -
	Direct			-0-			L		<del> </del>
	1-2-9			2,537	128				<del>                                     </del>
	Othor			_0-					<del> </del>
	TOTAL MATE	\ T + T							-
	Direct	INL		1,356	.068	1,000			<del> </del>
-	1-2-9			-1-	-				-
	Cther	· · · · · · · · · · · · · · · · · · ·		1,349	.068				<del>                                     </del>
	00/101			7					
	TOTAL IABO	e & Materia	L	7097	.196				
·				3,893	1.76	<u> </u>			$\top$
	AFE			2,375	./20				一
				<u> </u>	. /2-			,	
	TOTAL WORK	ED IMPERIAL		14	. 001				
	Natural	Gas		/	_				
	Special	ervices (;	791)	13	,001				
	MONTH OCET			6,280	. 3/7				
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	TCTAL SOLV	EMT PECIAL!	ED (lba.)			19820			<del> </del>
									┼
			Days Opera			- 0.			-
		<u> </u>	Drums on H	<del></del>		747			+-
			bruce on B		<b>!</b>	1,024		<del> </del>	+
<del></del>			Orums Froc	<u> </u>	(13. 3.0)	-0-			+
			Drums Trans	<u> </u>	81-10:	277			+-
			The Condo	<u> </u>		-0- 10 87 0			-
			Lbs. Decan	<del> </del>		19,820			+
			1	Storage:	•	19,820			+
-			Total Lbs.	<del> </del>	+ D-+-:	2570,865		<del>                                     </del>	+
_			- ACT TD8.	recovered	LO DUTE.	23/4,003			1
									$\top$
285A (11 E0) 3	Y-12 Data Sheet	1			<u> </u>	<del>                                     </del>			1
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				December	1959			
					t 2686			
			So	olvent Reco	very Facil	ity		
				Amount	Unit Co			
					01110 00:	3 4		
	TOTAL LAN	30R		2,752	.056			
	Direct			1,559	.032			
	1-2-9			912	.018			
	Other			281	.006			
	TOTAL MATE	HIAL		272	.006			
	Direct						<del>                                     </del>	+
	1-2-9			84,	.002			+
	Other			188		<del> </del>		<del> </del>
				1 200	.004	<u> </u>		<del> </del>
	TOTAL LABO	R & MATERI	At.	3,024	.062			+
				7,024	.002	<del></del>		
	APE			2,470	.051			
				2,410	.001			
	TOTAL WORK	BD MATERIAL		78	.001			
	Natural	7		58			<del></del>	
		ervices (2	2791 )	20	.001		-	
		70111000 (2	1727	20				
	TOTAL COST			5 572	1 77,	<u> </u>		
	20232 0001			5,572	.114			
	TOTAL SOLIA	NO DOCTOR	(BD /22 )					<u> </u>
	TOTAL SOLVI	THE VECTATIV	En (TDS.)			43,842	<del> </del>	
****			h 0					
			Days Cperat		<del> </del>	4		
			Drums on Ha			1,024		
			Drums on Ha		g:	1,069	<del> </del>	
	1/19		Drums Proce		<u></u>	186	<del> </del>	
		. 31	Drums Trans		RT-10:	231		
, f			Lbs. Conder			5,901	<u> </u>	
		<i>,</i>	Lbs. Decant			42,941		
	1	<u>,                                      </u>	Lbs. to A-A			25,306		
	130	/ •/	Lbs. to A-9			23,536		
	7	<u> </u>	Total Lbs.	Recovered	to Date:	2,619,707	V	
WCV SSEA (44 TC)	2.40 5			***				
WCX-885A (11-58)	r-12 Data Sheet	ļ		į			ļ	T

	1 (	1	-					
•								
•				December -	1959			
				Account				
			Sol	vent Recove	ry Facilit			
•					Italia Camb		condensed	
			'	Amount	Unit Cost		Unit Cost	
· · · · ·	momar value	·		2000			411	
	TOTAL IABO	K .		2,752	. 054		.446	
	Direct			1,559	.032	· · · · · · · · · · · · · · · · · · ·	.264	
	1-2-9			9/2	.006		, 155	
	Other			28/	. 0 0 0	·	. 047	
·· <u></u>	TOTAL MATER	тат		272	. 006		.044	
	Direct	TVD		2/0	. 000			
	<u> </u>			D.A	.002		.014	
	1-2-9 Other		<u> </u>	84 188	.004		. 032	
	Other			108	,007		.052	
	MOWAY TANOT	g ammintation		3,02-4	, / 2		. 512	
	LOTAL LYBOL	& MATERIA	•	3,027	.062		13,0	1
	AFE			2,470	. 051		. 419	
	AFE			2,770	. 021		, ///	
	TOTAL WORKE	D MATERIAL		78	.001		. 0/3	
	Natural C	<u> </u>		58	.001		: 0/0	
	- <del></del>	ervices (2	vo1 )	20			,003	
	ripocial .	0171003 (2	711					
	TOTAL COST			5,572	. 114		.944	
	ICINE OWI			9,0,0	- 117			
	memat sour	NT RECLAIM	TD (1hc )			48,842		
	TOTAL SOLES	111 103033113	108.7	-		7.6/8.7 =		
	<u> </u>		Days Operat	ad.		4		
				nd - Begin	ing:	1,024		
			T `	and - Ending		1,069		
		† · · · · · · · · · · · · · · · · · · ·	Drums Froce			186		
				Cerred to	81-10:	231		
			Lbs. Conder			5,70/		
			bs. Decan			12,7+1		
			<del></del>	Cascades		25,30le		
			<del></del>	Storage:		23,534		
		-		Pecovered	to Date:	2,6/9,70	1	
- <del></del>								
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		Sol	vent Recov	-	i i			
	·				Total Irod	<b>L</b>	Condensed	
				Amount	Unit Cost		Unit Cost	
	momar Tatio	· •		241	25/	· · · · · · · · · · · · · · · · · · ·	,344	
	TOTAL LABO	n		2,43/	.056		,250	
	Direct	<del></del>		1,669			.072	
	1-2-9			482 280	. 0//		192	
	Other			280	. 807		. 0, 0	
	TOTAL MATT	RIAL		478	, 0//		. 071	
	Direct			0-	_``		<u>.</u>	
	1-2-9			314	.607		647	
	Other			164	,604		,024	
	TOTAL LABO	r & hateri	AL	2,909	,067		.435	
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	VIE		<b></b>	2.568	.059		.384	<u> </u>
				<u> </u>	<del> </del>			
	TOTAL MOT	ED MATERIA		23	.00/		.003	<del> </del>
	Matural	Gos	<u> </u>					ļ
	Special	Services (	2791)	23	.00/		,003	
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	TOTAL COS	<u> </u>		5500	127	·	. 822	-
						12.276		
	TCTAL SOL	EIT RECIAI	ED (1bs.)			43,372		<del> </del>
						2 /		<del>                                     </del>
1			Days Oper	1		2/ 555		
_				and - Begi	i	590	<del> </del>	1
				lland - Endi	-44g *	103		1
		<del> </del>	Drums Fro		07. 20.	/38		<del>                                     </del>
			ŧ	nsferred to	1 81-101	6,687		
-			Lbs. Cond			31. 1.85		
			Lbs. Doca		İ	36,685		
			I	4 Cascader	l	Ti control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the control of the con	1	
		_	L	5 Storage	d to Date:	2.90/,618	2	
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	420.30	Solven	t Recovery	Facility				,
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					Total Prod	•	Condensed	
	(6) 112			Amount	Unit Cost		Unit Cost	<u></u>
						<del>                                     </del>		_!
	TOTAL LABO	OR		2,852	.155		.716	
	Direct			1,810	.098		.454	_
	1-2-9 Other			810	.044		. 204	_
	OMICT			232	.013		.058	_
	MOMAT MAG					-		_
	TOTAL MATE	ERIAL		546	.030	<del> </del>	.137	_
	Direct		!		-	<del> </del>		
	1-2-9			246	.013		.062	_
	Other	-		300	.017		.075	
			1	<u> </u>	!			_
	TOTAL LAB	BOR & MATERIA	AL !	3,398	.185	<del></del>	.853	_
					<u> </u>			_
	APE			3,344	.182		.839	_
<del></del>				<del> </del>	ļ			
		RKED MATERIA	<u>, ,                                  </u>	25	.001		.006	_
	Natural						The State	
	Special	Services (2	2791)	25	.001		.006	_
			]	<del>                                     </del>				
	TOTAL COST	<u>n</u>		6,767	.368		1.698	_
				ļ				
	TOTAL SOL	VENT RECLAIM	ED (lbs.)	ļ'		18,410		
				<u> </u>		-		
			Days Oper	ated:	ļ	22		
			Drums on	Hand - Begi	nning:	590		_
			Drums on	Hand - Endi	ng:	536		
			Drums Pro	cessed:		89		_
			Drums Tra	nsferred to	81-10:	35		_
			Lbs. Cond	ensed:		3,986		
			Lbs. Decar	nted:		14,424		
			Lbs. to A	4 Cascades	3:	18,410		_
			Lbs. to A	-5 Storage:				_
	-		ŀ		to Date:	2,920,028	/	_
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Λ¢ο	ount	2686		,
Solvent	Recov	gry	Facil	itv

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	1	1	Solven	Recovery	Facility				
	1			1	-	Total irod	iia_	Condensed	
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		Direct							1
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		TOTAL LABO	LIBETAN & BE	L	3,398	.185		.853	
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		TOTAL MORY	CD MATERIAL	L	25	.001		,006	
		Natural						2-1-7	I
		<del>                                     </del>	Services (2	2791)	25	.001		.cc6	
		TOTAL COST			6,767	.368		1,698	I
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		TOTAL SOLV	ENT PECLAIN	ED (lbs.)			18,410		I
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					and - Begi	inning:	590		
					Hand - Endi		536		
				Drums Pro	cessed:		89		$\downarrow$
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				Lbs. Cond	ensed:		3,986		
				Lbs. Deca	nted:		14,404		$\downarrow$
				Lbs. to A	-4 Cascades	<b>5 3</b>	18,410		_
				Lbs. to A	-5 Storage:		-		
			-	Total Lbs	. Recovered	to Date:	2,920,028		
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	·							
				JULY	- 1960			
•				Acco	unt 2686			-
				SOLVENT RE	COVERY FAC	LITY		
						Total Prod		Condensed
	·				Amount	Unit Cost		Unit Cost
		TOTAL LABO	R		1,792	.094		. 244
	··· · · · · · · · · · · · · · · · · ·	Direct			1,533	.080		. 208
		Maint. &	Engr.		259	.014		.036
		Departme	ntal					
	· · · · · · · · · · · · · · · · · · ·	Miscella	neous			منبص		
		TOTAL MATE	RIAL		540	.028		.073
		Direct				Circ data		
		Maint. &	Engr.		<b>25</b> 5	.013		.035
		Departme	ntal		285	.015	· · · · · · · · · · · · · · · · · · ·	.038
		Miscella	neous					
							·	
		TOTAL LABO	r & materia	L	2,332	.122		.317
		APE			1,745	.091		.237
		TOTAL WORK	ED MATERIAI	,	26	.CO1		.004
		Special	Services (2	791)	26	.001		.004
			1000 0000					
	<del></del>	TOTAL COST			4,103	.214		.558
		TOTAL SOLV	ENT RECLAIN	ED (1bs.)		•	19,155	
				Days Opera	ted:		20	
-				Drums on H	and - Begir	ning:	<u>536</u>	
				Drums on H	and - Endir	g:	524	
				Drums Proce	essed:		75	
				Drums Trans	sferred to	81-10:	63	
				Lbs. Conde	nsed:		7,359	
				Lbs. Decan	i		11,796	
				Lbs. to A-	Cascades:		19,155	
			·	Lbs. to A-	1		-C-	
				Total Lbs.	Recovered	to Date:	2,939,183	V
WCX-885 (1-59) Y	-12 Data Sheet							

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		ımv	- 1960			
		0 011	- 1900			
		Acco	int 26-6		: 	
		SOLVEIT PE	COVERY FAC	ILITY		
				Total Frod	<b>+</b>	Condensed
.			Amount	mit Cost		Unit Cost
TOTAL IABO	)		1 007			
Direct	1		1,792	. 094		. 244
Mint. &	Ener.		1,533 259	.080		.208
Dopurtier			-0-	.0/4		036
'inceller						
			-0-	_		7
TOTAL MATE	TAL		540	.028		,023
 Direct			-0-			
 Maint, &	Engr.		255	. 0/3		.035
Departmen	tul		285	. 015		. 038
'tiscellar	eous		-0 -			
TOTAL LABOR	A HATER LA	L	2,332	./22		.3/7
AFE			1,745	.09/		. 237
TOTAL WORKE	D MATERIAL		26	.00/		. 004
	orvices (2		24	.00/		.007
				.00/		7
TOTAL COST			4,163	.214		.558
TOTAL SCIVE	AT RECLAI:	ED (1bg.)			19,155	
		1.20				
		Days (perat	ed:	·	20	
		Drums on lic	nd - Begin	ning:	536	
		Drums on En	nd - Endin	7.1	524	
		drum Froce	ased:		75	
		Drums Trans	ferred to	01-10:	63	
		lbs, Conder	ged:		7359	
		Lbs. Decant	ed:		11,796	
	-	lbs. to	Cascados:		19,155	
		bs, to A-5	"torage:			
		otal Ibs.	ccovered	to Date:	2,939,153	
			•			

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			AUGUS	T - 1960			
			Acc	ount 2686			
			SOLVENT R	ECOVERY FAC	LITY		
					Total Pro	a	
				Amount	Unit Cost	<del></del>	Condensed Unit Cost
							GHIL GOST
	TOTAL LABO	R		3,369	.184		1.340
	Direct			2,122	.116		.844
	Maint, 8	Engr.		1,247	.068		.496
	Departme	ntal		-0-			
	Miscella	neous		-0-	-		
	TOTAL MATE	RIAL		790	.044		.314
	Direct			-0-			. , , , ,
	Maint. 8	Engr.		375	.021		.149
	Departme	ntal		415	.023		.165
	Miscella			-0-			
	TOTAL LABO	R & MATERI	AL	4,159	. 228		1.654
							1.074
	APE			3,063	.168		1.218
				2,002	.100		1,218
	TOTAL WORK	ED MATERIA:		76	.004		030
		Services (		76	.004		.030
			<u> </u>	70	.004		.030
	TOTAL COST			7,298	.400		0.000
				1,20	.400		2.902
	TOTAL SOLVE	ONT BECLATI	郷D (lbg )			10.0//	
		JAIL IUJULKIA	TDS.			18,266	
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			Drums Proc		5.		
	-	ŀ	i	sferred to	ี้ ชาา.ก.	<u>73</u> 58	
		i	Lbs. Conde		OT-TO!		
		ŀ	Lbs. Decan			2,515	
		İ		ced: Cascades:		15,751	
		l.	I			18,266	
			Lbs. to A-	_	to Date	-0- 2 957 119	
			TOVAL LDS.	Recovered	to Date:	2,957,449	-
WCX-885 (1-59) Y-12 Data Sheet							
	1			.			

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			Acco	unt 2686			
			SOLVERT RE	COVERY FAC	ILITY		
				Amount	Total Frod Unit Cost	<b>4</b> .	Condensed Unit Cost
	TOTAL LAB	OR		3,369	. 184		1.340
	Direct			2,122	1		.844
	Naint.	k Enor		1,247	.068		.496 .
	Departm						
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	TOTAL AT	BIAL		790	.614		.314
	Direct						_
	l'aint.	Engr.		<i>375</i>	.021		.149
	Departm	- "		115	. 023		.145
	Miscella	neous		-	_		
	TOTAL LABO	R & MATERI	ıL.	4,159	. 228		1.654
	AIE			3,063	.148		1.218
	ייראר ז זור <i>ס</i>	ED MATERIA	,	76	.084		.0.30
				76	,004		0.50
	Special	Services (	51/JL)	/ / /	,,,,,,		, <u>, , , , , , , , , , , , , , , , , , </u>
	TOTAL COST			7,298	.400		2.902
	TOTAL SOL	EM RECIAI	ED (1bs.)			18,246	
			Days Opera	ted:		23	
			-	and - Legi	nings	524	
				and - Endl	l - i	509	
			Drums Froc		_	73	
			Drums Tran	aferred to	81-10:	58	
			Lbs. Conde	nsed:		2,5/5	
			Ibs. Decur	ted:		15,751	
				4 Lascados		18,266	
		-	Ibs. to A-				
			'	cccvered	i i	2,957,449	

								1
			SEPTEMB	ER - 1960				
			Accou	n+ 2606				
		SC	LVENT RECO	VERY FACILI	TY			
-	W. C.	<u>.                                    </u>		Amount	Total Pro		Condens	
				11IIOUII C	Unit Cost		Unit Co	3t
	TOTAL LAF	BOR		2,397	.098			+
	Direct			1,492			.580	$\dashv$
	Maint.	& Engr.		905	.061		.361	+
	Departm				.037		.219	
	Miscell							+
								+
	TOTAL MAT	ERIAI.		673		-		-
	Direct				.028	<del> </del>	.163	+
	Maint.	& Engr.		543			-	+
	Departme			130	.022		.131	+
	Miscella			150_	.006		.032	-
								+
	TCTAL LABO	DR & MATERI	AT	2 070				$\bot$
		St & MAIBAL		3,070	.126		.743	-
	APE			2.0(3				-
				2,261	.093		.548	$\perp$
	TOTAL MORK	ED MATERIA		<del>                                     </del>				_
	İ	Services (2		38	.CO1		.009	-
	-200201	POTATCES /Z	1/91)	38	.CO1		.009	
	TOTAL COST							_
	101111 0001			5,369	. 220		1.300	
	TOTAL SOLD	PW DEGLATI						
	TOTAL SOLV	TMI KECTAIN	ED (lbs.)			24,373		_
			70 0					<u> </u>
			Days Opera			19_		_
				and - Begi		509		<u> </u>
				and - Endi	ng:	521		
			Drums Proc			47		
				sferred to	81-10:	59		
			Lbs. Conde			4,130		
		i i	Lbs. Decan			20,243		
		1		4 Cascades		24,373		
		1	1	5 Cascades		-0-	,	
			Total Lbs.	Recovered	to Date:	2,981,822	V	
WCX-885 (1-59) Y-12 Date	Sheet							
	1		j	Ĭ				

SEPTEMBER		1960
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## Account 2686 SOLVENT RECOVERY FACILITY

					Potal Prod. Unit Cost	•	Condensed Init Cost
	TOTAL LABOR			2,397	,098		.580
	Direct			1,492	.061		.341
		77		905	,037	·	.219
	Maint. &	1		-			
	Departmen						
	Miscellar	BEOUR					
	TOTAL MAYER	TAT.		673	.028		. 163
	Direct	Dil			7		
	Maint, &	Enco		5-43	.022		./3
				/30	.006		.032
	Doportme	1					
	Miscollar	100125					
	TCTAL LABO	ATERIA	<u> </u>	3,070	./26	·	.743
)	AFE			2,26/	. 093		.548
	,						
	TOTAL WORK	ED PATERIAL		38	.00/		.009
	Special	ervices (2	791)	3F	.00/		.007
	TOTAL COST			5,369	.220		1.300
	TOTAL SOLV	ERT RECLAIS	CD (1bs.)			24,373	
			Days Oper	at ad t		19	
			1	and - beri	inning:	509	
			1	Fond - Endi	1	521	
			irum iro	1	-	47	
				nsferred to	81-10:	59	
			Lbs. Cond			4/35	
			Ibs. Deca			20,243	
			1	/ Cascades	3	24,373	
				5 Cascades	1		
			1	. Recovered		2,98/822	
			A COULT KINGS	1.000,010.			

1	ì						
						1 .	
			OCTOBER	- 1960			
		===	Account	t 2686	]		
		30	TARL RECO	ELY FACILITY		·	
					Total Pro	a	Cohdensed
				Amount	Unit Cos		Unit Cost
TOTAL LABO							
Direct	n			2,709	.096		.423
Maint. 8	From		<del></del>	1,963	.070		.307
Departme				746	.026		.116
Miscella		<del> </del>		-0-	-0-		-0-
	ncoup		<del></del>	-0-	-0-	ļ	-0-
TOTAL MATE	DTAT						
Direct	UTAL			527	.019	ļ	.082
Maint. 8	Fr			0-	0		-0-
Departme				428	.015	ļ	.067
				99	.004		.015
Miscella	neous		<del> </del>	-0-	_0_		-0-
MODAT TARK					· ->2.24		
TOTAL LABO	K & MATERI	AL	<del> </del>	3,236	.115		.505
APE				_			
AFE				2,555	.091		.399
morner assess						ļ	
TOTAL WORK		·		27	.001		.004
Special	Services (	2791)	<del></del>	27	.001		.004
MCMAT COOL			<u> </u>	-			
TOTAL COST			<u> </u>	5,818	. 207		.908
TOTAL COLUM	IN PROTAT	en (n. )	<u> </u>				
TOTAL SOLVE	INT RECLAIL	MED (lbs.)			l (s) (real	28,090	
				<del>                                     </del>		····	
		Days Opera				18	
			and - Begi	1 3		521	
	1		and - Endi	g:	·	651	
	ı	Drums Proc	1			84	
	1		sferred to	81-10:		214	
	1	Lbs. Conde				6,403	
	1	Lbs. Decar				21,687	
	1		4 Cascades			28,090	
			5 Storage:			-0-	
		Total Lbs.	Recovered	to Date:		3,009,912	✓ <u> </u>
WCY-805A /11 FOX Y 40 -							
WCX-885A (11-58) Y-12 Data Sheet							T

OCTOBER -	1960
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				OCTCBER -	1960		1	1
				Account 2			1	1
	1	1	SOLV	EWI HECOVE	Y FACILITY	4	1	
	·				Amount	Total irod. Thit Cost	r	Condensed Init Cost
	TOTAL LABO	R			2,709	.076		.423
	Direct				1963	. 070		.307
	Maint. 8	Engr.			746	.026		.116
	Departme				_ c			_
	Miscella	neo is			0 -			
	TOTAL MATE	PIAL			527	.019		.082
	Direct							
	aint. 8	Engr.			428	, 015		.047
	Doj antino	1			79	.00+		.015
	Miscella							
	TOTAL LABO	E & MATPEI	AT,		3236	.115		.505
_						.,,-		
	APE			1	2,555	.09/		.379
					7,5	, , ,		
	TOTAL WORK	ED MATERIA			27	.00/		,004
		Services (	1		27	.00/		,007
			1721	. 1		.00		,,,,,
	TOTAL COST				5,818	.207		.908
							i	
	TOTAL SOLV	ENT RECLAI	ED (lbs.)				28,090	
	I			· 1				
			Days Cperc	ted:			18	
			1	and - Begin	hning:		521	
				and - Endir			651	
			Drums From				84	
				sforred to	81-10:		214	
			Lbs. Conde	1	01-10-		·	ĺ
			Ibs. Decar				6,403 21,687	
				V. Cascades			1 1	
		<u> </u>		<u> </u>			<u> 28090</u> - v -	
		1	Total Ubs.	5 Storace: Fecovered	to Data:		3,009,9/2	
<del></del>			10041	1 600401 000	W Dates		3,007,1/2	
	<u> </u>			<del></del>	<del></del>	<del> </del>	,	

					1		ı	į.	ı
				NOVEMBE	R - 1960				
			S	Account RECON	t  2686 /ERY FACILI	CTY			
					Amount	Total Pro Unit Con	ođ st	Condensed Unit Cost	
								circ cos (	-
	TOTAL LABO	R			2,056	.086		.422	
	Direct				1,475	.062		.302	
<del></del>	Maint &				344	.014		.071	
	Departm				237	.C10		.049	
	Miscell	aneous			0				
	ጥር እየለመን	DTAT		· · · · · · · · · · · · · · · · · · ·				· ·	
	TOTAL MATE	KLAL			367	.016		.075	
	Direct	I7			0				
	Maint &				92	.CO4		.019	
·	Departm				275	.012		.056	
	Miscell	aneous			0			****	
	COTAL LABO	TOTAL & S	AT						
	OTHER PROPERTY.	. « PHIERI	WT.	-	2,423	.102		.497	
	APE					-			_
				<u> </u>	1,951	.C32		.400	
1	OTAL WORK	D MATERTA	T.						ļ
			(2791)		0				
	-poota1	OCT ATCER	V~(71)		0	****			
1	OTAL COST				,				-
					4,374	.184		.897	<u> </u>
	OTAL SOLVE	NT RECLATI	MED (1he)					1.	
			(100)				23,778	-	
			Days Opera	ted:					
			1	and - Begin	ning•		21.		
				and - Endin			651		
			Drums Proc				1,047 148		
				sferred to	ੈ1 <b>–</b> 10:				
			Pounds Con				544		
			Pounds Dec				4,876 18,902		
				-4 Cascade	5:		23,778		
				-5 Storage			-0-		
				s Recovere			<u> </u>		
							<u></u>		
WCX-885 (1-59) Y-12	Data Sheet								
		· · · · · · · · · · · · · · · · · · ·	·	·		1		1	_ 1

	ember count	1 .	· .	
SOL	RECOVE			TT

			NOVEMBER Account	2686			
		Sot	TENT RECOVE	RY FACILITY			
				Amount	Total Prod		Condense Unit Cos
TOTAL LABOR	R			2,056	.086		422
Direct				1,475	.062		, 3 02
Maint &	Engr			344	.014		. 071
Departm				237	. 0/0		. 049
Miscell				0			
TOTAL MATE	RIAL			367	,016		.075
Direct				Ó			
Maint &	Engr			92	.007		.019
Departme	ental			275	. 0/2		.056
Miscell	nneous			0	_		
TOTAL LATIO	r & Materi	L		2,423	.102		.497
APE				1,951	.082		.400
TOTAL WORK	ED MATERIAL			0			_
Special	Services	2791)		0			
TOTAL COST				4,374	.184		. 897
TOTAL SOLV	ENT RECLAIM	ED (1bs)				23,778	
1		Days Opera	todi			21	
		Drums on H	and - Begin	ning:		651	
-		Drums on H	and - Endi	g;		1,047	
		Drums Proc	essed:			148	
			sferred to	81-10:		544	
		Pounds Con	<del> </del>			4,876	
	-	Pounds Dec	ł			18,902	
		Pounds to	A-4 Cascado	98 <b>1</b>		23, 778	<u> </u>
		Pounds to	<del> </del>	<del> </del>			
		Total Poun	ds Recovere	d to Date:		3,033,690	

	1	ł		ı	ı	1			
				DECEMBE	i <b>-</b> 1960				
				Account					
			SO	LVENT RECOV	ERY FACILI:	IX			
					·				
					Amount	Total Pro		Condensed	
	TOTAL LAB	OR				Unit Cos	7	Unit Cost	<u> </u>
	Dir	<del> </del>			2863	.101		•287	<u> </u>
		nt & Engr			2249 329	•079	<del> </del>	•226	
		artmental				•012		•033	
		cellaneous			285	•010		•029	
	1120				0	-		-	<u> </u>
	TOTAL MAT	ERTAT.			300				<b></b>
	Dir				199	•007	<del> </del>	•020	
					3	•0001	<del> </del>	. •0003	
	l i	nt & Engr artmental			18	•0006	1	•0022	
	1 - 1	cellaneous			178	•006	<del> </del>	•018	
		701100.up			0			0	
	πονατ. τ.α θέ	OR & MATERI	ΔT		22/2				
	TOTAL HAD	AL OF MAILINE	AL		3062	•108		•307	
	APE		<u> </u>						
				-	2778	•098		•279	
	TOTAL WORK	ED MATERIA	T	<u> </u>					
	TOTAL WOIL	ED PATERIA	<u> </u>		0	-		-	
	TOTAL COST				-01				
	TOTAL COST		<del></del>		5840	•206		•586	
*	TOTAL COLU	TAME DESCRIPTION							
	TOTAL SOLV	ENT RECLAI	MED (Lbs)				بندبار 28		
			D 0						
			Days Oper	<del> </del>			23		
				Hand - Begi			1,047		-
				Hand - Endi	ng		873	<u> </u>	
	1151110		Drums Pro				232		
- $A$				nsferred to	81-10		58		
- / / / /	RECEIVE	1	Pounds co				9,965		
	JAN 2519	, ,	Pounds de				18,449		
<del></del>	R. A. WALK			A-4 cascac			بلاباو28		····
				A-5 storag					
			Total pour	nds recover	ed to date		3,062,104	V	
	16111		<u> </u>						
						:			
NCV-007 /	10.5.								
WCX-885 (1-59) Y-	12 Data Sheet								_
· · · · · · · · · · · · · · · · · · ·								•	

DECEMBER	_	1960	
	_	<b></b>	

				ECEMBER -	1960			
	·		SOLVEN	Account 26				
					Amount	Total Prod Unit Cost	1	Condensed Unit Cost
	TOTAL LABO	R			2863	.1(1		.287
	Dire	at			2249	070		
		t & Engr			"	•079		•226
		rtmental			329 285	.012		•033
		ellaneous			0	-010		-029
+	TOTAL MATE	PTAT			199 3XXX	007		
$\dashv$	Dire	***						•020
+		t & Engr			3	.0001_		•0003
-					18	•0006		•0022
+		rtmental			178	•006		.018
	Misc	ellaneous			0	-		•
	TOTAL LABO	R & MATERI	AL		3062	.108		•307
	A PE	- <u>(, , , , , , , , , , , , , , , , , , , </u>			2778	•098		•279
	TOTAL WORK	ED MATERIA	7.		Ò	•		
	TOTAL COST				5840	•206		•586
	TOTAL SOLV	ENT RECLAI	ŒD (Lbs)				بلدباء 28	
			Days Opera	ted			23	
			Drums on h	and - Begi	nnino		1047	
			Drums on h		_		873	
			Drums Proc				232	
			Druma tran		81-10		58	
			Pounds con				9965	
			Pounds dec				18时6 18时	
			Pounds to				28414	
)			Pounds to	1			contri	
			Total Pour				3,062,104	
				~ 1000 1018	L OV DELOG		المستوعات ور	
					e camen			

				1.		]	1	I	•
		ı							
		•		JANUAL	Y 1961				
				Accour	t 2686				
			SOL	VENT RECOVE	RY FACILITY			4.	
٠.									
		· · · · · · · · · · · · · · · · · · ·		1.		Amount	Total Prod		Condensed Unit Cost
	TOTA	L LABOR				3246	•113		•285
		Dire	<del></del>			2786	•097		-245
			t & Engr			387	•013		•034
			rtmental			73	•002		•006
		Misc	ellaneous			0	0		0
	TOTA	L MATERIAL				519	•018		•045
		<b>*</b>							·
		Dire				. 0	. 0	·	0
		Main	t & Engr			172	•006		•015
		Depa	rtmental			347	•012		- •030
		Misc	ellaneous			0	0		0
						<del></del>			
	ТОТА	L LABOR &	MATERIAL			3765	.131		.331
-0									
	APE		<u>:</u>			3457	•120		•304
	TOTAL	L WORKED M	ATERIAL			16	•0006		•0014
-						····	·		
	TOTAL	L COST				7238	•252		<b>.</b> 636
	TOTAL	SOLVENT I	RECOVERED	(Lbs)				28,729	
						·			
				Days Oper				29.7	· · · · · · · · · · · · · · · · · · ·
		·			hand - Begi	-		873 676	
					hand - Endi	ng	\$	910	<u> </u>
				Drums Pro			Ç.	2356 159 11.378√	
-					nsferred to	81=10		159	
				Lbs. cond			~?.	11.378	•
				Lbs. deca				17,351	•
					L Cascades			-9 O	
			<u> </u>	1	5 Storage			28,729	AL DA BAN
				Total Lbs	recovered	to date	3	<b>,</b> 095 <b>,7</b> 87	3690,833
			<del></del>						+ 4954
			,			·			
1			>		l [		<u> </u>		

1	1			1	ı	ı	1	4	,
. 1									
				FEBR	UARY - 1961				
					ount 2686			1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	
	1		3		OVERY FACIL	Thy			
						Total Pro	d	Condensed	
:					Amount	Unit Cost	<u>,                                      </u>	Unit Cost	
	TOTAL LABO	R	<del>                                     </del>		07.57		<del> </del>		
	Dire				2151	•075		•292	
	Main	t & Engr	<del>                                     </del>		1617	•056	<del>                                     </del>	•220	
	i	rtmental			109	015		-058	
		ellaneous			0	•004		•015	
	TOTAL MATE	RIAL			195	•0068		0067	
	Dire				0	-		•0265	
	Main	t & Engr			48	•0016		•0065	
		rtmental			147	•005		.0199	
	Misc	ellaneous			0	-			· · · · · · · · · · · · · · · · · · ·
	TOTAL LABO	& MATERTA	т		2346	082		-319	
	TOTAL MODIE	W 264 (WWW.							
	TOTAL WORK	D MATERIAL			0			10.00	
	APE								
					2442	•085		•332	
1	FOTAL COST				1,000				
					4788	.167		•651	
	TOTAL SOLV	ENT RECLAT	MED (Lbs)						-
							28,735		
			Days O	erated			28		
				n hand - B	eginning		676	+	····
				n hand - E			522 ²		
				rocessed			177		
			Drums t	ransferred	to 81-10		23		<del></del>
				condensed	·		7,358	2. 1977	
				decanted			21,377		
				to A-4 Cas			0	31	
				to A-5 Sto			28,735		
			Total I	ounds Reco	vered to Da	te 3	124,522	NO	
					Astronomic Control				
					* * ;				
					l				

## FEURUARY - 1961

### Account 2686

	SOLVENT REC	OVERY PACIL	ITY	!		
		Amount	Total Prod Unit Cost	ł .	Condensed Unit Cost	
TOTAL LABOR		2151	•075		•292	
Direct		1617	•056			
Maint & Engr		425			•220	
Departmental		109	•015		•058	
Miscellaneous		0	•004		.015	
TOTAL MATERIAL		195	•0068		•0265	-
Direct		0	-		• •	
Maint & Engr		48	•0016		•0065	
Departmental		147	•005		,0199	
Miscellaneous		0	-		•	
TOTAL LABOR & MATERIA	Le .	2346	•082		.319	
TUTAL WORK D MATERIAL		0	-		•	
						-
APE		5hh5	•085		•332	
TOTAL COST		4788	.167		.651	
TOTAL SULVENT RECLAIS	ird (Lbs)			28,735		
	Days Operated			28		
	Drums on hand - i	seginning		67 <b>6</b>		
	Drums on hand - i			522		
	Drums Processed			177		
	Drums transferred	i to 81-10		23		
	Pounds condensed	1		7,358		
	Councis decanted		<u>†                                      </u>	21,377		
	Pounds to A-4 Cas	3Caues		0		
	Pounds to A-5 Sto			28,735		
	Total Pounds Reco		te 3,	124,522		
		1	1			

MARCH   1961   Account   2666   SOLVERT RECOVERY FACILITY   Amount   Init Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Co		ı	1	ł	1	1				
Account   2686   FACILITY   Amount   Total Frod   Condens   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit										***
Account   2686   FACILITY   Amount   Total Frod   Condens   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit										
Account   2686   FACILITY   Amount   Init Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Uni										
Account   2686   FACILITY   Amount   Total Frod   Condens   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit Cost   Unit		. 4			MARCH	1961				·
SOLVENT RECOVERY FACILITY		· ·								ļ
TOTAL LABOR   2906				SOLVI	ENT RECOVER	Y FACILITY		Potel Prod		Com dom.
TOTAL LABR		<del> </del>	<del> </del>	<del> </del>						Unit Co
Direct   2222		MORAT TAT	<del></del>		<del></del>		<u> </u>	-		
Maint & Engr   529				<del> </del>	+			•053	<b></b>	.133
Departmenta				<del></del>		<del> </del>	2222	•041		•102
Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Martine   Mart		1					529	.010		.0245
TOTAL MATERIAL   1,31   .008   .020		1				<del> </del>	155	_003	Ĺ	
TOTAL MATERIAL   1431	-	м	scellaneo	s		<u> </u>	-			
Direct			ļ		<u> </u>			·	l	
Direct		TOTAL MAT	ERIAL				431	•008		-020
Maint & Engr   226		D	rect							
Departmental   205		М	aint & Engi				226	-00)		
Miscellaneous		D	epartmenta						<del></del>	
TOTAL WORKED MATERIAL 33 .0006 .0015  A P E 2925 .054 .133  TOTAL COST 6295 .116 .287  TOTAL SOLVENT RECLAIMED (Lbs) 54,405  Days Operated 31 Drums On Hand - Beginning 522  Drums On Hand - Ending 278  Drums Processed 273  Drums transferred to 81-10 29  Pounds Condensed 21,912  Pounds Decanted 32,493  Pounds to A=5 Storage 54,405										
A P E 2925 .054 .133  TOTAL COST 6295 .116 .287  TOTAL SOLVENT RECLAIMED (Lbs) 54,405  Days Operated 31  Drums On Hand - Beginning 522  Drums Processed 278  Drums Processed 273  Drums transferred to 81-10 29  Pounds Condensed 21,912  Pounds Decanted 32,493  Pounds to A-5 Storage 54,405										
A P E 2925 .054 .133  TOTAL COST 6295 .116 .287  TOTAL SOLVENT RECLAIMED (Lbs) 54,405  Days Operated 31  Drums On Hand - Beginning 522  Drums Processed 278  Drums Processed 273  Drums transferred to 81-10 29  Pounds Condensed 21,912  Pounds Decanted 32,493  Pounds to A-5 Storage 54,405		TOTAL WOR	KED MATERIA	<b>左</b>	<del> </del>	<del></del>	22	2006		2235
TOTAL COST 6295 .116 .287  TOTAL SOLVENT RECLAIMED (Lbs) 54,405  Davs Operated 31  Drums On Hand - Beginning 522  Drums On-Hand - Ending 278  Drums Processed 273  Drums transferred to 81-10 29  Pounds Condensed 21,912  Pounds Decanted 32,493  Pounds to A-5 Storage 54,405				-			1	•0000		•0012
TOTAL COST 6295 .116 .287  TOTAL SOLVENT RECLAIMED (Lbs) 54,405  Davs Operated 31  Drums On Hand - Beginning 522  Drums On-Hand - Ending 278  Drums Processed 273  Drums transferred to 81-10 29  Pounds Condensed 21,912  Pounds Decanted 32,493  Pounds to A-5 Storage 54,405		APE								
TOTAL SOLVENT RECLAIMED (Lbs)  Days Operated  Drums On Hand - Beginning  Drums On Hand - Ending  Drums Processed  273  Drums transferred to 81-10  Pounds Condensed  21,912  Pounds Decanted  32,493  Pounds to A-5 Storage							2925	•054		.133
TOTAL SOLVENT RECLAIMED (Lbs)  Days Operated  Drums On Hand - Beginning  Drums On Hand - Ending  Drums Processed  273  Drums transferred to 81-10  Pounds Condensed  21,912  Pounds Decanted  32,493  Pounds to A-5 Storage		TOTAL COR			-	<del> </del>	<b>—</b>			
Days Operated   31		TUTAL COOP	<u> </u>	<b></b>		<b> </b>	6295	.116		-287
Days Operated   31		TOO TARIOR	TOWN DWGT AT							<u> </u>
Drums On Hand - Beginning   522		TOTAL SOLV			<b></b>				54,405	
Drums On Hand - Beginning   522						<b></b>			31	<u> </u>
Drums On Hand - Ending   278			1	1	1					
Drums Processed   273					1					
Drums transferred to 81-10   29			Da	ums Proces	sed					
Pounds Condensed 21,912 Pounds Decanted 32,493 Pounds to A-5 Storage 54,405			Dz	ums transf	erred to 81	-10				
Pounds Decanted 32,493 Pounds to A=5 Storage 54,405			Po	unds Conde	nsed					
Pounds to A=5 Storage 54,405			Po	unds Decan	ted	* .				
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MARCH - 1961

			n.	RCH - 1961			
		S		count 2686 VERY FACIL	LTY	Total Prod	Condense
					Amount	Unit Cost	Unit Co
	TARON				9006		
TUTAL	LABOR				2906	•053	.133
	Direct	**			2222	•011	•102
	Maint &				529	•010	•0245
	Departm	<b></b>			155	•003	•007
	Miscella	neous			•	-	•
TOTAL	MATERIAL				431	•008	.020
	Direct				434		
	Maint &	France			226	•004	•010
	Departme	11	<del></del>		205	•0037	.009
	Miscella		····				,
TOTAL.	WORKED MAY	FRIAL			.33	.0006	.0015
PE	· · · · · · · · · · · · · · · · · · ·				2925	•054	.133
TOTAL	COST				6295	.116	.287
				į į	1	1	
LATOT	SOLVENT RI	CLAIMED (L	b <b>s</b> )				54,405
LATOT	SOLVENT RI	CLAIMED (L	· · · · · · · · · · · · · · · · · · ·	•			54.405 31.
TOTAL	SOLVENT RI	Days Ope	· · · · · · · · · · · · · · · · · · ·				31
JATOT	SOLVENT R	Days Ope Drums On	rated	ginning			
TOTAL	SOLVENT RI	Days Ope Drums On	rated Hand - Be Hand - En	ginning			31. 522
TOTAL	SOLVENT RI	Days Ope Drums On Drums On Drums Pr	rated Hand - Be Hand - En	ginning			31 922 278
TOTAL	SOLVENT RI	Days Ope Drums On Drums On Drums Pr	rated Hand - Be Hand - En ocessed ansferred	ginning			31 522 278 273
TOTAL	SOLVENT RI	Days Ope Drums On Drums On Drums Pr Drums tr	rated Hand - Be Hand - En  cessed  ansferred  ondensed	ginning			31 522 278 273 29
TOTAL	SOLVENT RI	Days Ope Drums On Drums On Drums Pr Drums tr Pounds O Pounds D	rated Hand - Be Hand - En  cessed  ansferred  ondensed	ginning ding to 81-10			31 522 278 273 29 21,912
TOTAL	SOLVENT RI	Days Ope Drums On Drums On Drums Pr Drums tr Pounds C Pounds D	Hand - Be Hand - Encocessed ensferred ondensed ecanted o A-5 Stor	ginning ding to 81-10			31 522 278 273 29 21,912 32,493
TOTAL	SOLVENT RI	Days Ope Drums On Drums On Drums Pr Drums tr Pounds C Pounds D	Hand - Be Hand - Encocessed ensferred ondensed ecanted o A-5 Stor	ginning ding to 81-10			31 \$22 278 273 29 21,912 32,493 54,405
TOTAL	SOLVENT RI	Days Ope Drums On Drums On Drums Pr Drums tr Pounds C Pounds D	Hand - Be Hand - Encocessed ensferred ondensed ecanted o A-5 Stor	ginning ding to 81-10			31 \$22 278 273 29 21,912 32,493 54,405
TOTAL	SOLVENT RI	Days Ope Drums On Drums On Drums Pr Drums tr Pounds C Pounds D	Hand - Be Hand - Encocessed ensferred ondensed ecanted o A-5 Stor	ginning ding to 81-10			31 \$22 278 273 29 21,912 32,493 54,405
TOTAL	SOLVENT RI	Days Ope Drums On Drums On Drums Pr Drums tr Pounds C Pounds D	Hand - Be Hand - Encocessed ensferred ondensed ecanted o A-5 Stor	ginning ding to 81-10			31 \$22 278 273 29 21,912 32,493 54,405

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_				1	t 2686		!		$\Gamma = 1$
		!	s	CLVENT RECO	OVERY FACILI	dry Comb	!		1
					Amount	Unit Cost Total Prod	. '	Unit Cost Condensed	
	TOTAL	LABOR			2458	•037		•074	<b> </b>
	<u> </u>	Direct			2202	•033		•067	i
		Maint & En	gr.		256	•00/4		•008	<del></del>
		Department			-	-		<b>9</b> 000	
		Miscellane	pus		-	•		••	<u></u>
					<b>†</b>				
	TOTAL	MATERIAL			891	•013		•027	,
		Direct			-	-		-	
		Maint & En	-n		514	†		· · · • • • • • • • • • • • • • • • • •	
	1	Department				•0077		•0155	
	I I	Miscellane			377	•0056	<del></del>	•0114	
		FILOCELLA	Jus		· to	<b>66</b>			MT
	<b>ም</b> ርም ልፒ.	TINDVEN MAT		·	<del> </del>	<b> </b>			
	. IOTAL	WORKED MATE	SKLAL		-	••		•	anthonormal supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplication and supplicatio
-	APE								
	4 2 13 E				2755	•041		•083	
	TOTAL	COCM							
	TOTWE	COST			6104	•091		•182	
					<b></b>				
	TOTAL	SOLVENT REC		(Lbs)	<u> </u>		67.019		
			Days Oper	ted			30		
			Drums On I	and - Begi	nning		278		
		•	1	and - Endi	T T		67		
			Drums Pro				329		
				sferred ti	81-10		118		
			Pounds Con	idensed			33,089		
			Pounds Dec	ented			33,930		***************************************
			Pounds to	A-5 Storage	e		67,019		
				nds Recover			45,946		
									<del></del>
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# Account 2686

			SOLVENT R	COVERY PAC	LLITY			
<b>**</b>				Amount	Unit C Total P	ost rod.	Unit Condens	
101	AL LABOR			2458	•037		.074	
	Direct			2202	•033		-067	
	Maint &			256	•004		-008	<del>                                     </del>
	Dopartm	3						<b> </b>
	Miscoll	neous		-	•		-	<del>                                     </del>
101	L MATERIAL			891	•013	,	-027	
	Direct			-	-			
	Maint &			514	•0077		-0155	
	Departme			377	•0056		-0135	
	Miscella	neous		•	•		-0111	
TOTA	L WORKED A	LPL WTAT						
		TERLAL		490	-		•	
AP	E		\ <u></u>	2755	-041		083	
					9042		•083	
TOTA	L COST			6104	•091		.182	
TO TA								
TOTA	L SOLVENT 1		(Lbs)			67,019		!
		Days Ope				30		
			dand - Beg			278		
-		Drums On	Hand - End	ing		67		
		Drums Pr				329		
			unsferred t	<b>81-10</b>		118		
		Pounds Co				33,089		
		Pounds De	canted			33,930		
			A-5 Store			67,019		
	,	Total Pou	nds Recove	red to Date	3	245,946		
<b>F</b>		_						
					7	·	<i>C</i> :	
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## MAY - 1961 Account 2686

#### SOLVENT RECOVERY FACILITY

TOTAL LABOR   11h   11h   11h   11h   12h   62   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h   42h	
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## MAY - 1961 Account 2686

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#### Appount 2686

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# JULY - 1961 Account 2686 SOLVENT RECOVERY FACILITY

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			Direc	t			0		
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			Direct				1418.00	.049	.062
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-4		A	PB				3974	./37	.175
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		To	TAL COST				8145	. 280	. 358
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		To	TAL SOLVEN	RECLAIMED	(Lbs)		29,058		
	ļ			Days	Operated		20		
	ļ			Drums	On Hand -	Beginning	682		
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			<u></u>	Drums	Processed		102		
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				Pound	s Condense	ì	22,744		
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	TOTAL	COST			11,074	-134	<b>.</b> 280	
·	SOLVEN	T RECLAIME	) (Lbs)		82,508			
		Days Oper	ted		30			
 		Drums On	land - Begi	nning	398			
 		Drums On			185		Ugo ver dag	
		Drums Proc	essed		249			
 <u> </u>		Drums Tran	sferred to	81*10	36			
		Pounds - C			39,505			
		Pounds - D			43,003			
		Total Poin	ds Recover	ed to Date	3 505 000			
			~ 1000ABT	ed to Date	3,505,826			
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		Ma	rel, 1762		l		
							ı
		ACCOU	NT 2686				ı
			COVERY FACI				ı
		CONTENT RE	COVERT PROJ	1111			í
					Amount	Unit Cost Total Pro	Unit C
TOTAL	LABOR				5,125	.062	130
	Direct				3,052	,037	.077
	Maint &	Engr			1,014	,012	026
	Departm	ntal			1,059	. 013	.027
	Miscell	aneous					
TOTAL	MATERIAL				744	. 009	.012
	Direct						
	Maint &	Engr		·	730	.009	.018
	Departm	ental			14	.001	.001
	Miscell	neous				_	
TOTAL	WORKED M	TERIAL					
	·						
APE			ļ		5,205	.063	. 132
					i		-
TOTAL	COST				11,074	.134	.280
						,	-
TOTAL	SOLVENT I	ECLAIMED (	Lbs)		82,508		********
		Days Oper	ated		30		
		Drums On	Hand - Beg	inning	398		
	· · · · · · · · · · · · · · · · · · ·	Drums On	Hand - End	ing	185		
		Druns Pro	cessed		249		
		Drums Tre	nsferred to	81-10	36		
		Pounds Co	ndensed		39,505		
		Pounds De	canted		43,003		
					82,508		
	-	Total Pou	nds Recover	ed to Date	3,505,826		<del></del>
- O							
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	1 .			•				
			ACCOUNT	2686				
		s	OLVENT RECO	1	-			
	7			ĺ	1			
1			APRIL,	1962				
					Amount	Unit Cost		
	TOTAL L	L POP	1			Total Prod	Condensed	<b> </b>
					3873	-1026	-3035	
		rect			2563	•0679	2008	
		int & Engr			326	•0086	•0255	
		partmental	·		984	0261	.0771	
	M	cellaneous	3		0		**	-
	TOTAL MA	TERIAL			183	•0048	.0143	
	Di	rect					ربيده	
	1	int & Engr			0			
— <u>————————————————————————————————————</u>	1	partmental			174	•00/19	<b>-0136</b>	
-		scellaneous			9	<b>-0002</b>	•0007	
<del></del>	FIL	bcerraneons			0			
	MOMAT 1301							
	TOTAL WO	RED MATERI	AL					
	APE							
	AFE		·		4939	•1309	•3870	*
								· ·
	TOTAL CO	STP			0000		<u> </u>	
					8995	_2383	<b>20118</b>	
	TOTAL SO	VENT RECOV	(T)	<u> </u>				
				3)	37,739			
		s Operated			30			
			- Beginning		185			
	Dry	ms On Hand	- Ending		31			
	Dru	ms Process	d		171			<del></del>
-	Dru	ms transfer	red to 81-1	0	17			
		nds Condens			12,762			
		nds Decante			4,977			
				.				<del></del>
	Total	al Pounde b	ecovered to	Dot-	m n n n n n			
			ecoveted 10	Date	543,565			
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ACCOUNT	2886
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			Ì				1		
-			•	ACCOU	NT 2686				
-	1			SOLVENT REG	COVERY FACI	UTT			
			•	apri.	4,1962				
						·	Amount	Unit Cost Total Pro	
		TOTA	LIABOR				3813	.1026	,3035
			Direct				2563	.0679	. 2009
			Maint &	Engr			326	.0086	كتده.
			Departme	mtal			984	,026/-	.0771
			Miscella	neous					
	e de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de la companie de l								
		TOTA	L MATERIAL				183	.0048	.0143
	*		Direct					an : 4:	
			Maint &	Engr			174	.0046	10/36
	MT-4		Departme	ental			9	.0002	
			Miscella	<u> </u>					
		TOTAL	L WORKED M	TERIAL				·	
		AP	3				4939	,/309	. 3870
		TOTAL	COST				8995	.2383	.7048
		TOTAL	L SOLVENT H	ECLAIMED (	Lbs)		·	37,739	
				Days Oper				4757	
				<b>!</b> `	Hand - Beg	nning		185	<del></del>
				1	Hend - End	!		31	***************************************
				Drums Pro	1			171	<del></del>
					nsferred to	81_10		17	
i				Pounds Co	1	01910		12,162	
				Pounds De				24,977	
	to the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the same of the							100/1	
				Total Pou	nde Rocaver	ed to Date	3.1	43,505	
			· · · · · · · · · · · · · · · · · · ·	AV VRA£MN	MMS WOOMIS			10,500	
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	e.			ACCOUNT 26	186				
	-		SOL	VENT RECOVE	RY FACILITY				
				May, 1962					
				7, 2,02					- 1
	4.7				Amount	Unit Cost	Unit Cost		
4	<del></del>					Total Prod	Condensed	·	+
4		TOTAL LAI	BOR		2103	-1299	07/0		+
		Dia	rect				•2762		4
$\perp$			nt & Engr	<del>                                     </del>	1409	•0870	<b>.1850</b>		
1			artmental		237	•0146	•0311	<del> </del>	
			cellaneous		457	•0282	•0600		
$\perp$					0	0	0		
		TOTAL MAT	ERIAL		302	22.5			4
			ect		323	•0199	•0425		
T			nt & Engr		-	***			
T			artmental		244	•0151	•0320		
1			cellaneous		79	•0048	-0104		
1		PAS	CATTADEOUS		0	0	0		
$\dagger$		APE		<del> </del>					
T					2434	•1503	.3196		
+		SOURCE CO.							
+		TOTAL COS			1860	-3001	6382		
+									
+			ENT RECLAI		16,195				
+		Day	Operated		12				
-				- Beginning	31				
+	· ·	D ^{rt} ur	s on Hand	- Ending	164				
-			s Processe		72	3.6%			
-				red to 81-1	0 205				
_	·	Poun	ds Condens	ed	7,615				
		Poun	ds Decante	<u>a</u>	8,580				
-									-
		TOTAL POUNT	OS RECOVER	ED TO DATE		3,559,760			
			· .		·				
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				-					<del>Talija,</del>
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			-	-	•	•			

			i	T ABOUTER	Y FACILITY		ł	1
			,	May, 1962				
					Amount	Unit Cost Total Prod	Unit Cost	
		TOTAL LAI	DR		2103	•1299	.2762	
		Dir	ect		1109	•0870	•1850	
		Mai	nt & ingr		237	•0146	.0311	
		Гер	urtmental		457	•0282	•0600	
		Mis	cellaneous		0	0	0	
		TOTAL MAT	LILL		323	•0199	•0425	
	-		ect		•	, e •		
			nt & Engr	·	<b>5</b> i44	•0151	•0320	
			urtmental		79	•0048	•0104	
		lis	cellaneous		0	0	0	
		<u>-</u>						
*****		APE			2434	•1503	.3196	
				ļ				
		TOTAL CON	<u>r</u>		4860	•3001	•6382	
			VENT RICLAI		16,195			
			s Operated		12			
	·	<del></del>	<del></del>	- Beginning		·		<del></del>
			ns on iland	1	164			
			ns Processe		72			· · · · · · · · · · · · · · · · · · ·
				red to 61-1	O 205			
		· · · · · · · · · · · · · · · · · · ·	nds Condens		7,615			
		Pour	nds Decante	a	8,580			
		My Mat To	IDO DI ATTIVI					· · · · · · · · · · · · · · · · · · ·
		TOTAL LOOP	IDS MECOAF!	ED TO DATE:		ا 559,760 و 55ورو		*** 1
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								·····
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-885 (Jan'48)	Y-12 0.7: -:-							

		•	ACCOUNT 268	4		·	
		SOLV	ent recover	Y FACILITY			
			June 1962				
					Amount	<del> </del>	+.
	TOTAL TALLA	n			De 1	· · · · · · · · · · · · · · · · · · ·	+
	TOTAL LABO				754		<u> </u>
					458		+
	l l	t & Engr rtmental			11,12 151,		
		U.S. A. D. L.					
	TOTAL MATE	RIAL			-0-		
	Dire				-0-		
	i	t & Engr			-0-		
	t	rtmental			<b>-0-</b>	 	
	APE				955	 	-
							-
	TOTAL COST		-		-1,709		-
							+
							+
	TOTAL SOLVE	ENT RECLAIM	It:D		-0-		+
						· · · · · · · · · · · · · · · · · · ·	+
		·					+
	TOTAL POUN	randonea oc	מייניט מייני מיי		3,559,760		
	TOTAL TOOK	D MICOVERI	D IO DILLE		100		
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ĀC	COUNT	2686	

				! !	-	: 
		ACCOUNT 2686 SOLVENT RECOVERY				
		July 1962				
				Amount		
1	TOTAL LABOR			555		
	Direct	-		241		
	Maint & Engr			144		<del>                                     </del>
	Department			170		
	TOTAL MATERIAL					
				0		
	Direct			0		
	Maint & Engr			0		ļ
	Departmental			0		
	APE			427		
	momax does			<del></del>		
	TOTAL COST		· · · · · · · · · · · · · · · · · · ·	982		
)—						
·····	TOTAL SOLVENT RECLAIMED			<del>-</del> 0-		
·· · · · · · · · · · · · · · · · · · ·						
	TOTAL POUNDS RECOVERED T	O DATE		3,559,760		
				,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,		
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·		1.	N .	ACCOUNT	2686				
· -				SOLVENT REC		. T <b>?</b> ▼			
		!		AUGUST,					
		1		AUGUSI,	1902		Unit Cost		ł
	1-4					Amount	Total Prod		
		TOTAL I	ABOR			1,432	•0ñ89		_
		Direc				843	.0286		+
		Maint	& Engr			247	•0084		+
1 (1) (1) (1) (1) (1) (1) (1) (1) (1) (1		Depar	tmental			2با3	•0116		
1 - 3									
1 A 1 4			ATERIAL			94	•0032		
		Direc				-0-	<del>-</del> 0-		
21			& Engr			1.8	•0006		
		Depar	tmental			76	÷0026		
							·		<del></del> -
		APE				7 202	01.30		+-
		`				1,292	.0439		+-
		TOTAL E	ipense			2,818	.0957		+
				·			44//		+
									1
		Solvent	RECLAIMED	(Lbs)	29,453				
		1	ted (Lbs)		29,453				
		Conde	nsed )Lbs)		-0-				
								•	<del> </del>
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								····	┼
		TOTAL PO	וושתים פעימון	ERED TO DAT	mp	3,589,7/3			┼
		TOTAL FO	OCEAN CARO	EVED IO DEI	<u>.</u>	3,613,624			+
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385 (Jan'48)	Y-12 DATA SHE	ET				1			

			Acc	04N+ 268	4				
•			Sept.	1962					
					AmT.	UNIT GST Total Arod.			
		Total 4	AboR		486	.0964			
		DiRECT			250	.0494			
		Maint +			184	,0365			
		Departa	<b>,</b>		52	.0/03		·	-
			MAteRial		5	.0009			-
		Durke			0				-
			+ ENGR		0		<u>-</u>		-
		Depar	PHENTOL		5	.0009			
		APE			376	.0746			-
+		<u> </u>						ļ	-
		Total t	Rpense		867	.172			
		Solvent	Reclaime	4	5,039		·		-
				(2)	5,039				
		Cond	ensed (H	(5)	0	<del></del>	·		<del> </del>
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·····									<del> </del>
			1 1		<b></b>				<del>                                     </del>
· · · · · · · · · · · · · · · · · · ·		70184 F	ounds he	overed To	date	3,594,252			-
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									<del>-</del>
35 (Jan'48	3) Y-12 DATA S	SHEET							

Y/HG-0023

## ACCOUNT 2606 SOLVENT RECOVERY FACILITY

1962 1962

i.		·		7 19	102			
् क्रिंग 					Amount	Unit Cost		
	TOTAL	LABOR			53			
· <del></del> -		Direct			0			
		Maint & E	ng <b>r</b>		0			
		Departmen	tal		53			
		Other			0			
	TOTAL	MATERIAL			0			
		Direct			0			
		Maint & E	ner		0			
		Departmen			0			
		Other			0		<del>4 </del>	
	APE		<u> </u>		45			
			Pair v 1904 5 - 5 6 6 6 6 6 9 6 6 6 6 6 6 6 6 6 6 6 6 6					
	TOTAL	EXPENSE			98			
<del></del>	Solver	t Reclaime	i (Lts)		0			
		Decanted	(Lbs)		0			
		Condensed	(Lbs)		0			
	Total	Pounds Rec	vered To	Date .	594,252			
			*					
								,
			ADDROVE					
			APPROV	FOR PL	BLIC RELI	ASE	W	
			Ste	1	3/4/	54		
			Technical	Information	Office Dat	¢		
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				1			<del></del>	